



**US Army Corps
of Engineers**
Construction Engineering
Research Laboratories

**USACERL Technical Report 97/143
November 1997**

Development of a Biosolids Management Strategy for U.S. Forces, Korea Installations

by

Byung J. Kim
Amy R. Swanson

DTIC QUALITY INSPECTED 2

Currently, wastewater sludge for the U.S. Forces, Korea (USFK) and the Eighth U.S. Army (EUSA) is disposed at landfills by Korean contractors. In the United States, CFR 40, Part 503 regulations encourage the beneficial use of biosolids. However, beneficial use of sludge is not practiced in Korea. This report discusses the different regulatory frameworks in the United States and Korea, the current status of USFK/EUSA sludge management at four Directorates of Public Works (DPWs) and improved sludge management systems. Technical alternatives for improving sludge management include mobile mechanical dewatering, alkaline stabilization, composting, reed bed use, and autothermal thermophilic aerobic digestion (ATAD). Technologies were chosen for review

based on their ability to comply with U.S. and Korean regulations and to achieve long-term improvement, and their availability in Korea. The study recommended:

1. Use of mobile mechanical dewatering followed by either aerated static pile composting, windrow composting or alkaline stabilization for the Western Corridor DPW
2. Discontinuation of the current secondary treatment at the Yongsan DPW
3. Conversion of the Camp Humphreys' current sand-drying beds to reed beds
4. Establishment of a long term goal to convert Camp Casey's aerobic digester to ATAD and using the biosolids as a soil supplement at Camp Casey.

19980317 070

The contents of this report are not to be used for advertising, publication, or promotional purposes. Citation of trade names does not constitute an official endorsement or approval of the use of such commercial products. The findings of this report are not to be construed as an official Department of the Army position, unless so designated by other authorized documents.

DESTROY THIS REPORT WHEN IT IS NO LONGER NEEDED

DO NOT RETURN IT TO THE ORIGINATOR

USER EVALUATION OF REPORT

REFERENCE: USACERL Technical Report 97/143, *Development of Biosolids Management Strategy for U.S. Forces, Korea Installations*

Please take a few minutes to answer the questions below, tear out this sheet, and return it to USACERL. As user of this report, your customer comments will provide USACERL with information essential for improving future reports.

1. Does this report satisfy a need? (Comment on purpose, related project, or other area of interest for which report will be used.)

2. How, specifically, is the report being used? (Information source, design data or procedure, management procedure, source of ideas, etc.)

3. Has the information in this report led to any quantitative savings as far as manhours/contract dollars saved, operating costs avoided, efficiencies achieved, etc.? If so, please elaborate.

4. What is your evaluation of this report in the following areas?

a. Presentation: _____

b. Completeness: _____

c. Easy to Understand: _____

d. Easy to Implement: _____

e. Adequate Reference Material: _____

f. Relates to Area of Interest: _____

g. Did the report meet your expectations? _____

h. Does the report raise unanswered questions? _____

i. General Comments. (Indicate what you think should be changed to make this report and future reports of this type more responsive to your needs, more usable, improve readability, etc.)

5. If you would like to be contacted by the personnel who prepared this report to raise specific questions or discuss the topic, please fill in the following information.

Name: _____

Telephone Number: _____

Organization Address: _____

6. Please mail the completed form to:

Department of the Army
CONSTRUCTION ENGINEERING RESEARCH LABORATORIES
ATTN: CECER-TR-I
P.O. Box 9005
Champaign, IL 61826-9005

REPORT DOCUMENTATION PAGE

Form Approved
OMB No. 0704-0188

Public reporting burden for this collection of information is estimated to average 1 hour per response, including the time for reviewing instructions, searching existing data sources, gathering and maintaining the data needed, and completing and reviewing the collection of information. Send comments regarding this burden estimate or any other aspect of this collection of information, including suggestions for reducing this burden, to Washington Headquarters Services, Directorate for Information Operations and Reports, 1215 Jefferson Davis Highway, Suite 1204, Arlington, VA 22202-4302, and to the Office of Management and Budget, Paperwork Reduction Project (0704-0188), Washington, DC 20503.

1. AGENCY USE ONLY (Leave Blank)

2. REPORT DATE
November 1997

3. REPORT TYPE AND DATES COVERED
Final

4. TITLE AND SUBTITLE

Development of Biosolids Management Strategy for U.S. Forces, Korea Installations

5. FUNDING NUMBERS

MIPR
7-017

6. AUTHOR(S)

Byung J. Kim and Amy R. Swanson

7. PERFORMING ORGANIZATION NAME(S) AND ADDRESS(ES)

U.S. Army Construction Engineering Research Laboratories (USACERL)
P.O. Box 9005
Champaign, IL 61826-9005

8. PERFORMING ORGANIZATION
REPORT NUMBER

TR 97/143

9. SPONSORING / MONITORING AGENCY NAME(S) AND ADDRESS(ES)

Headquarters, U.S. Forces, Korea (USFK) and 8th U.S. Army (EUSA)
ATTN: HQ USFK/EUSA
Environmental Program Office, Unit 15237
APO 96205-0010

10. SPONSORING / MONITORING
AGENCY REPORT NUMBER

11. SUPPLEMENTARY NOTES

Copies are available from the National Technical Information Service, 5285 Port Royal Road, Springfield, VA 22161.

12a. DISTRIBUTION / AVAILABILITY STATEMENT

Approved for public release; distribution is unlimited.

12b. DISTRIBUTION CODE

13. ABSTRACT (Maximum 200 words)

Currently, wastewater sludge for the U.S. Forces, Korea (USFK) and the Eighth U.S. Army (EUSA) is disposed at landfills by Korean contractors. In the United States, CFR 40, Part 503 regulations encourage the beneficial use of biosolids. However, beneficial use of sludge is not practiced in Korea. This report discusses the different regulatory frameworks in the United States and Korea, the current status of USFK/EUSA sludge management at four Directorates of Public Works (DPWs) and improved sludge management systems. Technical alternatives for improving sludge management include mobile mechanical dewatering, alkaline stabilization, composting, reed bed use, and autothermal thermophilic aerobic digestion (ATAD). Technologies were chosen for review based on their ability to comply with both U.S. and Korean regulations and to achieve long-term improvement, and their availability in Korea. The study recommended:

1. Use of mobile mechanical dewatering followed by either aerated static pile composting, windrow composting or alkaline stabilization for the Western Corridor DPW
2. Discontinuation of the current secondary treatment at the Yongsan DPW
3. Conversion of the Camp Humphreys' current sand-drying beds to reed beds
4. Establishment of a long term goal to convert Camp Casey's aerobic digester to ATAD and using the biosolids as a soil supplement at Camp Casey.

14. SUBJECT TERMS

Korea
sludge disposal
wastewater treatment systems
waste management

15. NUMBER OF PAGES
160

16. PRICE CODE

17. SECURITY CLASSIFICATION
OF REPORT

Unclassified

18. SECURITY CLASSIFICATION
OF THIS PAGE

Unclassified

19. SECURITY CLASSIFICATION
OF ABSTRACT

Unclassified

20. LIMITATION OF
ABSTRACT
SAR

Foreword

This study was performed for the United States Forces, Korea (USFK) and the Eighth United States Army (EUSA). Environmental Program Office, under MIPR 7-017, Work Unit V17, "USFK/EUSA Sludge (Biosolids) Management Study." The technical monitors were Ernest P. Eddy and Munkyu Park, HQ, USFK/EUSA, Assistant Chief of Staff Engineer, Environmental Program Office, Unit #15237, APO 96205-0010.

This work was performed by the Industrial Operations Division (UL-I) of the Utilities and Industrial Operations Laboratory (UL), U.S. Army Construction Engineering Research Laboratories (USACERL). Amy R. Swanson is a Civil Engineer employed as a Research Assistant by USACERL while studying at the University of Illinois towards her masters degree in Environmental Engineering. The USACERL principal investigator was Dr. Byung J. Kim. Walter J. Mikucki is Chief, CECER-UL-I; Martin J. Savoie is Acting Laboratory Operations Chief, CECER-UL; and Gary W. Schanche is the responsible Technical Director, CECER-UL. The USACERL technical editor was William J. Wolfe, Technical Resources.

COL James A. Walter is Commander and Dr. Michael J. O'Connor is Director of USACERL.

Contents

SF 298	1
Foreword	2
1 Introduction	5
Background	5
Objectives	6
Approach	6
Scope	6
Mode of Technological Transfer	7
2 Regulatory Framework	8
United States Environmental Regulations	8
Part 503 Overview	9
Korean Environmental Regulations	14
3 Current USFK/EUSA Sludge Management	17
Technical Options for Improved USFK/EUSA Biosolids Management	18
Western Corridor	18
Yongsan	30
Camp Humphreys	30
Camp Casey	34
4 Conclusions and Recommendations	37
Conclusions	37
Recommendations	37
References	39
Abbreviations and Acronyms	41
Appendix A: Frontier Technology Belt Filter Press	A1
Appendix B: JWI J-press	B1
Appendix C: Sharples Centrifuge	C1

Appendix D: TRIMAX Environmental	D1
Appendix E: N-Viro	E1
Appendix F: CemenTech	F1
Appendix G: Davis Industries	G1
Appendix H: Resource Recovery Systems	H1
Appendix I: Transcripts of Phone Interviews With Composting Facilities	I1
Appendix J: Krüger	J1
Distribution	

1 Introduction

Background

Effective sludge management can be a difficult and expensive task for wastewater treatment plant (WWTP) operators. As sludge regulations become more stringent and more landfills are closed down, many WWTPs are consequently forced to develop new and more effective residual management plans. Solids residual management is a global environmental problem. While it may appear that each nation takes a different approach for residual management, in reality, individual WWTPs have unique combinations of environmental conditions and regulatory requirements. The best solution for solids residual problems may vary by location and by individual WWTP. Key factors affecting the success of good residual management for a WWTP include, but are not limited to:

- the regulatory framework and attitude of government
- available technologies and "know-how"
- economical feasibility and available resources
- public awareness and acceptance.

The U.S. Forces, Korea (USFK) and Eighth United States Army (EUSA) installations have been proactive in environmental protection within the Republic of Korea. In Korea, all host country WWTP's sludge is landfilled. Currently, USFK/EUSA spend about \$1 million a year for contracted sludge disposal. Korean sludge contractors transport sludge to local WWTPs for further thickening, stabilization, and disposal at landfills. One of USFK/EUSA Environmental Program Office initiatives is to develop a sludge management strategy for USFK/EUSA's wastewater treatment plants.

Objectives

The objectives of this study were:

1. To compile and analyze design and operational data of the 10 USFK/EUSA WWTPs operated by the Western Corridor Directorate of Public Works (DPW), the Yongsan DPW, the Camp Humphreys DPW, and the Camp Casey DPW.
2. To identify and evaluate technical alternatives for beneficial use of sludge and improved sludge management at USFK/EUSA WWTPs.
3. To recommend a sludge management program in which: (a) the technology can comply with Korean environmental regulations as well as U.S. regulations, (b) the system is cost effective and could be implemented with a 5-year return on investment, and (c) the technology is readily available or accessible to USFK/EUSA.

Approach

1. An extensive literature search was performed to review technologies available for dewatering and/or ultimate use and disposal of WWTP biosolids. Appropriate vendors of the feasible technologies were contacted.
2. U.S. WWTPs that operate compost facilities of similar size to USFK/EUSA's needs were contacted and interviewed.
3. The USFK/EUSA WWTPs discussed in this report were visited by an author to review the unit operations that generate, treat, and affect the beneficial use of sludge as well as available space and equipment that would affect decisions on implementation of sludge management systems.
4. Preliminary cost information from vendors and existing facilities was compiled and compared.

Scope

Since the technology implementation must meet both Korean and U.S. regulations, this study's recommendations pertain specifically to U.S. Forces, Korea installations. However, USFK sludge generation volume is extremely small in comparison with the volume generated in Korea. It is hoped that the

implementation of improved USFK/EUSA sludge management systems, designed to meet both U.S. and Korean requirements, may provide a constructive model for improved sludge management in Korea and for closer cooperation between the Korean Government and U.S. Forces, Korea.

Mode of Technology Transfer

It is anticipated that the USFK/EUSA will implement the technologies presented in this report at such a time when sludge disposal costs have risen to a level where a 5-year return on investment is possible.

2 Regulatory Framework

United States Environmental Regulations

Although manure and sludge have long been used as agricultural fertilizer, the scientific evaluation of sludge use is relatively recent. Rudolfs (1928) determined the fertilizer value of various sludges at different wastewater treatment plants. Five decades later, the Federal Water Pollution Control Amendments of 1972 recognized land application of sludges as an alternative method for sludge disposal, and also recognized a need for land application research. In 1979, the U.S. Environmental Protection Agency (USEPA) implemented land application criteria including pH, cadmium application rates, and polychlorinated-biphenyl (PCB) concentrations. In 1984, the USEPA issued its "Policy on Municipal Sludge Management," which actively promoted the beneficial use of sludge while maintaining and improving environmental quality and protecting public health. The "beneficial use of sludge" provides two benefits: (1) it saves landfill space while reducing liability from landfill, incineration, and ocean dumping, and (2) it improves soil properties by increasing nutrient levels while reducing the use of chemical fertilizers as soil amendments or organic fertilizers. In 1993, the USEPA adopted the most comprehensive, technically based sludge regulation to date. These regulations, known as Part 503, encourage the beneficial use of biosolids. (Note that this report uses the terms "biosolids," "sludge," and "residual" interchangeably.)

Residual management strategy is greatly affected by different federal, as well as State and local policies, laws, and regulations. In addition to Part 503 regulations, the Federal regulations applied to sludge use and disposal include:

- *Marine Protection, Research and Sanctuaries Act*, which bans ocean dumping of sludge.
- *Toxic Substance Control Act*, which requires sludge containing PCB to be disposed of in a hazardous waste incinerator, in a chemical waste landfill or by an USEPA approved alternative method.

- *Clean Air Act Ambient Air Quality Standards*, New Source Performance Standards, and National Emissions Standards for Hazardous Air Pollutants, which apply to the operation of sludge incinerators and dryers.
- *Resource Conservation and Recovery Act*, which considers a sludge with hazardous characteristics as hazardous waste and regulates landfill and land application.
- *Clean Water Act*, which requires the USEPA to identify all major sludge use and disposal methods. The USEPA established Part 503 regulations to meet these requirements.
- *National Environmental Policy Act*, which may require an environmental impact statement for sludge facilities that significantly affect the environment.
- *Comprehensive Environmental Response, Compensation, Liability Act and Superfund Amendments and Reauthorization Act*, which apply to clean-up of sludge containing hazardous substance, and information release to the public.

Part 503 Overview

Title 40 of the Code of Federal Regulations, Part 503 was published on 19 February 1993 and became effective on 22 March 1993. Commonly referred as "Part 503," these regulations establish standards for beneficial land application, surface disposal, and incineration of biosolids. However, since the focus of this study is on the beneficial use of sludge, surface disposal and incineration regulations will not be discussed in this report. The requirements of Part 503 apply to generators, preparers, and appliers of sewage sludge. Land application requirements include pollutant limits, pathogen, and vector attraction reduction as well as site restrictions, management regulations, general requirements, monitoring, and recordkeeping and reporting requirements. Since Part 503 was published, many biosolids treatment processes that previously had not been used in the United States have been re-explored as technologies capable of meeting the new regulations.

Part 503 regulates the concentrations of 10 heavy metals in land applied biosolids. All biosolids must meet the ceiling concentration limits shown in Table 1 to be applied to land. In addition to the ceiling concentration limits, at least one of the other requirements, i.e., pollutant concentration limits, cumulative pollutant loading limits, or annual pollutant loading limits (Table 1) must be met. Note that the limits are on a dry weight basis. Commonly,

Table 1. Pollutant Limits.

Pollutant	Ceiling Concentration Limits for All Biosolids (mg/kg)	Pollutant Concentration (mg/kg)	Cumulative Pollutant Loading Rate Limits (kg/hectare)	Annual Pollutant Loading Rate Limits (kg/hectare/year)
Arsenic	75	41	41	2.0
Cadmium	85	39	39	1.9
Chromium	3,000	1,200	3,000	150
Copper	4,300	1,500	1,500	75
Lead	840	300	300	15
Mercury	57	17	17	0.85
Molybdenum	75	—	—	—
Nickel	420	420	420	21
Selenium	100	36	100	5.0
Zinc	7,500	2,800	2,800	140
Applies to	All biosolids that are land applied	Bulk biosolids and bagged biosolids	Bulk biosolids	Bagged biosolids
From Part 503 (EPA, 1994)	Table 1, Section 503.13	Table 3, Section 503.13	Table 2, Section 503.13	Table 4, Section 503.13

analysis and reporting of biosolids are mistakenly performed in incorrect units (e.g., mg/L). This is an easily avoidable error in complying with Part 503.

In addition to the heavy metal requirements, Part 503 specifies pathogen reduction levels. Biosolids are classified as either Class A or Class B according to the achieved pathogen reduction. Class A biosolids may be applied anywhere without site restrictions. Class B biosolids still contain some pathogens and site restrictions must be applied. The site restrictions ensure that Class B biosolids present no hazard to public health. Pathogen reduction should be performed prior to or concurrently with vector attraction reduction, with few exceptions.

Class A biosolids must have either a density of fecal coliform less than 1000 most probable numbers (MPN) per gram total solids or a density of *Salmonella* sp. bacteria less than 3 MPN per 4 grams of total solids. Both these densities are on a dry weight basis. In addition to meeting this requirement, Class A biosolids must meet one of the following six alternatives:

- *Alternative 1: Thermally Treated Biosolids.* Biosolids must be subjected to one of four time-temperature regimes. The regimes are based on the percentage of solids in the biosolids. Equations are used to relate the temperature and time required to treat the biosolids.
- *Alternative 2: Biosolids Treated in a High pH-High Temperature Process.* The pH must be elevated to greater than 12 for at least 72 hours while

maintaining the temperature above 52 °C for at least 12 of the 72 hours. The biosolids must be air dried to over 50 percent solids after this period.

- *Alternative 3: Biosolids Treated in Other Known Processes.* The preparer must demonstrate that the process can reduce enteric viruses and viable helminth ova. The operating conditions used in the demonstration must be maintained after the pathogen reduction demonstration is completed.
- *Alternative 4: Biosolids Treated in Unknown Processes.* This alternative applies to cases where the biosolids treatment is either unknown or operated under conditions that are less stringent than would qualify under any other Class A alternative. Under this alternative, the biosolids are analyzed for enteric viruses and viable helminth ova when being used, disposed, or prepared for sale, give away or tests to ensure that EQ requirements are met.
- *Alternative 5: Biosolids Treated in a Process To Further Reduce Pathogens.* Biosolids must be treated in one of the following Processes to Further Reduce Pathogens (PFRP): composting, heat drying, heat treatment, thermophilic aerobic digestion, beta ray irradiation, gamma ray irradiation, or pasteurization. Minimum operating requirements for each of these PFRPs are established in Appendix B of Part 503. These requirements are presented throughout this report where they apply to USFK/EUSA sludge.
- *Alternative 6: Biosolids Treated in a Process Equivalent to a PFRP.* The treatment process used must be determined to be equivalent to a PFRP by the permitting authority. The treatment process must consistently reduce pathogens to levels that compare to those achieved using one of the listed PFRPs and must be operated under conditions that do so. The permitting authority is responsible for verifying equivalency.

Class B biosolids must meet one of the following three alternatives:

- *Alternative 1: Monitoring of Indicator Organisms.* Seven samples of the treated biosolids must be collected shortly before use or disposal. The geometric mean fecal coliform density of the samples must be less than 2 million colony forming units (CFU) or less than 2 million MPN per gram biosolids. These seven samples should be collected over a 2-week period since the fecal coliform density test has poor precision and biosolids quality can vary.

- *Alternative 2: Biosolids Treated as a Process To Significantly Reduce Pathogens.* Biosolids must be treated in one of the following Processes to Significantly Reduce Pathogens (PSRP): aerobic digestion, air drying, anaerobic digestion, composting, or lime stabilization. Minimum operating requirements for each of these PFRPs are established in Appendix B of Part 503. These requirements are presented throughout this report where they apply to USFK/EUSA sludge.
- *Alternative 3: Biosolids Treated in a Process Equivalent to a PSRP.* The treatment process used must be determined to be equivalent to a PSRP by the permitting authority. The permitting authority is responsible for verifying equivalency.

Vector attraction reduction (VAR) requirements are necessary since vectors, such as flies, mosquitoes, fleas, rodents, and birds, are capable of transmitting pathogens from wastewater sludge to humans and animals. Part 503 contains 12 options for the reduction of vector attraction. Options 1 through 8 reduce the attractiveness of the sludge to vectors. Options 9 and 10 prevent vectors from coming in contact with the biosolids. Options 11 and 12 apply to surface disposal and incineration.

- *Option 1: Reduction in Volatile Solids Content.* The mass of volatile solids in the biosolids is reduced by at least 38 percent during treatment.
- *Options 2 and 3: Additional Digestion of Anaerobically Digested or Aerobically Digested Biosolids.* The preparer must demonstrate after 40 additional days in the digester at temperatures between 30 and 37 °C that the volatile solids in the biosolids are reduced by less than 17 percent during the bench test.
- *Option 4: Specific Oxygen Uptake Rate for Aerobically Digested Solids.* Adequate VAR is demonstrated when the specific oxygen uptake rate (SOUR) of the biosolids is equal to or less than 1.5 milligrams of oxygen per hour per gram of total biosolids, at 20 °C.
- *Option 5: Aerobic Processes at Greater Than 40 °C.* The biosolids must be treated aerobically for at least 14 days at an average temperature of 45 °C. The temperature must not drop below 40 °C during this time.
- *Option 6: Addition of Alkaline Material.* Adequate VAR is achieved when enough alkaline material is added to raise the pH to at least 12, at 25 °C, and maintain the pH without adding any more alkaline material. In addition, the pH must be maintained at 11.5 for an extra 22 hours without adding more alkaline material.

- *Option 7: Moisture Reduction of Biosolids Containing No Unstabilized Solids.* Water must be removed from biosolids containing no unstabilized solids to achieve a solids content of at least 75 percent.
- *Option 8: Moisture Reduction of Biosolids Containing Unstabilized Solids.* Water must be removed from biosolids containing unstabilized solids to achieve a solids content of at least 90 percent.
- *Option 9: Biosolids Injection Biosolids Are Injected Below the Ground Surface.* Class A biosolids must be injected within 8 hours after the pathogen-reducing process is complete. No biosolids may be present on the surface within 1 hour of injection.
- *Option 10: Incorporation of Biosolids into the Soil.* Biosolids are incorporated into the soil within 6 hours of application by plowing or some other means of mixing. Class A biosolids must be applied within 8 hours after the pathogen-reducing process is complete.

The heavy metal, pathogen, and vector attraction reduction requirements discussed above are used to determine which land application option is met. Four options, all of which equally protect public health through management practices, site restrictions, and general requirements, are (in order of increasing regulatory requirements) Exceptional Quality (EQ), Pollutant Concentration (PC), Cumulative Pollutant Loading Rate (CPLR), and Annual Pollutant Loading Rate (APLR).

To qualify under the EQ option, biosolids must meet the ceiling concentration and the pollutant concentration limits in Table 1, Class A pathogen requirements and one of the first eight VAR options. EQ standards are typically met through alkaline stabilization, composting, and heat drying. During land application, the following are not required: site restrictions, general requirements, management practices, and tracking of added pollutants.

To qualify under the PC option, biosolids must meet the ceiling concentration and the pollutant concentration limits in Table 1, Class B pathogen requirements, and one of the first 10 VAR options. Class A biosolids, which meet either VAR Option 9 or 10, are considered PC biosolids. PC biosolids may be land applied anywhere except lawn and home gardens. PC biosolids must meet all management requirements, and PC biosolids that only meet Class B pathogen requirements also require site restrictions.

CPLR biosolids must meet the ceiling concentration limits and the Cumulative Pollutant Loading Rates in Table 1, either Class A or Class B pathogen

requirements, and one of the first 10 VAR options. In addition, CPLR biosolids are subject to general requirements, applicable site restrictions, and management practices. CPLR biosolids may be applied in bulk. When any one or more of the CPLRs in Table 1 is reached at a site, no additional bulk solids subject to these limits may be applied.

APLR biosolids must meet the ceiling concentration limits and the Annual Pollutant Loading Rates in Table 1, Class A pathogen requirements, one of the first eight VAR options and Part 503 general requirements, applicable site restrictions and management practices. APLR biosolids may be sold or given away in labeled bags or other labeled containers. The APLR option limits the total amount of biosolids that may be applied at one site annually. When any one or more of the APLRs in Table 1 is reached at a site in a given year, no additional biosolids may be applied that year.

To ensure the requirements of Part 503 are met, all biosolids, regardless of which land application option is met, must follow frequency of monitoring, recordkeeping, and reporting requirements through sampling and analysis of biosolids. Typically, the preparer is responsible for sampling the sludge. However, the land applier, surface disposer, and incinerator of biosolids may be responsible, depending on the circumstances. When biosolids are to be land applied, they must be sampled for metals, pathogens, vector attraction reduction and nitrogen. Part 503 has a frequency of monitoring schedule for biosolids sampling (Table 2). The main purpose is to ensure that biosolids are sampled before use or disposal. Part 503 provides specific analytical methods to be used during sampling.

Korean Environmental Regulations

The Korean Ministry of Environment has no specific regulations such as the United States Part 503 to encourage and regulate beneficial use of sludge. Korean environmental regulations potentially related to sludge include:

1. *Water Environment Preservation Law, Presidential Decree and Implementation Orders*, which regulates the discharge of wastewater into Korean waters and emphasizes industrial wastewater treatment.
2. *Waste Management Law, Presidential Decree and Implementation Orders*, which regulates hazardous waste generated from industrial activities.
3. *Soil Environment Preservation Law, Presidential Decree and Implementation Orders*, which regulates disposal of hazardous waste to soil environment.

The *Soil Environmental Law Implementation Order Annex 3* shows soil pollution countermeasure standards (Table 3). Table 3 also contains the Pollutant Concentration limits of Part 503 Exceptional Quality biosolids for comparison. Korean standards in Table 3 are concentrations in the environment. In comparison, the U.S. standards for pollutant concentration limits are in the biosolids. The Korean standards are very stringent, and it is unknown at this time whether USFK/EUSA will be required to meet these criteria before land application. However, it has been assumed that the Korean government will allow the U.S. Army to land apply biosolids on USFK/EUSA grounds if U.S. regulations are met.

Table 2. Frequency of monitoring for surface disposal of biosolids (USEPA 1993).

Biosolids Amounts (metric tons/year)	Biosolids Amount (English tons)		Frequency
	Average per day	per year	
Greater than zero but less than 290	>0 to <0.85	>0 to <320	Once per year
Equal to or greater than 290 but less than 1,500	0.85 to <4.5	320 to <1,650	Once per quarter (4 times per year)
Equal to or greater than 1,500 but less than 15,000	4.5 to <45	1,650 to <16,500	Once per 60 days (6 times per year)
Equal to or greater than 15,000	>45	>16,500	Once per month (12 times per year)
Methane gas in air			Continuously with methane monitoring device if biosolids unit is covered

Table 3. Soil Pollution Countermeasure Standards and Part 503 Concentration Limit.

Pollutant	Farmland (mg/kg)	Industrial Area (mg/kg)	U.S. Part 503 Pollutant Conc. Limit (mg/kg)
Cadmium	4	31	39
Copper	125	500	1,500
Arsenic	15	50	41
Mercury	10	40	17
Lead	300	1,000	300
Chromium (6+)	10	30	1,200
PCB	—	30	—
Cyanide	5	300	—
Phenol	10	50	—
Oil and grease	—	200	—

3 Current USFK/EUSA Sludge Management

The USFK and EUSA own and operate approximately 30 small wastewater treatment plants with design capacities ranging from 0.03 to 2.5 million gallons per day (MGD) (1 gal = 3.78 L). Of these plants, WWTPs in four DPWs are discussed below as typical examples in USFK/EUSA and are analyzed in this report.

The Western Corridor DPW operates the seven following WWTPs: (1) Camp Howze (design flow of 0.18 MGD), (2) Camp Edwards (0.09 MGD), (3) Camp Pelham (0.15 MGD), (4) Camp Giant (0.03 MGD), (5) Camp Stanton (0.10 MGD), (6) Camp Greaves (0.10 MGD), and (7) Liberty Bell (0.80 MGD). These are package WWTPs consisting of primary clarification, rotating biological contactors (RBC), secondary clarification, and aerobic sludge digestion. Digested sludge is collected by a Korean contractor and further treated at a Korean night soil plant. The night soil plant sludge is disposed at Kimpo Landfill. Approximately 1,333,488 gal of sludge is disposed annually. Currently, the Western Corridor DPW spends \$90,737 annually for removal and disposal of accumulated sewage sludge.

The Yongsan DPW operates the Yongsan WWTP, which treats wastewater produced by the industrial and residential complexes of Yongsan Main Garrison. The plant discharges into the Han River. Designed for a flow of 2.5 MGD and an influent BOD concentration of 250 mg/L, this WWTP consists of a bar screen, a grit channel, Imhoff tank, RBC, a final clarifier, a sludge storage tank and chlorine contact. Secondary sludge from the final clarifier is returned to the Imhoff tanks where the sludge is resettled and anaerobically digested with the primary sludge in the bottom of the tank. Digested sludge is collected in the storage tank and disposed by a Korean contractor. However, USFK/EUSA pays a sewer user fee for the Yongsan WWTP, and Korean regulations do not require secondary treatment of the wastewater.

The Camp Humphreys DPW operates the Camp Humphreys WWTP, which treats wastewater produced by the industrial and residential complexes of Camp Humphreys. The plant was designed for a flow of 0.5 MGD and discharges into

an enclosed lake, which receives intermittent discharge. Currently, the daily flow rate into the plant is 0.65 MGD. The plant configuration consists of an Imhoff tank, RBC, a final clarifier, sludge drying beds, and chlorine contact. After anaerobic digestion in the Imhoff tank, sludge is dried on the sludge-drying beds. The present estimate of sludge production is 350 dry kg/day. The sludge-drying beds have a total surface area of 14,480 sq ft (1345 m²). Dried sludge is removed and disposed by a Korean contractor. Currently, the Camp Humphreys' DPW spends \$19,213 annually for removal and disposal of sludge.

The Camp Casey DPW operates the Camp Casey WWTP, which treats wastewater produced by Camp Casey, a typical troop installation. Designed for a flow of 1.45 MGD, this WWTP currently handles 2.0 MGD and discharges into Casey Creek. The plant consists of three primary clarifiers, two RBC trains with six stages each, three secondary clarifiers, a dissolved air flotation thickener and an aerobic digester. Vacuum assisted drying beds are currently under construction. Sludge is collected and disposed by a Korean contractor.

Technical Options for Improved USFK/EUSA Biosolids Management

Sludge management consists of the following major steps: thickening, stabilization, conditioning, dewatering, and beneficial use or disposal. These steps should be compatible with each other, and the overall system management should be integrated to minimize total costs. This section briefly summarizes technical options for each plant and recommends strategies to improve USFK/EUSA sludge management.

Western Corridor

Technical options considered for the Western Corridor's WWTPs must be capable of producing higher quality biosolids, including greater solids content, than the current aerobic digesters. Aerobic digestion is listed as a *Process to Significantly Reduce Pathogens (PSRP)* in Appendix B of 40 CFR, Part 503. Using aerobic digestion as a PSRP, biosolids must be agitated with either air or oxygen to maintain aerobic conditions with the mean cell residence time and temperature between 40 days at 20 °C and 60 days at 15 °C. Since aerobic digestion is only capable of meeting Class B requirements, site restrictions would be applied. A process that could meet Class A requirements is more desirable. The option explored for the Western Corridor DPW is a mobile

mechanical dewatering system followed by either alkaline stabilization or composting.

Mobile Mechanical Dewatering

The mobile dewatering system would be designed to service all seven WWTPs in the Western Corridor with the capacity to collect from each plant two to three times per month. Such a service would include trailer-mounted equipment, provision of technicians and operators to run the dewatering device, and any required dewatering aids (e.g., polymer). Operational costs include polymer, maintenance, transportation, and power. Water must also be provided for mixing the polymer. All dewatered sludge would be transported to a single location (i.e., regional facility) where either an alkaline stabilization or a composting facility would be located.

Dewatering devices explored for this purpose include a belt filter press, a fixed-volume filter press, and solid bowl centrifuges. In a belt filter press, water is squeezed from the cake by sandwiching biosolids between two filter belts and exerting pressure using rollers. Belt filter presses are the most common dewatering choice, especially for small wastewater treatment plants, i.e., less than 5 MGD. Using a polymer, belt filter presses are capable of producing sludge cake with 16 to 35 percent solids (Black and Veatch 1995). Appendix A to this report includes further information on a belt filter press from Frontier Technology, Inc.

A fixed-volume filter press consists of a series of metal or heavy plastic plates that have filter media lining their sides. Slurry is pushed through the plates and pressure is released when the filtrate flow gets small. The plates are separated and dried cake falls off the plates. This option requires continuous operator attention since the press operates in batch and the operator may need to scrape the cake from the filter plates. (This may not be a concern if a mobile system is used since mobile system operation requires the operator to be present continuously.) The possible solids content of the final product ranges from 30 to 60 percent (Black and Veatch 1995). Appendix B provides information on a filter press from JWI.

Solid bowl centrifuges rely on centrifugal force and the density differences in liquid and solid portions of the sludge to separate them. Centrifuges are the most economical choice to install at large treatment plants, i.e., greater than 50 MGD, but are not usually economical for small treatment plants. Conventional centrifuges achieve between 15 and 25 percent solids. High-solids centrifuges

are capable of achieving between 20 and 32 percent solids, depending on the type of sludge. However, when compared to conventional centrifuges, high-solids centrifuges have a higher capital cost and use double the electricity (Black and Veatch 1995). Appendixes C and D give more information on centrifuges.

The characteristics of the sludge may be important in choosing the most appropriate dewatering option. Western Corridor needs to have its sludge tested in each option to ensure that it is possible to achieve 20 percent solids or greater. Most manufacturers perform these tests free of charge.

Alkaline Stabilization

Advanced alkaline stabilization combines lime stabilization with pasteurization to achieve Class A biosolids. During lime stabilization, quicklime is added to the sludge. The exothermic reaction of the quicklime with water raises the temperature to 50 °C, which is high enough to inactivate worm eggs, and raises the pH above 12 to kill any pathogens (Metcalf and Eddy 1991). Lime stabilization meets PSRP requirements listed in Appendix B, 40 CFR, Part 503. Advanced alkaline stabilization uses the principles of lime stabilization while also achieving pasteurization. The PFRP requirement for pasteurization is to maintain the temperature of the biosolids at 70 °C or higher for 30 minutes or longer. Most advanced alkaline stabilization processes are proprietary, and the ways in which pasteurization is accomplished differ. Chemicals may be added in addition to the lime to achieve pasteurization. These chemicals may include cement kiln dust, lime kiln dust, Portland cement, or fly ash. A high heat regime may also be used to achieve pasteurization.

Lime stabilization provides no direct reduction of organic matter. Thus, the quantity of sludge produced is not reduced as it would be in a biological stabilization process (USEPA 1979). A larger sludge volume will be a concern for the Western Corridor if the Korean government does not allow land application of sludge. Increasing the quantity of sludge by adding lime will dilute the concentration of metals in the sludge. If land application is allowed, this may be an advantage when meeting the Korean regulations for metals in soil.

Two proprietary alkaline stabilization processes were studied for the treatment of Western Corridor sludge. The first, the N-Viro process, is a patented system that can meet PFRP requirements. Technically, the process is defined as an "advanced alkaline stabilization with subsequent accelerated drying." Two alternative methods of conducting the N-Viro process have been approved by the USEPA as PFRP equivalent processes. In the first process, alkaline materials

are added to and mixed with the sludge in sufficient quantity to achieve a pH of 12.0 or greater for at least 7 days. For example, Burnham et al. (1992) used 35 percent kiln dust and a small amount of quicklime. Following mixing, the alkaline-stabilized sludge is dried in windrows for at least 30 days and until a minimum solids concentration of at least 65 percent is achieved. In the second process, a pH greater than 12.0 is maintained for at least 72 hours while the sludge is heated to a temperature of at least 53 °C, and maintained at that temperature for at least 12 hours. The Western Corridor will windrow-stabilize biosolids rather than heat drying. Information provided by N-Viro International Corporation is in Appendix E.

CemenTech, Inc. provides a lime/high heat stabilization process, which has been approved by the USEPA as a process to produce Class A biosolids. In this process, the temperature of the sludge is raised to 70 °C for 30 minutes and the pH is raised to 12 for 2 hours and 11.5 for an additional 22 hours. In the Western Corridor's case, manual operating controls will be used due to the very small quantity of sludge produced. Normally, lime is provided to the system from a bulk material silo, but the Western Corridor does not require enough alkaline material to need a silo. Bagged lime would be used instead. Both these factors lower the cost of the system when compared to most alkaline stabilization systems. Appendix F includes more information on CemenTech.

Fresh alkaline stabilization soil has been shown to inhibit seed germination. Any or all of the following soil characteristics may be responsible: high soluble salts, free NH_3 , fatty acids, and pH. Testing performed at Ohio State University show that a passive storage period of at least 6 months is required before seed germination will occur in N-Viro soil. The tests also showed that the odor of the soil changed from a cement-like smell to that of a moist field soil by the seventh month (Logan et al. 1995). Thus, curing of biosolids for at least 6 months is necessary to achieve a desirable land applicable soil.

Ammonia odors are typically encountered at alkaline stabilization facilities. The elevated pH resulting from the addition of alkaline materials causes the dissolved ammonia in the liquid to be released as a gas. Odor control systems can be chosen from simple enhanced ventilation with a single scrubber to a three-stage system, packed tower/mist scrubber/packed tower. The latter system may use sulfuric acid, sodium hypochlorite, and sodium hydroxide to neutralize and oxidize the odor-causing compounds (WEF 1995a). Alkaline stabilization does have an advantage over other sludge treatment processes that have odor problems in addition to ammonia. The pH is sufficiently high so that hydrogen sulfide odors will not be present (Lue-Hing 1992). In addition,

alkaline stabilization destroys the organisms involved in decomposition of organic matter, which otherwise would cause odor.

Operator safety is a concern with alkaline stabilization. If adequate ventilation is not provided, operators may need to wear respirators due to the ammonia vapors released. In addition, alkaline material creates a caustic dust that causes skin and eye irritation. This is of special concern if bagged lime is used.

Composting

Composting is an aerobic sludge stabilization process. The heat generated from biochemical reactions destroys pathogens, and the humus-like end product can be used as soil amendment meeting Class A requirements of Part 503 regulations. In composting, where temperatures reach the thermophilic range, practically all viral, bacterial, and parasitic pathogens are eliminated (WEF 1995a).

Historically, composting has been more of an art than a science. About 50 years ago, several mechanical composting systems were introduced in Europe. The static pile method was introduced by the U.S. Department of Agriculture in the 1970s. Many advances were made in composting based on this early work (WEF 1995b). Almost 300 WWTPs in the United States either currently use or plan to use composting for their sludge stabilization (Goldstein and Steuteville 1996).

The objectives of composting are to: (1) reduce pathogens to meet PFRP requirements in Part 503 regulations; (2) further stabilize biosolids by decomposing odor-producing compounds; (3) dry the biosolids; and (4) produce a marketable product. The major factors affecting composting processes include biosolids and amendment characteristics (solids content, carbon-to-nitrogen (C/N) ratio, particle size and shape, porosity, biodegradability, and energy content), initial mix ratios, aeration rates, temperature, and detention time (WEF 1995b).

Aeration must be provided during the composting process to satisfy the oxygen demand of organic decomposition, to remove moisture and to control the temperature. The air flow rate for forced aeration composting is governed by temperature control, which is the most critical and most easily measured of the three air functions. During the early stages of composting, the temperature of the composting mass is the critical operational parameter. As the compost matures, moisture levels decrease to a point where the need to retain moisture becomes more of a concern than temperature control. At this point, forced

aeration of the compost should be limited. Turning of compost piles can be a more effective way to control temperature. As a rule of thumb, aeration demands for temperature control should be approximately 0.2 to 0.25 standard m^3/ton (WEF 1995b).

Before composting, a mix is formed with the dewatered sludge cake and a bulking agent. The bulking agent provides structural integrity, is a source of carbon, and increases porosity while also increasing the solids content. To allow adequate structural integrity along with porosity and free space, bulking the initial total solids concentration to 40 percent is recommended. The bulking agent is a combination of an organic amendment and recycled compost (Lue-Hing et al. 1992). A higher concentration of recycled compost is economical in that less amendment needs to be purchased. However, too high a recycled concentration in the bulking agent will result in reduced porosity in the mix. A wide variety of organic amendments have been used: wood chips, sawdust, shredded yard wastes, processed agricultural wastes, earthworms, and shredded tires. Lang and Jager (1993) reported that some amendments such as wood ash suppress compost odors. Reducing particle size increases surface area and thereby enhances composting rates because the optimum conditions of decomposition occur on the surfaces of organic materials. However, reducing particle size reduces the pore size, limiting the movement of oxygen required for composting. Thus, an optimum range of particle size exists, depending on the method of aeration used. Coarse amendments can be recovered in post processing, typically by screening. Benedict (1986) indicated that compost screening typically results in the recovery of 65 to 85 percent of wood chips entering the composting process.

Carbon and nitrogen, the principal nutrients in composting, affect the process speed and final volume of the compost. C/N ratios, also referred to as the biodegradable C/N, between 20 and 50 have been cited as optimum. Low C/N ratios (less than 20) result in a loss of excess nitrogen from ammonia volatilization (Haug 1993). In severe cases of nitrogen deficiency, the addition of urea or other nitrogen sources may be required (Kulhman 1990). High C/N ratios (greater than 80) result in a slowing of decomposition rate and subsequent reduction of composting temperatures (WEF 1990). Municipal sludges generally contain adequate nutrients to support composting (Haug 1993).

Composting is performed in two phases, a high rate phase followed by a curing phase. The high rate phase has higher oxygen transfer rates, higher (thermophilic) temperatures, higher biodegradable volatile solids reductions, and higher odor potential than the curing phase. The curing phase is less

controlled and often has fewer design considerations. However, it is equally as important as the high rate phase (Haug 1993). If space is limiting, the bulking agent may be screened from the compost before curing.

The most common types of composting processes used are the in-vessel process, the windrow process, and the aerated static pile process. In-vessel composting processes are proprietary while aerated static pile and windrow composting processes have to be designed by an engineer. Usually, while any of the three processes may be used for the high rate composting phase, the curing phase is either static pile or windrow (Haug 1993).

In the in-vessel composting process, the mixture is fed into one end of a silo, tunnel, or open channel and moved continuously toward the discharge end where it is outloaded after the required detention time. The mixture may move as an undisturbed plug, or be periodically agitated as it is moved through the vessel. Air is forced through the mixture. A retention time of 21 days followed by 30 days of curing is needed. Appendix G gives further information on an in-vessel composting process from Davis Industries.

In the windrow process, the mixture is stacked in trapezoidal windrows with sufficient ratio of surface area to volume to provide aeration by natural convection and diffusion. The windrow is remixed periodically by a mechanical aerator, such as an auger, to further aerate. Smaller facilities may use the same front end loader that is used to build the windrows to turn them. Using a front end loader to turn the windrows allows the operator to pile the windrow higher than mechanical aerators allow. This will reduce the required land area (Roberts 1997). This would be a more cost effective option for the Western Corridor than buying a large and expensive turning machine. Appendix H contains information on a compost turner from Resource Recovery Systems. The amendments are typically of a smaller particle size than with aerated static pile and may include recirculated compost. The active windrow composting period is around 30 days. In the aerated windrow process, the natural convection and diffusion provided in the windrow process are supplemented by forced aeration. Air is supplied through trenches in the paved working surface.

Presently, 43 percent of the composting facilities in the United States use aerated static pile systems (Goldstein and Steuteville 1996). This type of composting has been widely applied for wet substrates, such as sludge cake (Haug 1993). In this process, approximately 1 ft of bulking agent is stacked over a porous bed above air piping that is connected to blowers. The cake/bulking agent mixture is piled over the bulking agent. The piles are covered with a layer

of either bulking agent or finished compost to provide insulation and to capture odor (Story 1997). Air is provided to the pile either through positive aeration or negative aeration, i.e., air is either forced upward or drawn downward through the mixture. When the pile is taken down after composting, the bulking agent may be partially recovered by screening and then reused. Compost from the aerated static pile is usually not dry enough to be screened. Thus, either a curing or a separate drying phase may be needed before screening.

An advantage of the aerated static pile is its low labor requirement. The operator will need only to check the temperature daily and adjust the air flow to the pile, if necessary. All other associated operator tasks are performed periodically (Story 1997). A disadvantage of the aerated static pile is clumping of compost caused by incomplete mixing and nonaerated parts of the pile. Front end loaders may not mix the compost uniformly and may compact the compost, reducing pore size. This can lead to anaerobic conditions that result in odors and inadequate decomposition and pathogen destruction to achieve Class A biosolids. However, operators who were interviewed for this report had no problems with the quality of the compost (Hutchinson 1997; Story 1997). Appendix I contains transcripts from these interviews. An active composting period of 21 days followed by 30 days of curing is required.

When choosing a bulking agent for aerated static piles, the optimum particle size range is between 12.5 and 50 mm (0.5 and 2 in). Use of a larger bulking agent maintains air voids without the need of periodic agitation, as in the windrow process (Haug 1993). For example, sawdust will not provide enough air cavities for proper aeration and heat flow. Wood chips are most commonly used for aerated static pile bulking agent. Using the correct mix ratio is essential in reaching thermophilic temperatures. When starting up a facility, the operator may need to experiment until the correct ratio is found (Hutchinson 1997). For example, a North Carolina facility at Burnsville was able to maintain temperatures between 150 °F (65 °C) and 160 °F (71 °C) for at least 15 days using a mix ratio of 2:1, tree bark: sludge (Story 1997).

The USEPA (1993) established minimum requirements for composting as a PFRP in Appendix B of Part 503 regulations: (1) using either the within-vessel composting method or the aerated static pile composting method, the temperature of the biosolids is maintained at 55 °C or higher for 3 days; and (2) using the windrow composting method, the temperature for biosolids is maintained at 55 °C or higher for 15 days or longer. During the period when the compost is maintained at 55 °C or higher, the windrow is turned a minimum of every 5 days. Appendix B of Part 503 regulations also established minimum

requirements for composting as a PSRP. The biosolids temperature must be raised to 40 °C or higher for 5 days and during 4 hours of that period, the temperature in the pile must exceed 55 °C. This requirement applies to all three types of composting. The Western Corridor's goal is to meet the PFRP requirements.

Odor control is an important aspect of successful composting operation. In-vessel composting facilities suppress odors better than the other processes due to the nature of the enclosed "reactor." Proper mixing is essential for odor control since unmixed sludge clumps can lead to anaerobic conditions (Benedict et al. 1986). The treatment methods for compost odors include wet chemical scrubbing and regenerative absorption (WEF 1995a). In the aerated static pile method, pile cover material acts as an odor scrubber during positive aeration. Negative aeration, however, requires a separate exhaust scrubber system (Benedict et al. 1986). Biofilters using compost and bulking agents have become more popular for odor treatment at composting facilities in the United States.

Condensate and leachate from the composting pile need to be collected and treated. Condensate forms when the moist, hot exhaust gas is cooled (Haug 1993). A composting facility for the Western Corridor would need to be located at one of the WWTPs where pipes could carry runoff from the piles back to the headworks.

Structures to house the composting process provide protection from the weather and play a critical role in odor control. Depending on the circumstances, a structure may only have a roof or it may have walls. For example, the Fort Collins, CO facility has three walls in addition to a roof due to high winds (Putnam 1997). Wind will carry odor from the composting facility. Rain reduces the solids content in the compost, and thus, the composting time must be increased. In the winter, snow and cold temperatures may cause the compost temperature to fall below the Part 503 requirements. The Springville, UT windrow facility, which does not have a shelter, has not been able to maintain their temperatures at high enough levels to meet requirements. In addition, when the snow melts in the spring, the windrows become too wet and the fecal coliform requirements are not met (Roberts 1997). Current aerated static pile facilities that operate without shelters do not experience any problems detrimental to the quality of the compost. The layer of bulking agent over the pile acts as an odor filter and provides insulation from the elements to keep the pile temperature above levels required for pathogen destruction (Story 1997; Steuteville and Goldstein 1997). In Korea, a shelter may not be required, but should be considered due to the volume of rain in the summer months.

Numerous testing methods exist for measuring compost stability. No single test is accepted universally (Jimenez and Garcia). These test methods (WEF 1995a; Haug) include: testing for percent volatile solids, using a respiration test to measure carbon dioxide or oxygen demand, measuring for a C/N ratio less than 20 for manure compost, seed germination and root elongation tests, and measuring redox potential.

Cost Comparison

Table 4 provides rough cost estimates for mechanical dewatering systems. Information on each of these systems is provided in Appendixes A-D. A truck to haul the dewatering trailer is not included in any of the prices quoted and should be considered in final cost decisions. Another addition to the cost of any item purchased in the United States is shipping to Korea. Since a trailer adds to the cost of the system, the Western Corridor may want to consider installing the dewatering system at the stabilization facility and hauling the sludge to that plant before dewatering. Typical annual operations and maintenance (O&M) costs range from \$5,000 to \$12,000.

Table 5 contains prices for composting and alkaline stabilization processes. Information on each of these processes is provided in Appendixes E-I. Comparison between each figure in Table 5 is difficult for several reasons. The in-vessel composting and alkaline stabilization processes are proprietary, and the companies provided figures based on an estimate of the quantity of sludge that is produced by the Western Corridor. The aerated static pile figures were obtained by an author via phone interviews with city officials and plant operators. The interviewed composting facilities were chosen because they handle quantities of sludge similar to that handled by the Western Corridor. The Burnsville, NC facility has no shelter, and the facility already owned a front

Table 4. Cost comparison of mechanical dewatering systems.

Dewatering Device	Hyd. Cap. (gpm)	Device Price	Trailer Price	Total System Cost	Percent Total Solids
Frontier Technology, 0.5 m Belt Filter Press	11-20	\$85,000 (skid mounted)		\$105,000 (w/trailer)	20-32
JWI J-Press 100 PSI STD				\$258,000 (w/trailer)	
Sharples Solid Bowl Centrifuge Model PM-38000	50	\$160,000	\$250,000	\$410,000	>16
Trimax Environmental (Centrifuge)		\$50,000- \$100,000	\$10,000- \$20,000	\$150,000- \$200,000	30-35

Table 5. Cost comparison of different composting processes and alkaline stabilization.

Process	Company/facility	Equipment included	Annual O&M Costs	Total Process Cost	Percent Total Solids
Aerated Static Pile Composting	Burnsville, NC	Entire facility	Not significant above rest of WWTP	\$80,000	
	Go Wanda, NY	Conversion of existing drying beds to asp	\$20,000	\$30,000	50-60
In-vessel Composting	Davis Industries, Inc.	Econobay	\$8,499	\$410,000	50-60
Alkaline Stabilization	CemenTech	Model CSP-5		\$59,877	
	N-Viro		\$38,060	\$617,614	62

end loader and other required machinery. The Western Corridor owns a front end loader also. However, if the Western Corridor needs a shelter or additional machinery, the construction cost will be higher than the price quoted in Table 5.

The Springville, UT facility is the only windrow facility that was interviewed. The Springville construction cost of \$250,000 is not quoted in Table 5 because it would not be representative for the Western Corridor since the facility was built for 2 dry tons/day. A price of \$130,000 was quoted on a compost turner from Resource Recovery Systems of Nebraska, Inc. The Western Corridor may decide to use its front end loader in lieu of purchasing a compost turner, however. Windrows are not piled as high as aerated static piles (Haug 1993). Thus, more land area would be required for a windrow facility versus an aerated static pile facility. Aerated static pile has the added cost of air piping and blowers, however. In comparison with the operations and maintenance expenses at an aerated static pile facility, a windrow facility will require more labor due to pile turning, but less energy requirements since blowers are not used. For the purposes of this report, it has been assumed that the construction and operation and maintenance of a windrow facility for the Western Corridor will cost no more than that of an aerated static pile facility.

The total costs of the two alkaline stabilization facilities are difficult to compare. The estimate provided for the N-Viro process by the company was for a 1 dry ton per day facility. The cost was scaled down to a 0.37 dt/d facility by the authors. Thus, the number quoted in Table 5 may not be representative of the actual cost. The N-Viro quote includes site work, construction costs, engineering fees, and a technology fee, none of which are included in the CemenTech quote. The CemenTech quote covers only the basics required for alkaline stabilization.

As stated previously, the Western Corridor currently spends \$90,737 annually on sludge disposal. Assuming that the sludge produced from any of the stabilization processes above can be land applied, a 5-year savings of \$453,685 will be achieved. The following combinations could be used to achieve a 5-year payback:

- CemenTech alkaline stabilization, and a Frontier Technology belt filter press
- aerated static pile composting, and any dewatering option except Sharples with a trailer and JWI J-Press
- windrow composting, and any dewatering option except Sharples with a trailer and JWI J-Press.

These combinations were calculated using an O&M cost of \$12,000/yr for all the dewatering devices, \$20,000/yr O&M, and \$80,000 construction cost for aerated static pile composting, and assuming that, over a 5-year period, windrow composting would cost less than aerated static pile composting, if a front loader were used instead of a compost turner. All other prices were taken from Table 5 as shown.

If the produced biosolids cannot be land applied, the Western Corridor should still consider the processes above. The solids content will be increased dramatically above that of the current aerobically digested sludge that is landfilled. The following sludge volumes were calculated for each process:

- dewatering to 20 percent solids: 166,686 gal/yr
- composting to 50 percent solids: 66,674 gal/yr
- alkaline stabilization to 40 percent solids: 96,700 gal/yr.

A comparison of these volumes to the current sludge volume of 1,333,488 gal/yr shows significant reduction. The tipping fees will be increased, however, due to greater solids content. It is believed that, with the reduced volume and increased fees, the sludge disposal fees for composting and alkaline stabilization will be within 5 percent of the current disposal fees.

Sludge collection/disposal costs are expected to rise sharply in a few years. This study recommends the Western Corridor continue using current procedures and implement the mobile mechanical dewatering system with either aerated static pile composting, windrow composting, or alkaline stabilization when disposal costs significantly rise. The belt filter press is the most suitable dewatering option due to economics. However, before a final decision is made on the

dewatering technology, Western Corridor should have its sludge tested in the various dewatering devices. A greater volume of sludge will be produced from alkaline stabilization than from composting. Thus, if land application is not permitted, aerated static pile or windrow composting will be the more cost effective option. Windrow composting should not be chosen over aerated static pile due to the believed lower costs. Careful consideration should be taken as to how much labor the Western Corridor wishes to expend on stabilization. Aerated static piles are well suited for small treatment plants. Each WWTP has an unique approach, as may be seen from the interviewed composting facilities, and capital costs vary from a few tens of thousand to millions of dollars. It is extremely important that engineers/operators take an active interest in improving sludge management system before any new technology is implemented.

Yongsan

Due to space restriction, a sludge treatment program cannot be implemented at the Yongsan WWTP. However, the need for a sludge treatment program can easily be eliminated at the plant. Currently, the Korean Ministry of Environment does not require secondary treatment at the Yongsan WWTP, and USFK/EUSA pays a wastewater system users fee to the Korean Government. Therefore, it is recommended that RBC operation be halted and the Imhoff tank effluent be directly discharged to Seoul's sewer system. This will result in significant reduction of disposal costs for the secondary treatment sludge from RBCs.

Camp Humphreys

Upgrading the existing sludge drying beds to reed beds is the option considered for Camp Humphreys. Sand-drying beds can have long dewatering times (2 to 4 weeks), intensive labor requirements to remove dried sludge, and can experience clogging. Camp Humphreys WWTP has actually experienced clogging and poor drainage. Reed beds may be a more cost effective technology at this site by virtue of its added microbial degradation and by lesser requirement for operator attention.

Although it was started in Europe more than 10 years ago, reed bed dewatering is still an emerging technology in the United States and a new technology in Korea. Reed bed technology has been largely used in the northeastern United

States, including New Jersey, Pennsylvania, Maine, and Vermont. Like sand-drying beds, the reed bed is a natural dewatering system that is well suited for smaller treatment plants. A disadvantage with such natural systems is the greater requirement for available land. This will only be a concern at Camp Humphrey if the current sludge drying beds do not provide enough area. The reed bed process can produce biosolids with a solids content ranging from 30 to 60 percent (Kim et al. 1993). USACERL has experience with the implementation and operation of reed bed technology through a demonstration at Fort Campbell, KY.

The reed bed process basically operates as a modified sand-drying bed with a dense growth of reed vegetation. Therefore, the construction is similar to that of sand-drying beds. An excavated trench is first lined with an impermeable barrier to prevent leaching to the surrounding soil. Precast Hypalon liners have been successfully demonstrated for lining the trenches at several installations. A 10-in. layer of gravel is placed over the drainage pipe and is then covered with a 10-in. layer of sand. The side walls are commonly made of concrete and include at least 1 m freeboard. This freeboard ensures adequate storage capacity of the sludge for a design period of 10 years. Camp Humphreys' current drying beds may easily be converted to reed beds by raising the side walls. A door, or some other means to facilitate the removal of dried biosolids, also needs to be constructed in each bed.

Once the beds are constructed, reeds are planted at 1-ft centers. Several species are available, but generally the common reed *Phragmites* is used. *Phragmites* is well suited for reed bed use because of its elevated evapotranspiration rate and its great tolerance for variable climates. In fact, on a visit to Korea, *Phragmites* was found in the Han River banks. Once the reeds are established, sludge may be applied to the beds. Reed beds are designed to accommodate stabilized sludge that contains 3 to 4 percent solids.

Reed beds have some important advantages over other natural systems. The dried sludge removed at the end of bed is very similar in quality to compost with regards to pathogen content and stabilization. These results are mainly due to the long detention of the sludge, added microbial degradation due to oxygen provided through the root system, and an additional storage period that follows the final sludge addition. While not yet documented, it is believed that, if the sludge is allowed to weather for 1 year following the last sludge application, it will pass the EQ biosolids criteria. The root system of the reeds enables long term storage through evapotranspiration and maintenance of a pathway for the liquid to drain through.

Reed beds require very little operator attention in comparison with sand-drying beds. Typical operator attention is 200 hours per year to monitor sludge additions and to perform other miscellaneous tasks. Labor requirements for sand-drying beds range from 0.5 hr/yr/m², for large systems, to 4 hr/yr/m², for small systems (USEPA 1987). Thus, for the current sand-drying bed area (1345 m²) at Camp Humphreys, the operators may spend between 672.5 and 5,380 hours per year working on the sand-drying beds. Unlike sand beds, which require the removal of the sludge after each individual sludge application, reed beds are designed to hold sludge for a period of 10 years. The time and cost of periodic replacing of sand torn up during sludge removal would be eliminated. One relevant manpower requirement is harvesting of the reeds each fall. Harvesting may be performed manually with hedge clippers or sickles or using mechanical devices. Alternately, the reeds may be burned after filling the bed with 2 in. of water, if local authorities permit.

At the time of disposal, the final volume is significantly lower than the total volume from a sand bed after 10 years, which results in disposal savings. Several ultimate disposal alternatives are available for the sludge after it is removed from the beds. It is likely that the weathering of the sludge over the storage period will result in Class A biosolids. Therefore, under U.S. standards, the material could be as freely used as any commercial soil conditioner, in a manner similar to compost. In the worst case, the biosolids would meet the Class B standards and could still be beneficially applied to land. The solids content of over 40 percent would facilitate ease of application. Landfilling of the sludge remains an alternative. Since the volume of sludge would be reduced through organic destruction, landfilling would be less expensive than currently practiced.

The reed bed has a few disadvantages or potential problems. One commonly occurring problem with the reed bed is infestation, especially by aphids, during the first year of growth. This problem is typically controlled by purchasing lady bugs, a natural predator of the aphids. Another problem that must be considered is the removal and extinction of the reed system from the final compost product. This may possibly be addressed by killing the reeds at the beginning of the 1-year holding period and screening the final product. Another potential disadvantage is the preparation period before the reed bed becomes fully operational. Reeds must be planted during the growing season. The establishment of healthy reeds requires several weeks of growth. Sludge should not be applied until the plants are well established. Some sites have waited up to 2 months before applying sludge (Kim et al. 1993).

The reed bed process is an empirical technology. Further science-based research is needed to "fine tune" this technology. Design parameters for reed bed sizing are widespread based on the number of variables that affect the dewatering rate. Also, data from existing reed bed facilities varies significantly. Experience at Fort Campbell indicates that approximately 20,000 sq ft of reed bed area is required per 1 MGD of wastewater flow when anaerobic digestion is used for stabilization (Kim et al. 1993). This would correspond to 13,000 sq ft (1208 m²) for the Camp Humphreys WWTP. The solids loading rate must also be considered, though. Solids loading rates for operational reed bed systems using anaerobically digested sludge with 5 percent total solids range between 2.5 and 12 lb/sq ft/yr (12 and 58.6 kg/m²/yr) (Kim et al. 1993). For Camp Humphreys' present estimated solids production of 350 dry kg/day, a reed bed area between 19,300 and 94,184 sq ft (1792 and 8750 m²) is required. The hydraulic loading rate may also be considered. Hydraulic loading rates for operational reed bed systems using anaerobically digested sludge with 5 percent total solids range between 0.49 and 3.28 cu ft/sq ft/yr (0.15 and 1.0 m³/m²/yr) (Kim et al. 1993). For Camp Humphreys, a reed bed area between 22,150 and 147,700 sq ft (2058 and 13,720 m²) is required. These ranges of possible required space illustrate that a good estimate of the requirements for Camp Humphreys is not feasible without more data on sludge characteristics and volume. The solids and hydraulic loading rate estimates are based on typical values for conventional anaerobic digesters. No data is available for Imhoff tank sludge. In addition to the required bed space, at least two extra beds need to be built to allow a reed bed to remain idle the year prior to its excavation and for emergencies. Thus, even at the 13,000 sq ft approximation, which is below the low end of the both loading rate approximations, the current 14,480 sq ft may not be adequate since the additional space for two extra beds is not available.

Costs of implementing reed beds vary as much as the design parameters. Retrofitting existing sand-drying beds to reed beds range in cost from \$0.45/sq ft to \$9.30/sq ft. If Camp Humphreys had only to retrofit the existing beds, implementing this option would be ideal. However, construction of new reed beds is quite costly in comparison, with a range from \$9.33/sq ft to \$25/sq ft (Kim et al. 1993). Without an in-depth analysis of Camp Humphreys' sludge and construction costs in Korea, an exact construction cost cannot be calculated. However, assuming that the cost of retrofitting Camp Humphreys' sand beds to reed beds would be \$4.88/sq ft, the DPW would spend \$70,660 to implement this change, which is within the 5-year payback criteria. This study recommends the conversion of Camp Humphreys' current sand-drying beds to reed beds.

Camp Casey

The options explored for the Camp Casey WWTP include: (1) upgrading the current aerobic digester to autothermal thermophilic aerobic digestion (ATAD) with land application, and (2) maintaining the existing aerobic digester with the vacuum-assisted bed currently under construction followed by either composting or alkaline stabilization. The current aerobic digester is larger than required and loses energy. A more efficient process is desirable. In addition, as mentioned earlier, conventional aerobic digestion is not capable of producing Class A biosolids. However, implementing composting or alkaline stabilization would also produce Class A biosolids. This is important since the final biosolids products may be reused at golf course or training area rehabilitation projects on Camp Casey grounds.

Autothermal thermophilic aerobic digestion (ATAD) was developed by Pöpel in the 1970s in Germany. In 1977, Herr Fuchs installed the first German ATAD system in Vilsbiburg. Fuchs system is the most commonly used ATAD system in the Federal Republic of Germany (FRG) and probably in the world. Currently, ATAD facilities are successfully being operated in FRG, the United Kingdom, France, Italy, Switzerland, and Canada. Since 1993, when Part 503 came into effect, ATAD has emerged in the United States as a technology capable of meeting PFRP requirements. Currently, Krüger, Inc. has 12 operating ATAD systems in the United States with five more under construction.

ATAD is a compact, fully enclosed process which, with an adequate supply of oxygen, microorganisms, and nutrients, will decompose complex organic substances in wastewater. The heat produced during decomposition is adequate to maintain the desired operating temperature. Thus, ATAD is more efficient than aerobic digestion since no external heat supply is required. This results in lower operation and maintenance costs. ATAD does, however, require energy for aeration and mixing as aerobic digestion does. ATAD achieves a greater reduction of bacteria and pathogens than aerobic digestion in about one fifth the time. Removal rates of up to 70 percent of the biodegradable organics are achievable in thermophilic aerobic digestion (Metcalf and Eddy 1991). When comparing ATAD to other sludge management strategies, advantages include no nitrification and no required chemical additions or amendments.

The ATAD process works well with both primary and secondary sludges and may be operated on either a semi-continuous or a batch basis. Typically, a batch system is used. Since ATAD systems rely on heat to achieve the operating temperature, sludge must be thickened prior to entering the digester to limit

energy needed for heating and mixing. Ideal conditions are obtained when the sludge is thickened to 4 to 6 percent total suspended solids (TSS) (USEPA 1990) and has a chemical oxygen demand of 40 mg/L or greater (WEF 1995a). Camp Casey currently has a dissolved air flotation unit that is capable of meeting the 4 to 6 percent TSS requirement.

The current digester at Camp Casey would be replaced with a minimum of two insulated reactors in series. While single reactor processes do achieve similar reduction in volatile suspended solids, they will not achieve the required pathogen reduction. Temperature and pH parameters vary between the two reactors. The first reactor should maintain a temperature between 35 and 50 °C and a pH greater than or equal to 7.2 while the second reactor maintains a temperature between 50 and 65 °C with a pH around 8. Desired temperatures are acquired through adequately thickened sludge, good reactor insulation, efficient aeration, and foam management. Since the thermophilic operating temperatures in the reactors suppress nitrification, the pH usually will not have to be specially considered during design.

Biosolids treated through ATAD meet the requirements for Class A pathogen reduction in Part 503. Thermophilic aerobic digestion is one of the PFRPs listed in Appendix B of 40 CFR Part 503. To meet these requirements liquid biosolids must be agitated with air or oxygen to maintain aerobic conditions with a mean cell residence time of 10 days at 55 to 60 °C. In addition, Kelly (1993) showed that ATAD reduces volatile solids by 38 percent in a system with a degree C-day product of 400 and a 7-day total retention time. Thus, ATAD is capable of meeting both the Class A and the VAR requirements to create exceptional quality biosolids. ATAD is ideal over aerobic digestion in that Class A instead of Class B requirements are met.

Aerating at the appropriate rate is important. If air is supplied at a higher rate than needed, evaporative latent heat loss will cause cooling in the tank. Inadequate aeration and/or mixing causes poor digestion and a musty or humus-like odor in the exhaust (Kelly 1993). This odor can be sufficiently controlled by returning exhaust air to the rotating biological contactors, water scrubbing, passing through a biofilter, or dilution with ambient air. Gaseous ammonia, which is released by thermophilic aerobic degradation, also releases odor. The elevated pH in the second reactor enhances the stripping of ammonia in the exhaust. Various aeration and mixing devices have been used including aspirating aerators, turbines, and diffused air.

A dense foam layer develops quickly on the reactor due to aeration of the substrate and plays an important part in the ATAD system. Wolinski (1985) reported that the foam layer enhances biological activity, improves oxygen use, and provides insulation to the reactor. However, foam also retards the volume of air entering the reactor (USEPA 1990). Thus, foam volume must be controlled. Methods of foam control include mechanical horizontal shaft foam cutter, vertical mixers and spray systems, and chemical defoamers.

Post treatment of the biosolids includes cooling and thickening. Twenty days of cooling is desirable to reduce the temperature to 20 °C. Post thickening is most successful after the sludge is allowed to cool. Thickening of ATAD biosolids by gravity will typically achieve 6 to 10 percent solids (USEPA 1990).

To completely install an ATAD system, the Camp Casey DPW would spend around a million dollars. Annual operations and maintenance costs would be \$33,800. Over 5 years, the Camp Casey DPW would spend roughly \$1,182,000 on an ATAD for Camp Casey's sludge management. Exact information on the operation and maintenance costs for the plant's current aerobic digester and sludge disposal costs are needed to prove whether a 5-year return on investment is attainable in this situation. It is assumed that a 5-year payback is not possible. However, conversion of the aerobic digester to an ATAD system is a project that most likely would achieve a 10-year return on investment.

Sludge disposal costs are expected to rise significantly in the near future based on rapidly changing Korean environmental regulations and the high inflation rate. This study recommends that, when such a time arrives, upgrading the existing aerobic digester to an ATAD system with land application be compared to the addition of either composting or alkaline stabilization in conjunction with the facility's current processes, and that one of these options be implemented. The final biosolids product will be used as soil amendments at Camp Casey golf courses and for training area land management/erosion control.

4 Conclusions and Recommendations

Conclusions

It is hoped that this study will open a new era in USFK/EUSA sludge management where beneficial use of biosolids replaces landfill disposal. However, regulatory and economic barriers may make this a difficult task. Since no biosolids regulations or practices currently exist in Korea, the management improvements discussed in this report are based on Part 503 criteria for beneficial land application of biosolids. It is assumed that biosolids that meet Part 503 regulations may be land applied at USFK/EUSA installations. The USFK/EUSA Environmental Program Office recommended a 5-year payback as a criteria to compete with other real property improvement projects. This study concludes that, even considering the economic benefits of using processed biosolids as soil amendments, a 5-year payback is currently a difficult criteria to meet. However, an increase in sludge disposal costs is foreseen. At that time, the recommendations in this report should be implemented.

Recommendations

This study recommends that:

1. The Western Corridor DPW use a mobile mechanical dewatering device to dewater sludge at its seven plants, transport the sludge to a regional facility for stabilization, and install either aerated static pile composting, windrow composting, or alkaline stabilization at the regional facility.
2. The USFK/EUSA discontinue the current secondary treatment at the Yongsan WWTP to reduce operation costs and sludge generation.
3. The Camp Humphreys DPW convert the current sand-drying beds at the Camp Humphreys WWTP to reed beds. This conversion requires low capital investment and can be accomplished with in-house labor.

4. The Camp Casey DPW set a long-term goal to convert the aerobic digester to an ATAD system and, after dewatering in the vacuum-assisted bed, the biosolids be used as soil supplements at Camp Casey's golf course and training land management/erosion control.

Appendix G interview data show the wide variety of approaches and costs to implementing improved biosolids management. It is strongly recommended that USFK/EUSA engineers/operators start implementing improved sludge management strategies in the very near future for the benefit of both Korea and the United States.

References

- Benedict, H., E. Epstein, and J. English, "Municipal Sludge Composting Technology Evaluation," *Journal of Water Pollut. Control Fed.*, vol 58 (1986), p 279.
- Black and Veatch, and The Electric Power Research Institute, *Wastewater Biosolids and Water Residuals: Reference Manual on Conditioning, Thickening, Dewatering and Drying* (Kansas City, MO, 1995).
- Burnham, J., N. Hatfield, G.F. Bennet, and T.J. Logan, *Use of Kiln Dust With Quicklime for Effective Municipal Sludge Treatment With Pasteurization and Stabilization With the N-Viro Soil Process*, ASTM Stand. Tech. Publication 1135 (American Society for Testing and Materials [ASTM], Philadelphia, PA, 1992).
- Goldstein, N., and R. Steuteville, "Biocycle Survey: Steady Climb for Biosolids Composting," *Biocycle* (1996), pp 68-78.
- Haug, R., *The Practical Handbook of Compost Engineering* (CRC Press, Boca Raton, FL, 1993).
- Hutchinson, M., Phone interview with author, 24 April 1997.
- Jimenez, E., and V. Garcia, "Evaluation of City Refuse Compost Maturity: A Review," *Biol. Wastes*, vol 27 (1989), p 115.
- Kelly, H.G., H. Melcer, and D.S. Mavinic, "Autothermal Thermophilic Aerobic Digestion of Municipal Sludges: A One-Year, Full-Scale Demonstration Project," *Water Environment Research*, vol 65, No. 7 (1993), p 849.
- Kim, B.J., R.R. Cardenas, and S.P. Chennupati, *An Evaluation of Reed Bed Technology To Dewater Army Wastewater Treatment Plant Sludge*, Technical Report (TR) EP-93/09/ADA273500 (U.S. Army Construction Engineering Research Laboratories [USACERL], 1993).
- Kuhlman, L.R., "Windrow Composting of Agricultural and Municipal Wastes," *Resources, Conservation and Recycling*, vol 4, No. 151 (1990), p 160.
- Lang, M., and R. Jager, "Compost Marketing in New England," *Biocycle*, vol 34, No. 8 (1993), p 78.
- Logan, T.J., B.J. Harrison, L.E. Goins, and N. Hatfield, "Soil Substitute From Alkaline Stabilization," *Biocycle*, vol 36, No. 9 (1995), p 80.
- Lue-Hing, C., D. Zenz, and R. Kuchenrither, eds., *Municipal Sludge Management: Processing, Utilization and Disposal* (Technomic Publishing Co., Inc., Lancaster, PA, 1992).
- Metcalf and Eddy, Inc., *Wastewater Engineering: Treatment, Disposal, and Reuse*, 3d ed. (McGraw Hill, Inc., New York, 1991).

- Putnam, S., Phone interview with author, 15 April 1997.
- Roberts, R., Phone interview with author, 13 May 1997.
- Rudolfs, W., "Sewage Sludge as Fertilizer," *Soil Sci.*, vol 26 (1997), p 455.
- Story, T., Phone interview with author, 23 April 1997.
- Steuteville, R., and N. Goldstein, "Compost Structure Options," *Biocycle*, vol 38, No. 2 (1997), pp 58-62.
- United States Environmental Protection Agency (USEPA), *Process Design Manual: Sludge Treatment and Disposal*, EPA 625/1-79-011 (USEPA ORD, Cincinnati, OH, 1979).
- USEPA, *Design Manual: Dewatering Municipal Wastewater Sludges*, EPA/625/1-87/014 (USEPA ORD, Cincinnati, OH, 1987).
- USEPA, *Environmental Regulations and Technology: Autothermal Thermophilic Aerobic Digestion of Municipal Wastewater Sludge*, EPA/625/10-90/007 (USEPA ORD, Washington, DC, 1990).
- USEPA, 40 CFR Part 503, *The Standards for the Use or Disposal of Sewage Sludge*, FR 58 (1993), pp 9248-9404.
- Water Environment Federation (WEF), *Operation of Municipal Wastewater Treatment Plants*, Manual of Practice No. 11 (WEF, Alexandria, VA, 1990).
- WEF, *Wastewater Residuals Stabilization*, Manual of Practice FD-9 (WEF, Alexandria, VA, 1995a).
- WEF, *Biosolids Composting, A Special Publication* (Residuals Subcommittee of the Technical Practice Committee, WEF, Alexandria, VA, 1995b).
- Wolinski, W.K., "Aerobic Thermophilic Sludge Stabilization Using Air," *J. Water Pollut. Control*, vol 57 (1985), p 433.

Abbreviations and Acronyms

APLR	Annual Pollutant Loading Rate
ATAD	Autothermal Thermophilic Aerobic Digestion
C/N ratio	Carbon-to-Nitrogen Ratio
CFU	Colony Forming Unit
CPLR	Cumulative Pollutant Loading Rate
DPW	Directorate of Public Works
EQ	Exceptional Quality
EUSA	Eighth United States Army
FRG	Federal Republic of Germany
MGD	Million Gallons per Day
MPN	Most Probable Number
O&M	Operation and Maintenance
PC	Pollutant Concentration
PCB	Polychlorinated Biphenyl

PFRP	Process to Further Reduce Pathogens
PSRP	Process to Significantly Reduce Pathogens
RBC	Rotating Biological Contactors
SOUR	Specific Oxygen Uptake Rate
TSS	Total Suspended Solids
USACERL	U.S. Army Construction Engineering Research Laboratories
USEPA	U.S. Environmental Protection Agency
USFK	United States Forces, Korea
VAR	Vector Attraction Reduction
WEF	Water Environment Federation
WWTP	Wastewater Treatment Plant

Appendix A: Frontier Technology Belt Filter Press

Note: the following appendixes include information and proposals regarding specific products, provided by commercial manufacturers to USACERL researchers for use in this study. All information cited here remains the property of the cited manufacturers. All data reproduced here is meant to be used for informational purposes only; citation of trade names does not constitute an endorsement or approval of the use of such commercial products. Views or opinions expressed herein do not represent either the views or policies of any agency of the Federal government, including the U.S. Army, the U.S. Army Corps of Engineers, or the U.S. Army Construction Engineering Research Laboratories.

04/07/1997 12:02 6166739629

FRONTIER TECH.

PAGE 01

**FAX Transmission**

From: Elisebeth Haluch Frontier Technology
Questions? Call 616/673-9464 609 N. Eastern Ave.
Fax 616/673-9629 Allegan, MI 49010
To: Amy Swanson 217/373-3490
Company: U.S. Army Corps of Engineers
Address:

Date: April 7, 1997

Time: 10:22 AM

Pages: 2 (including this one)

CC:

Amy,

Here is the budget pricing you requested for a mobile unit to dewater sludge at the following design and production rates.

The design flow rate of 0.73 million gallons per day. Sludge production of 91.25 lb of d.s. per hour on an 8 hour day to achieve 20 % solids during dewatering.

- | | | |
|----|---|--------------|
| 1. | 1/2 Meter Skid mounted Belt filter press system | \$85,000.00 |
| 2. | 1/2 Meter Trailer mounted Belt Filter System | \$105,000.00 |
| 3. | 0.8 Meter Trailer mounted system | \$153,000.00 |

Both the 1/2 meter Belt presses process between 11-20 gpm of sludge. The .8 meter press can process between 25-40 gpm of sludge.

Could you please let me know when you plan on taking this project to the bidding process? Please let me know if I can be of further assistance or answer any questions.

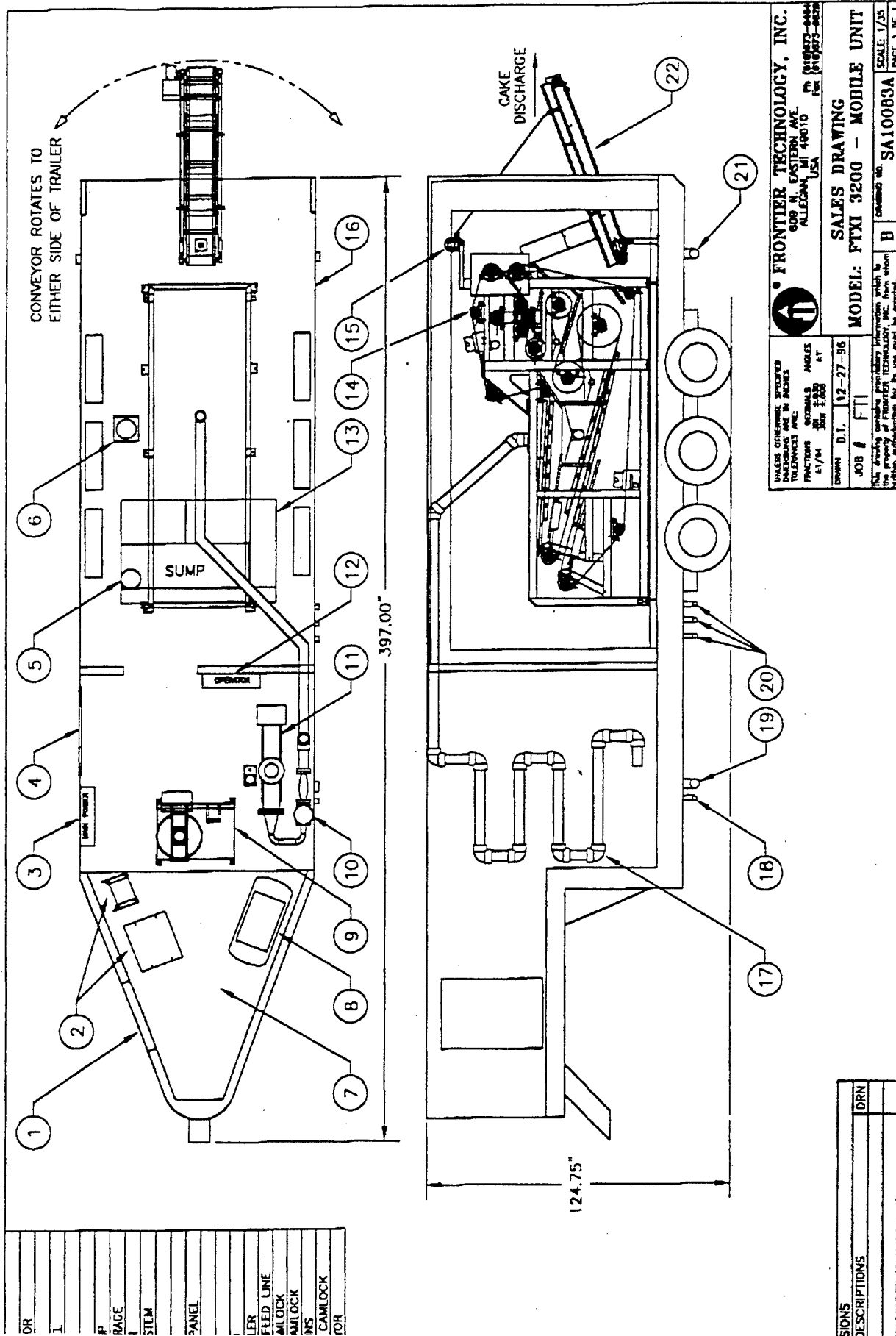
Best Regards,

Elisebeth Haluch

04/07/1997 12:02 6166739629

FRONTIER TECH.

PAGE 02



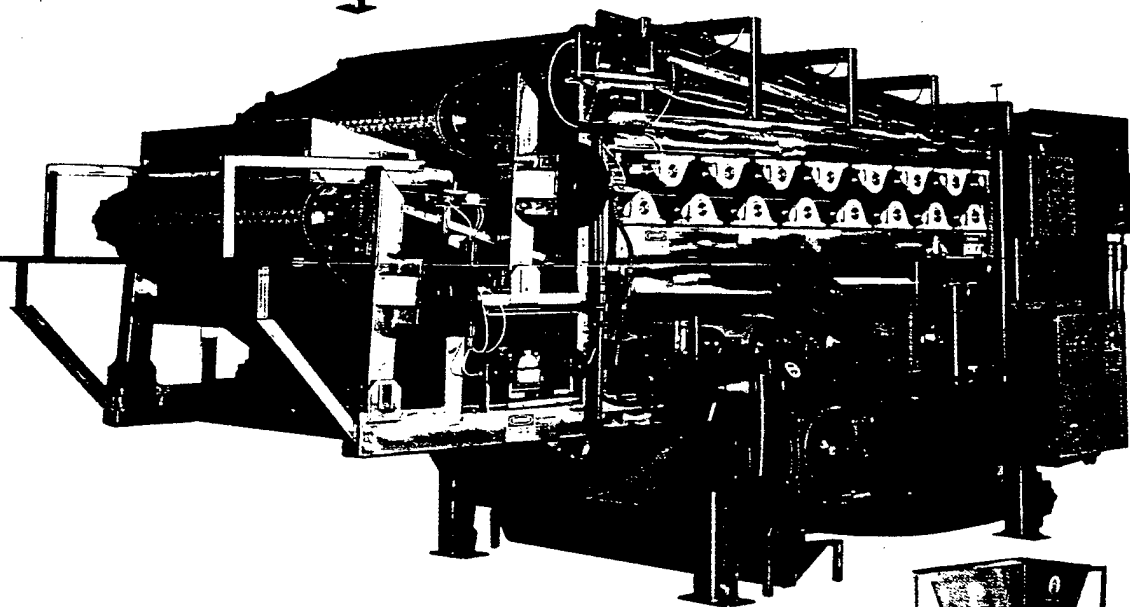
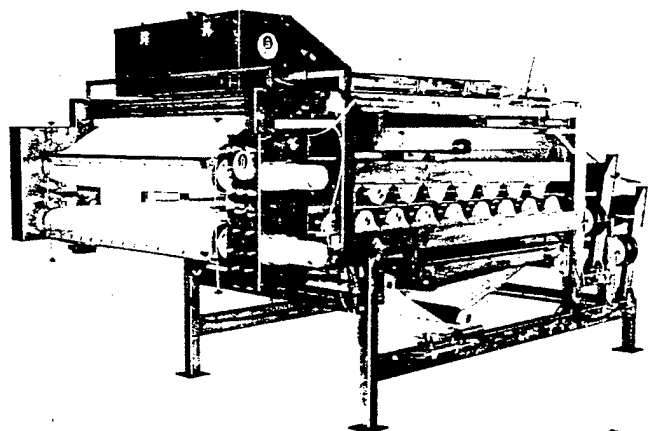
ITEM	DESCRIPTION
1	UPPER ACCESS DO
2	TRANSFORMERS
3	MAIN POWER PANI
4	SIDE DOOR
5	SUMP PUMP
6	WASH WATER PUM
7	UPPER DECK - SIDE
8	AIR COMPRESSOR
9	POLYMER MIXING ST
10	PINGH VALVE
11	SLUDGE PUMP
12	OPERATOR CONTROL
13	SUMP
14	BELT PRESS
15	ELECTRIC WINCH
16	CURTAIN SIDE TRAI
17	MIXED SLUDGE/POLYMER
18	WATER INLET - 1" C
19	SLUDGE INLET - 3" C
20	SUMP/FLOOR DRA
21	MAIN SUMP DRAIN - 4"
22	DISCHARGE CONVE

DATE	REV.	REV.

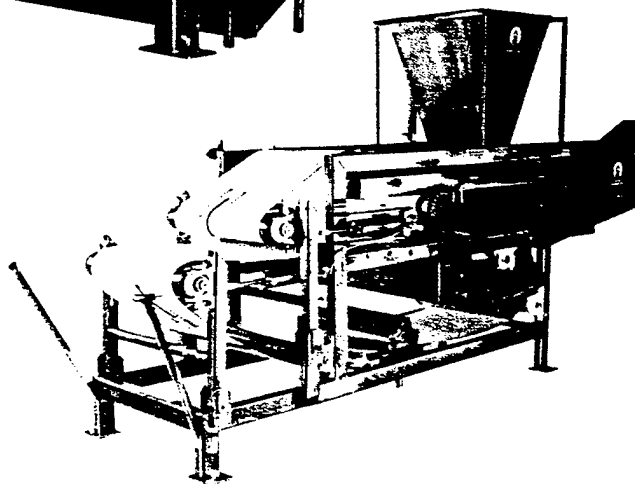
DEWATERING SOLUTIONS



**FTI
Belt Filter
Presses**



**CUSTOM
SOLUTIONS
WITH
ECONOMICAL
RESULTS**





While no two applications are identical, Frontier Technology, Inc. believes in taking an individual approach to your dewatering applications. Working together to go beyond the scope of original objectives with common sense engineering, keeping it simple, efficient and cost effective for capital purchase and operation.

Our broad experience over a wide range of dewatering applications has allowed us to efficiently manufacture continuous dewatering systems to the application for both process and sludge dewatering.

Frontier Technology has made it possible for the highest quality equipment to be built at economical prices solving your dewatering problems for the years to come.

THE COST EFFECTIVE SOLUTION FOR PR

DIFFERING APPROACHES TO EFFICIENT REMOVAL OF SLUDGES/SLURRIES

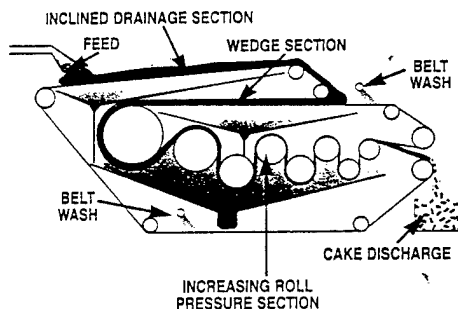
Frontier Technology, tailored Belt Press Dewatering Systems assures you of the right equipment for the application, no one model fits all applications. Time/pressure profiles are designed to meet the application and are adjustable to maximize performance, reducing the cake solids volume to be handled.

Water (moisture) in the sludge or slurry is held in different ways requiring different approaches to the efficient removal. Some applications will require polymers to break the bonding of the liquids/solids in the sludge/slurry, agglomerating the particles,

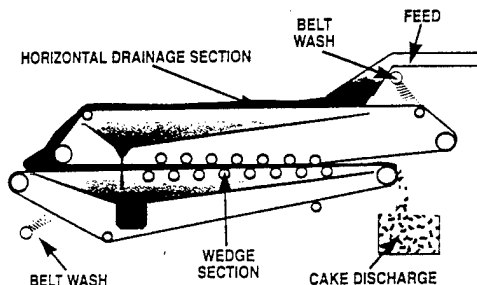
releasing the inter-cellular moisture and allowing the solids to be effectively dewatered. Many other applications however, will not require any polymer addition to be efficiently dewatered, this is much of the time with more fibrous sludges/slurries.

Frontier Technology, users can look forward to high throughput capacities with the highest cake solids, trouble-free operation requiring minimal maintenance, labor savings of continuous operation and superior reliability using the highest quality design and construction.

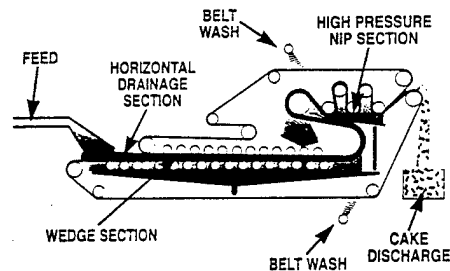
OUR FLEXIBLE CONSTRUCTION DESIGN ALLOWS FOR EASY ADAPTATION TO YOUR SPECIFIC REQUIREMENTS



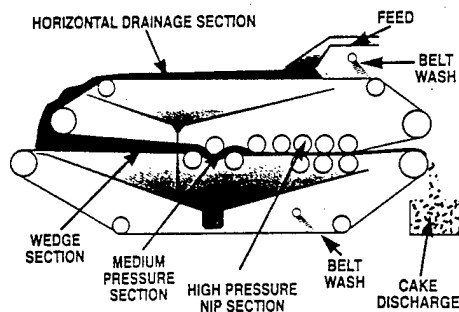
FTXI profile is tailored for delicate sludge such as municipal sludge with low solids in the product feed, utilizing increased filtration area and time under pressure for low polymer use and highest cake solids.



FTWP profile is designed for delicate product dewatering over a wide range of applications with constant automatic pressure control with no shearing pressure applied to difficult-to-dewater product streams.



FTEX profile is tailored for higher solids in the slurry/sludge product stream and fibrous products which require very short drainage time, increased shear pressure to achieve maximum cake dryness.



FTHP profile is used for solids that are not pressure sensitive, dewater rapidly, and can accept nip pressure. Cantilever frame allows for the use of seamless belts which is crucial for high nip roll pressures.

PROCESS DEWATERING AND SLUDGE VOLUME REDUCTION

FEATURES AND BENEFITS

Custom Built To Your Application

Assures you of the right equipment the first time. Saving operating and capital cost, while increasing throughputs and cake solids.

Space Saving Designs

Uses the least amount of floor space, saving building cost without sacrificing throughput capacity or filtration area.

Engineered With Experience

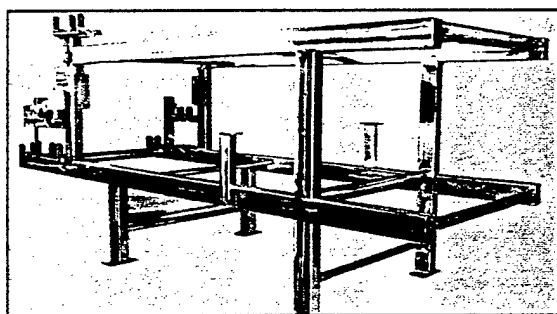
Our experience with many different process and waste applications brings the benefits of maximum corrosion protection, lowest maintenance cost, reduced polymer cost, maximized service life, increased throughputs and highest cake solids.

Highest Quality Construction Materials

Long service life, reduced operating cost, best price value with no shortcuts.

Complete Range Of Sizes

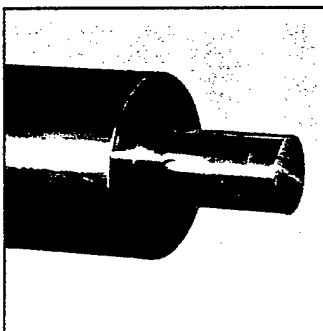
No application too small or too large with sizes ranging from 0.3 meter(12") to 3.2 meters(127")



FRAME

Heavy duty, built to perform with the reliability and dependability you expect with an all welded tubular frame construction in either epoxy coated or all stainless steel construction for maximum corrosion protection and a conservative safety factor is standard for all units. The open frame design allows for easy

cleaning and maintenance, saving valuable time for many years of trouble free operation.



ROLLERS

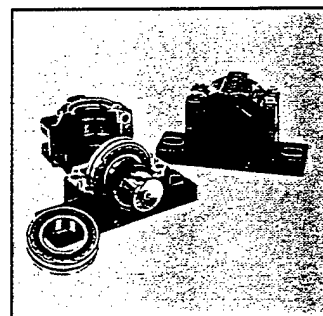
All presses are available with a choice of roll construction and materials used. Many materials are available to meet the particular requirements you may

have. these are rubber coated, nylon coated or all stainless steel construction. Roll deflection is maintained to a minimum for durability and the high stresses encountered during operation.

BEARINGS

All bearings are designed for a minimum of 500,000 hours of B-10 life and are located away from the product for cleaner operation. The split case, triple lip

sealed design bearings provide for the maximum service life requiring only semi-annual lubrication with outstanding moisture protection.



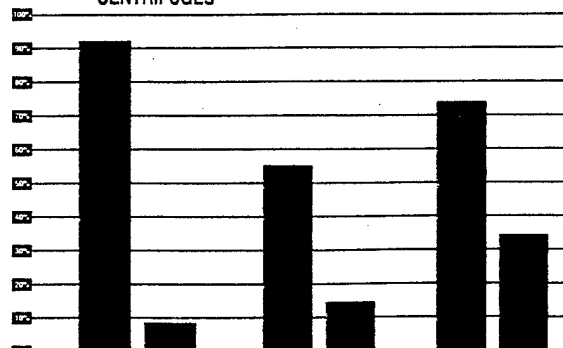
OTHER QUALITY FEATURES

All presses have tension/pressure control by simple pneumatics eliminating the need for a separate hydraulic unit. Stainless steel pans and trays collect and contain all fluids during dewatering of the slurry for a cleaner and safer operation. Adjustable wedge section allows for maximization of filtration area. Gentle inclined gravity drainage section for reduced polymer requirements and higher sludge/slurry throughputs. Maximum number of press rolls for highest cake solids. Twin belt positive drive system for better control and higher cake solids.

UP TO 90%
CAPITAL COST
SAVINGS OVER
USING DRYING BEDS,
CENTRIFUGES

UP TO 2/3
LESS POLYMER
USED OVER
CENTRIFUGES

50% MORE VOLUME
REDUCTION THAN
THICKENING ALONE



FTI BELT PRESSES VS. CENTRIFUGES, DRYING BEDS

OPTIONS TAILORED TO YOUR APPLICATION

Carbon Steel Or Stainless Steel Frames

All Stainless Steel, Rubber Or Nylon Coated Rolls

Time/Pressure Profiles Matched To Your Application

Complete Range Of Sizes

Press Mounted Mechanical Thickeners

Wash Water Reuse System

Skid Mounted Systems

Mobile Systems

For maximum corrosion protection.

Matched to your application

Higher Throughputs and maximum cake dryness.

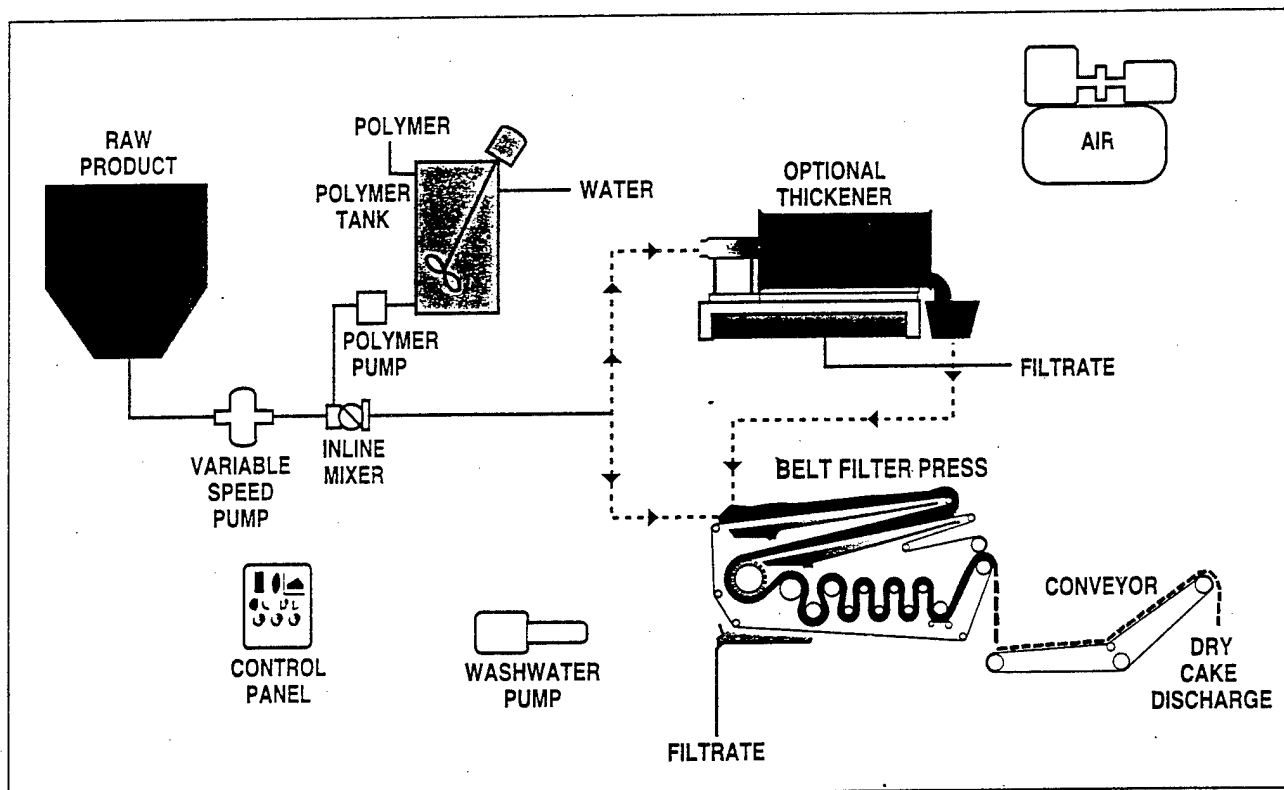
From 0.3 meters (12") to 3.2 meters (127") belt width to match exact capacities required, saving valuable capital dollars.

Gravity belt or rotary screen thickeners mounted on the presses or separately for increased throughputs.

Uses filtrate and or used wash water to clean the belts.

Complete with auxiliary equipment required to do the job.

Trailer mounted with required auxiliary equipment for portable operation.



If your application requires liquid/solid separation we will be glad to start a FREE ANALYSIS showing you the benefits. We also have mobile pilot units that are available for lease that can directly tap into your process or waste stream.

FTI's broad line of liquid/solid separation equipment and systems leaves no room for compromise. You get exactly the right equipment required to do the job right the first time. Working together we collectively find simple process solutions that go beyond the scope of original objectives.

REPRESENTED BY:



FRONTIER TECHNOLOGY, INC.
609 N. EASTERN AVE.
ALLEGAN, MI 49010
PHONE: 616-673-9464
FAX: 616-673-9629

FTI Mobile On-Site Dewatering Systems

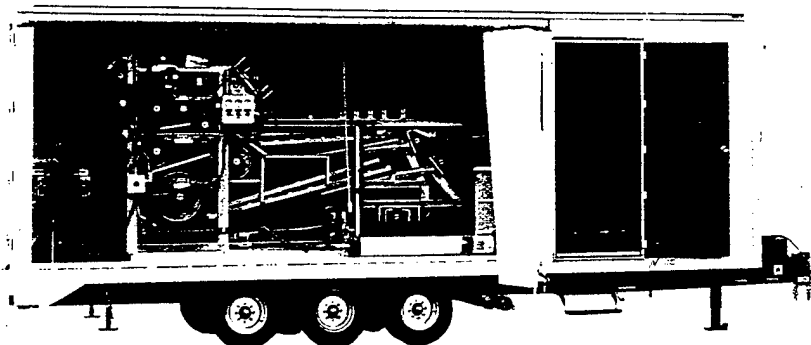


...self-contained, simple, efficient and economical for a full range of applications

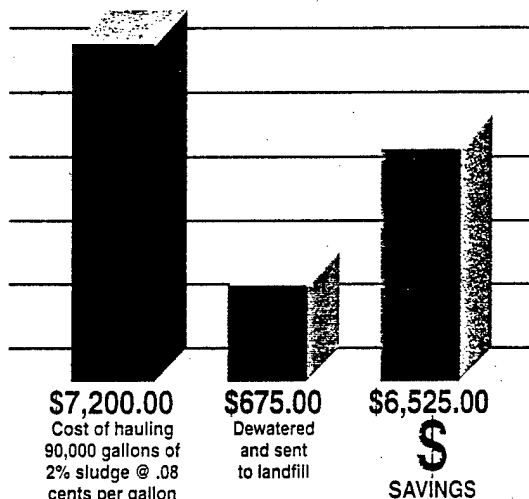
Frontier Technology has the equipment to serve the broadest range of municipal and industrial dewatering needs. Our common sense engineered dewatering systems effectively remove waste and particulate matter from your sludge/slurry wastewater. The resulting dry cake significantly reduces your handling and disposal cost and meets demanding EPA standards.

The self-contained mobile dewatering system offers the flexibility of portable operation with open, partially closed or totally enclosed trailers. These mobile systems are available with the FTI Gravity Belt Thickener or the FTI Belt Filter Press for a simple, cost effective solution, to your solid/liquid separation requirements. These systems can be purchased or rented and are used for many applications and purposes:

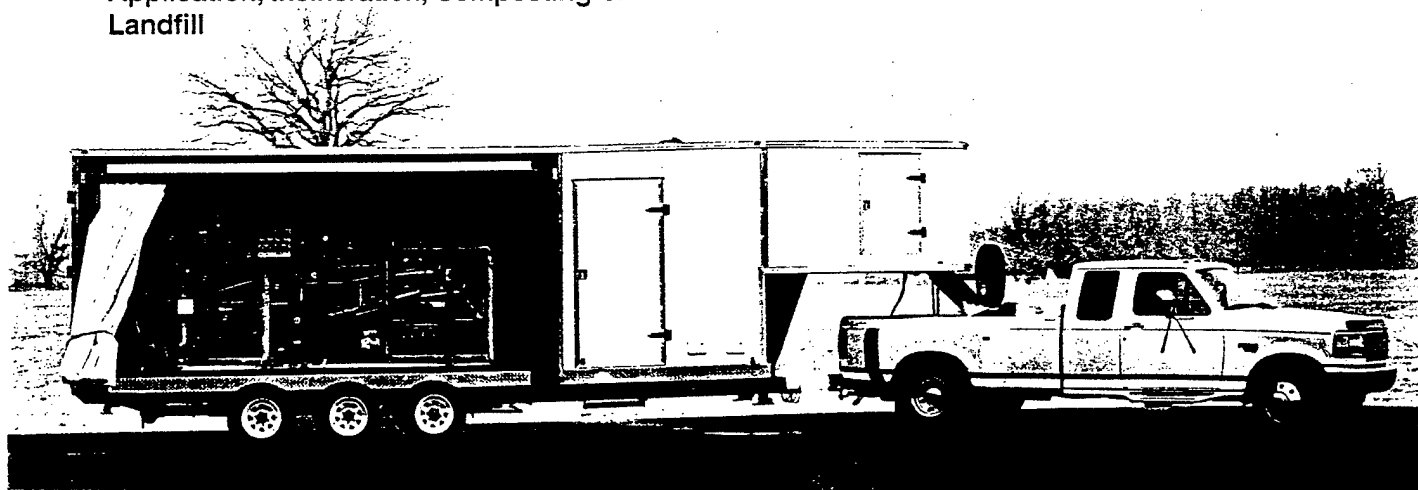
- Contract dewatering- reducing hauling costs
- Dewatering a number of wastewater plants with just one unit
- Temporary sludge volume reduction when storage capacity is full
- Adding dewatering capability without adding expensive building or renovation cost
- Reduce product liability, producing landfillable sludge
- Control of disposal options, Land Application, Incineration, Composting or Landfill



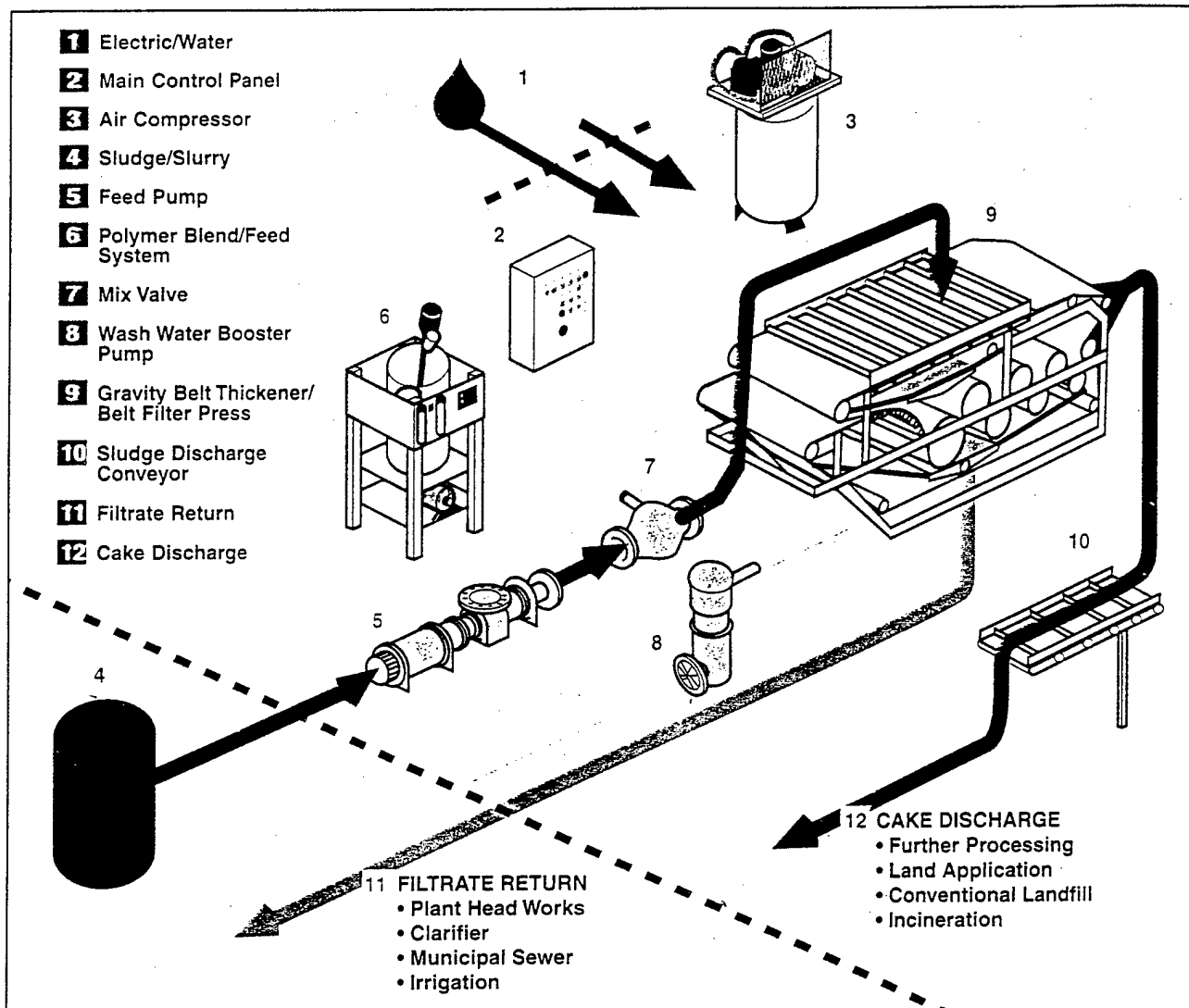
Liquid Hauling/Land Application vs. Dewatering/Landfill



All cost savings are based on actual customer information and include all hauling, labor, tipping fees and chemical used.



Frontier Technology Self-Contained Mobile Dewatering System



Size	Belt Thickener	Belt Press
3200	—	30 - 40
4700	120 - 300	50 - 80
6700	180 - 450	70 - 120
8700	240 - 600	100 - 160
12700	360 - 950	—

Flow rates based on averages and stated in GPM.
 Smaller and custom designed systems available

The FTI models 3200 & 4700 are available in pintle or 5th wheel style trailers, suitable to be pulled with a 1 ton truck or larger. All other sizes are available on semi-trailers. Should an application exist where a trailer is not required, all these systems are available on a skid or as stand alone equipment.

Our lab is available to assist you in the proper equipment selection, ensuring your system will be designed to suit the waste stream.

REPRESENTED BY:



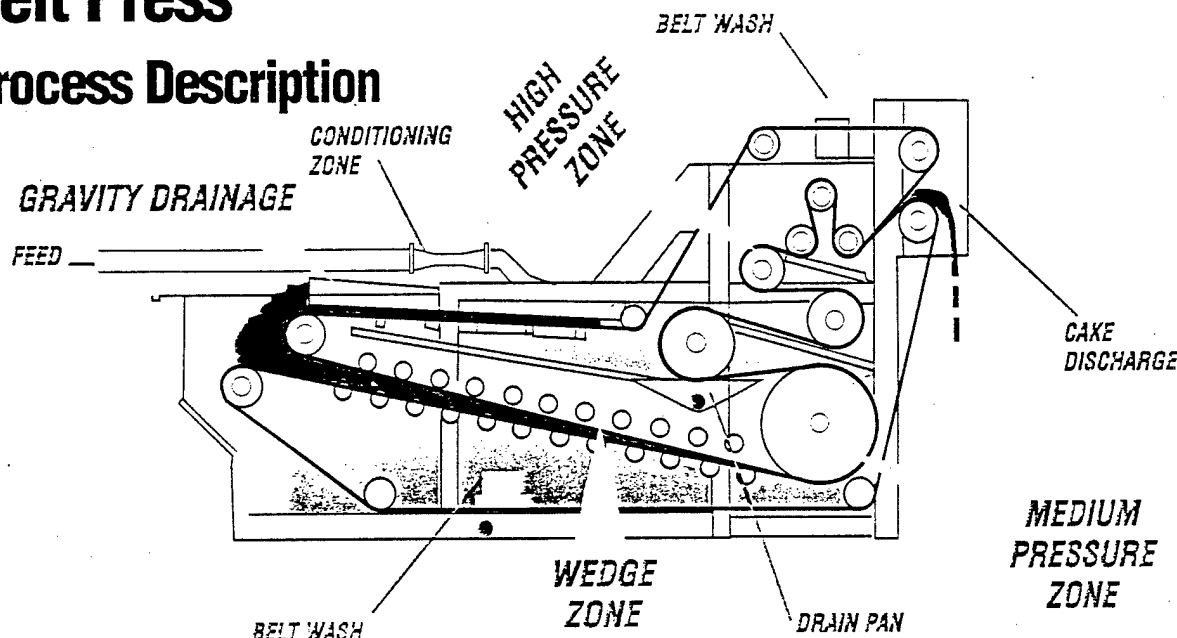
FRONTIER TECHNOLOGY, INC.
 609 N. EASTERN AVE.
 ALLEGAN, MI 49010
 PHONE: 616-673-9464
 FAX: 616-673-9629

609 N. EASTERN AVE. • ALLEGAN, MI 49010 9593 • USA • PHONE: 1-616-673-9464 • FAX: 1-616-673-9629



Belt Press

Process Description

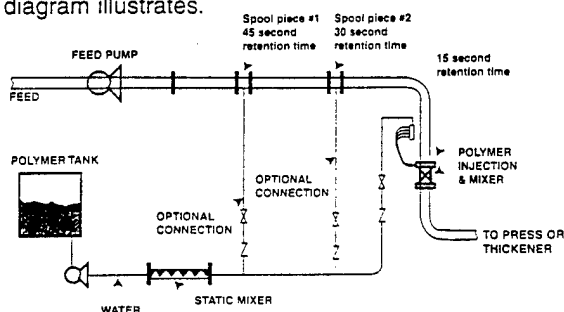


The FTI Belt Press continuously dewateres by the use of two porous belts which are threaded through a series of rollers. There are four specific processes in a belt filter press: conditioning, gravity drainage, low pressure (wedge zone), medium and high pressure (pressure zone).

Conditioning

Conditioning involves the addition of a polymer, inorganic salt, etc. to the slurry. The clumping that results from the flocculation leads to the release of freewater and gives the solid matter the necessary consistency to accommodate pressure filtration.

Different types of conditioning agents are used depending on the slurry's characteristics. The FTI polymer injection ring and mixer is placed into the feed line upstream of the press. This injection ring allows the mixing energy to be varied according to the effect on the formation of the floc. To allow for changes in slurry characteristics, the piping should be designed to allow for 15 second, 30 second and 45 second retention times, as the diagram illustrates.



Gravity Drainage

The slurry enters the belt press from the feed line and onto the belt in the gravity zone. The water from the slurry immediately begins to fall through the porous belt as it moves towards the wedge zone through a series of plows and/or dams.

Wedge Zone

As it moves into the wedge zone, the slurry becomes a loosely structured cake. As the cake proceeds forward, the bottom belt and top belt gradually compress. This forms a wedge that applies low non-shear pressure.

High Pressure Zone

The sandwiched belts move into the medium and high pressure zones through a combination of rollers that decrease in size. Some of these are designed to shear the cake to rearrange and expose the wetter inner cake. At the last shearing roller, the cake is scraped off the belts and is discharged.

The belts separate and each continues moving through the belt wash stations and back to the beginning of the process.

Gravity Belt Thickener's

The belt thickener dewateres using gravity drainage through a porous belt. Conditioning can also be added upstream just as with the belt press, depending on the sludge/slurry and ending solids range between 6 - 10%.

609 N. EASTERN AVE. • ALLEGAN, MI 49010 9593 • USA • PHONE: 1-616-673-9464 • FAX: 1-616-673-9629



Applications Typical Results

The following sizes have been compiled for estimating purposes only and may vary for a specific application. Comparable or better results with similar sludges/slurries can be anticipated. We recommend a lab and/or pilot test, when the pertinent sludge or slurry exist, to confirm degree of dewaterability, polymer consumption, flow rates and capture rates. Please contact Frontier Technology for further information regarding those services.

APPLICATION	AVG. FEED % % DRY SOLIDS	TYP. CAKE % % DRY SOLIDS	THROUGHPUT		POLYMER lbs/ ton DRY SOLIDS	CAPTURE Rate %
			GPM	lbs/d.s./hr/M		
MUNICIPAL						
Primary 100%	2 - 6	26 - 38	80	2,400	4 - 6	96 - 98%
Anaerobic Digested	2 - 5	18 - 26	60	1,500	7 - 10	96 - 98
Aerobic Digested	0.5 - 2	12 - 20	55	550	10 - 14	96 - 98%
Primary/ Secondary 50%/50%	3 - 6	20 - 32	70	2,100	6 - 10	96 - 98%
Waste Activated	1.5 - 3	16 - 24	45	675	8 - 14	96 - 98%
Alum Sludge	1.5 - 3	16 - 22	40	600	5 - 12	96 - 98%
Lime Sludge	3 - 5	38 - 45	50	1,250	2 - 5	96 - 98%
PULP & PAPER						
Primary 100%	2 - 4	38 - 45	80	1,600	2 - 4	96 - 98%
Secondary 100%	1.5 - 3	18 - 25	50	750	4 - 8	96 - 98%
Primary/Secondary 50%/50%	1.5 - 3	20 - 30	60	900	3 - 6	96 - 98%
INDUSTRIAL						
Wet Die Cast Sludge	28 - 30	78 - 82	50	7,600	2 - 4	95 - 97%
Fiberglass Washwater Sludge	4 - 6	38 - 47	70	2,100	1.5 - 3	97 - 98%
Potato Peel Waste	10 - 15	32 - 40	60	4,503	N/A	95 - 97%
Cattle Paunch	12 - 16	36 - 44	50	4,000	N/A	94 - 96%
Meat Processing, Activated	2 - 4	23 - 30	50	1,000	4 - 10	95 - 97%
Canning Sludge, Activated	1 - 3	14 - 22	60	900	3 - 6	95 - 97%
Coal Refuse	20 - 35	60 - 68	50	8,750	1 - 4	95 - 97%

- 1) Cake solids and throughputs are based on standard pressure roll configurations.
2) Design rates will vary in direct proportion to differences in % feed concentration.

- 3) Yields will decrease with a higher proportion of secondary sludge.
4) Numbers listed are expected but can not be guaranteed as this is a function of sludge characteristics, concentration, etc. and other variables involved.

Belt Press Sizing Use for Approximation Only

The following sizes have been compiled for estimating purposes only and may vary for a specific application. Comparable or better results with similar sludges/slurries can be anticipated. We recommend a lab and/or pilot test, when the pertinent sludge or slurry exist, to confirm model to be used, degree of wewaterability, polymer consumption, flow rates and capture rates. Please contact Frontier Technology for further information regarding those services.

APPLICATION	AVG. FEED % % DRY SOLIDS	THROUGHPUT - GPM/ft. D.S. Hr.					
		0.3 m	0.5 m	0.8 m	1.2 m	1.7 m	2.2 m
MUNICIPAL							
Primary 100%	2 - 6	10/300	20/600	40/1,200	80/2,400	120/3,600	160/4,800
Anaerobic Digested	2 - 5	7/187	15/375	30/750	60/1,500	90/2,250	120/3,000
Aerobic Digested	0.5 - 2	6/56	13/112	27/225	55/550	80/825	110/1,100
Primary/ Secondary 50%/50%	3 - 6	8/260	17/525	35/1,050	70/2,100	105/3,150	140/4,200
Waste Activated	1.5 - 3	5/84	11/168	22/337	45/675	65/1,010	90/1,350
PULP & PAPER							
Primary 100%	2 - 4	10/200	20/400	40/800	80/1,600	120/2,400	160/3,200
Secondary 100%	1.5 - 3	6/93	12/187	25/375	50/750	75/1,125	100/1,500
INDUSTRIAL							
Swine Flush Wastewater	1 - 2	7/75	15/150	30/300	60/600	90/900	120/1,200
Potato Peel Waste	10 - 15	7/687	15/1,375	30/2,750	60/4,500	90/6,750	120/9,000
Cattle Paunch	12 - 16	8/500	15/1,000	40/2,000	60/4,000	90/6,000	120/6,000
Meat Processing, Activated	2 - 4	6/125	12/250	25/500	50/1,000	75/1,500	100/2,000
Canning Sludge, Activated	1 - 3	7/112	15/225	30/450	60/900	90/1,350	120/1,800
Coal Refuse	20 - 35	6/1,093	12/2,187	25/4,375	50/8,750	75/13,125	100/17,500
FOOD							
Apples, Juice Processing	N/A	1,300	4,000	10,000	16,000	25,000	30,000
Relish	N/A	1,000	3,000	6,500	10,000	14,000	19,000

- 1) FFFP series of presses is to be used with a gravity thickener or Wedge Press.
2) Designs can vary in proportion to differences in % feed concentration, desired cake solids, sludge/slurry to be dewatered and existing plant equipment.

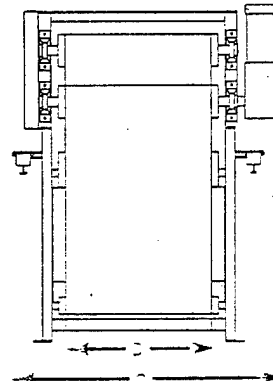
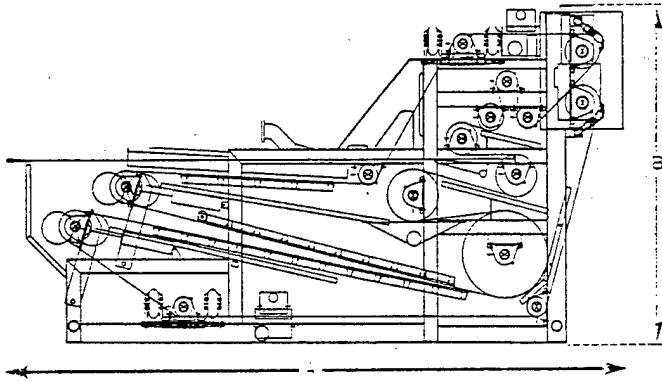
- 3) Flow rates will decrease with a higher proportion of secondary sludge and model used.
4) Numbers listed are expected but can not be guaranteed as this is a function of sludge characteristics, concentration, etc. and other variables involved.

609 N. EASTERN AVE. • ALLEGAN, MI 49010 9593 • USA • PHONE: 1-616-673-9464 • FAX: 1-616-673-9629



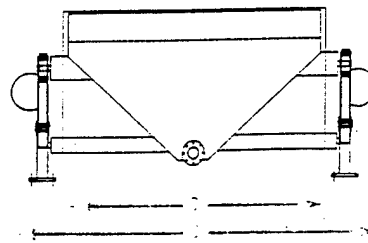
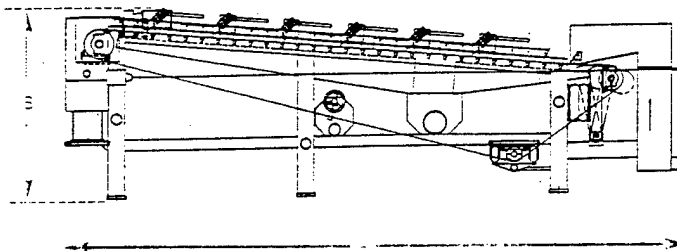
Low Demand Dewatering Equipment

Bed Filter Press — Dimensions



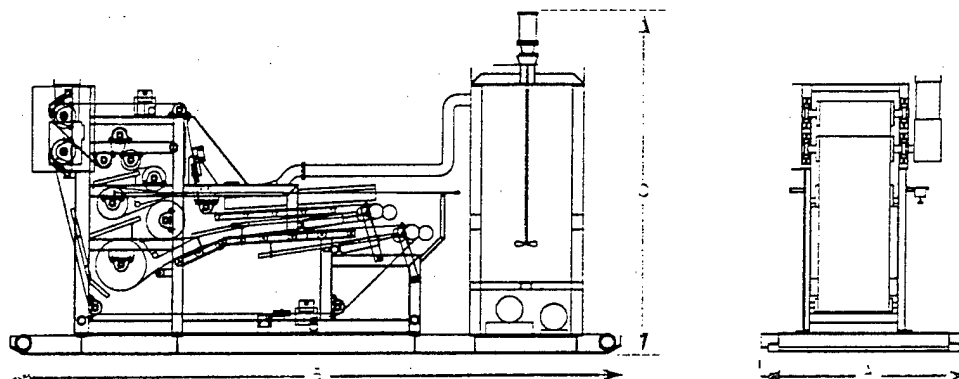
MODEL #	A	B	C	D
FTXL-1200	118"	69"	35"	12"
FTXL-2000	118"	69"	43"	20"
FTXL-3200	140"	70"	59"	32"
FTXL-4700	140"	70"	78"	47"

Gravity Bed Filter Press — Dimensions

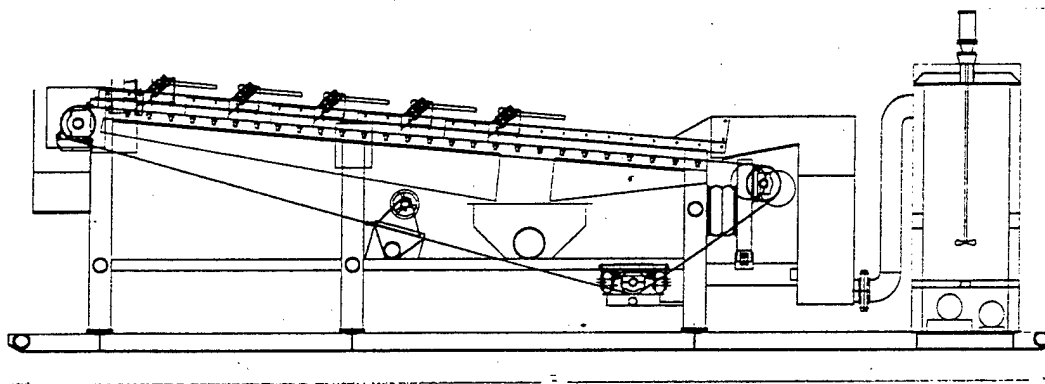


MODEL #	A	B	C	D
FTGB-32	14' 4"	5' 8"	59"	32"
FTGB-47	18' 8"	5' 8"	78"	47"
FTGB-67	18' 8"	5' 8"	102"	67"
FTGB-87	18' 8"	5' 8"	127"	87"
FTGB-127	18' 8"	5' 8"	167"	127"

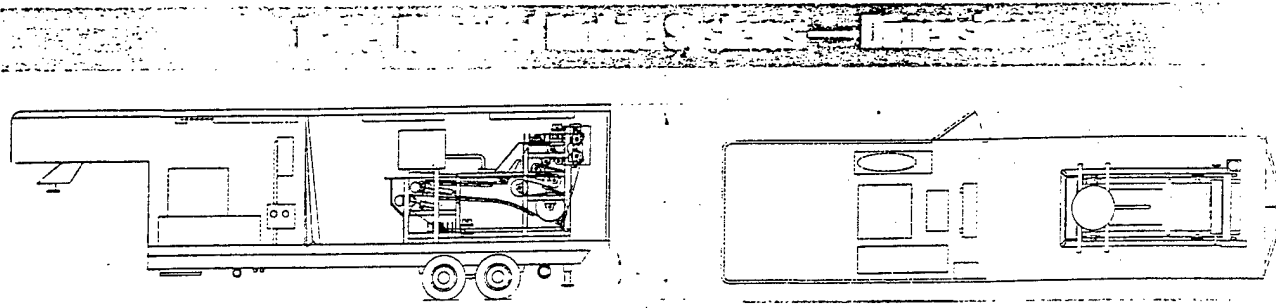
Soil Systems — Dimensions



MODEL #	FTXL 1200	FTXL 2000	FTXL 3200	FTXL 4700	FTXL 6700	FTXL 8700
A	59"	59"	72"	92"	112"	132"
B	166"	166"	200"	200"	230"	230"
C	93"	93"	93"	93"	93"	93"



MODEL #	FTGB 3200	FTGB 4700	FTGB 6700	FTGB 8700	FTGB 12700
A	59"	72"	92"	112"	132"
B	166"	200"	200"	230"	230"
C	93"	93"	93"	93"	93"

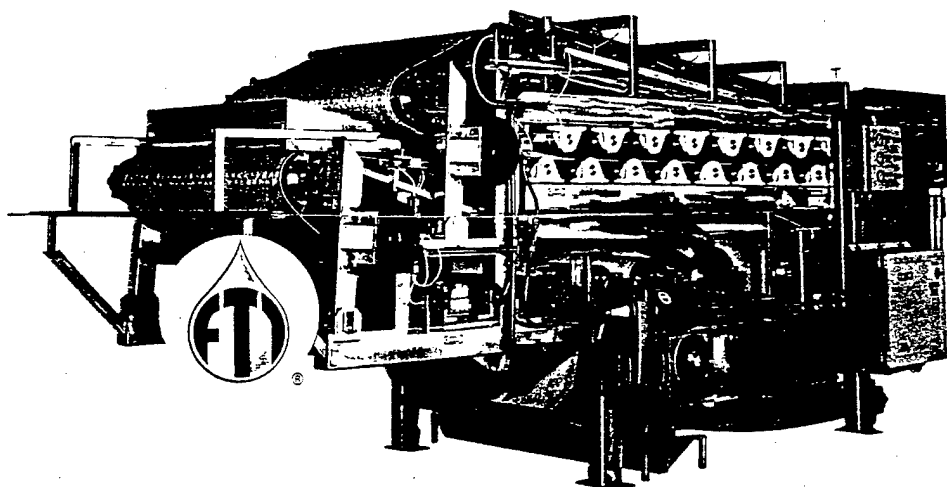


	A	B	C	D	E
FTXL MOBILE	8'	30'	24'	10'	3'

609 N. EASTERN AVE. • ALLEGAN, MI 49010 9593 • USA • PHONE: 1-616-673-9464 • FAX: 1-616-673-9629



Compare price from an overall perspective...



BRAND B BELT PRESS

Point by point... add up the cost savings.

- › 304 Stainless Steel
- › 500,000 hr. Bearings
- › Dual Drive Rolls
- › 3-year Warranty
- › Large Gravity Drainage Zone
- › Long Wedge Zone
- › Maximum Pressure Contact

*Compared
To*

- Carbon Steel
- 100,000 hr.
- Single Drive
- 1-year Warranty

Unequaled Quality through Common Sense Design

- ✓ **More Hydraulic Capacity**
- ✓ **More Dry Solids per Hour**
- ✓ **Lower Polymer Consumption**
- ✓ **Less Maintenance**
- ✓ **Longer Service Life**



*"Simple, effective, efficient solutions
to your Liquid/Solid Separation needs."*

Appendix B: JWI J-Press

JWI. 2155 112th Avenue, Holland, Michigan 49424-9604 U.S.A. • Telephone (616) 772-9011 • Fax (616) 772-4516



JWI PORTABLE DEWATERING TRAILER-MOUNTED FILTER PRESS

(100 PSI - Standard)

APPLICATION OF EQUIPMENT

The proposed system is designed to accept sludge from a lagoon or waste treatment process for dewatering. A 108-cubic-foot capacity filter press is mounted to a commercial semi-trailer for easy transportation between dewatering sites.

EQUIPMENT TO BE SUPPLIED WITH FILTER PRESS TRAILER UNIT

- A. Filter press with semi-automatic plate shifter
- B. Trailer
- C. Cake chutes
- D. Belt conveyor
- E. Stainless steel, cake-washing, air blowdown manifold
- F. Two (2) stainless steel feed pumps
- G. Walkways, railings, and stairs
- H. Double-end feed
- I. Compressor
- J. Control Panel
- K. Water wash-down deck
- L. Fluorescent lights mounted in trailer

DESCRIPTION OF EQUIPMENT TO BE SUPPLIED WITH FILTER PRESS TRAILER UNIT

A. FILTER PRESS WITH MOUNTINGS:

1. Total Volume - (cubic feet):	108
2. Total Area - (square feet):	2735
3. Model Number:	1200N25-110-108SYLS
4. Plate Size - (mm/inches):	1200/48
5. Number of Chambers:	110
6. Cake Thickness - (mm/inches):	25/1
7. Area/Chamber - (square feet):	24.86
8. Volume/Chamber - (cubic feet):	0.98
9. Height - inches:	78
10. Length - approx. inches:	396
11. Width - inches:	72

The standard filter press includes:

- * Lightweight polypropylene, 100-PSI design, non-gasketed plates, center feed, four-corner alternating discharge type, complete with #46210-6-series polypropylene filter cloths with latex edges.
- * 304 stainless steel discharge manifold with cake wash capability.
- * Air/hydraulic opening and closing system.
- * Closing force - 251 tons.
- * Rugged fabricated steel construction, coated with polyurethane finish.
- * Cabinet to house air and hydraulic components.
- * Semi-automatic, air-operated plate shifter.
- * Double-end feed.
- * Cleaning spatulas.
- * Operating manual.

The rugged fabricated steel construction is quality-engineered for strength and long service. Strong sub-arc-welded, box-formed components and solid side bars provide uniform stress distribution at the side bar joggle areas. The skeleton design operating pressure is 225 PSI to allow the installation of 225 PSI high-pressure chamber plates or membrane plates at a later date.

A pneumatically-actuated hydraulic pump closes the press, eliminating hand cranking or pumping. The hydraulic pump automatically compensates for varying temperatures and pressures that can expand or contract the polypropylene filter plate stack.

Hydraulic pump and pneumatic components are fully enclosed in a steel cabinet for protection from contamination and accidental damage, yet are easily accessible for maintenance by opening the full-width cabinet door. The components are modular for easy removal or replacement if necessary.

Lightweight, grey (RAL 7032), polypropylene plates are corrosion-resistant and are accepted as a superior material by industry worldwide to provide long service life. J-Press plates provide effective filtration and liquid/solids separation, and produce low moisture filter cake for cost-effective processing and handling. The plates are lightweight, non-gasketed, center-feed, four-corner discharge for 100 PSI feed pressure design. The plates are complete with #46210-6-series, mono-multifilament polypropylene filter cloths with impermeable rubber center sleeves for abrasion resistance. These cloths feature excellent cake-release qualities as well as virtually eliminating cake build-up in center feed port and are supplied with latex edges.

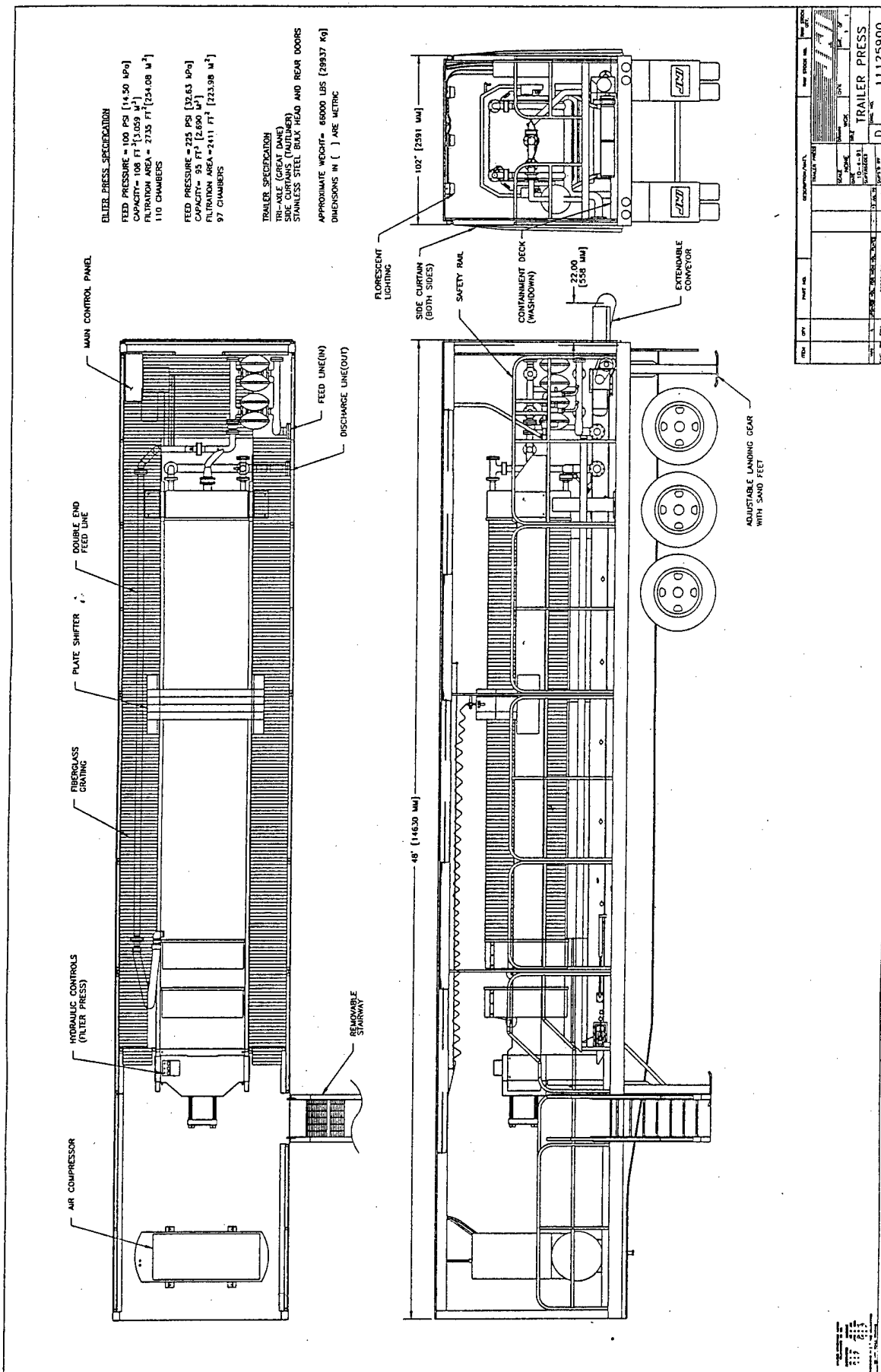
The pneumatically-powered, semi-automatic plate shifter is a time- and labor-savings option that eliminates manual separation of the plates, simplifying the removal of filter cake from the press. The plate shifter is controlled by a rocker switch with a "deadman" safety feature. The operator must maintain pressure on one side of the switch to activate plate-shifting motion. He must "rock" switch to opposite side to return to start position. Pressure must be maintained on either side of the rocker switch or no movement takes place. All operating components are mounted in an enclosed housing for maximum protection.

- B. TRAILER: The trailer will be a 48-foot long, tri-axle, flat-deck, commercial- quality, semi-trailer, specifically built to carry the filter press and equipment. The trailer will have a design capacity of 80,000 pounds. The unit will be equipped with air brakes, lights, etc., to meet DOT requirements. The unit will have four (4) leveling legs. Trailer will include rigid roof; stainless-steel-clad, swing-open rear doors; stainless-steel-clad rigid front bulkhead; and weatherproof side curtains. Vinyl side curtains are roller-suspended on continuous full-length tracks which allow curtains to be pulled back for full access to both sides of trailer.
- C. CAKE CHUTES: Chutes will be provided to direct filter cakes onto the belt conveyor. Also to include skirt board rubber on edges to seal against belt.
- D. BELT CONVEYOR: An industrial-quality, flat, 42-inch-wide belt conveyor will be mounted under the filter press to move filter cake from under the press to 30 inches past the tail-end of the trailer. The conveyor will be complete with a powered retraction/extension system to allow conveyor to move back and forth completely under the press for over-the-road movement. Drive to be 5 HP TEFC, 230/460 Volt motor.
- E. PIPING AND VALVES: Filter press piping, including manifold on press head, to be 304 stainless steel with welded and flanged fittings. Valves to be butterfly-type with stainless steel butterflies, cast-iron bodies and elastomer linings. Suction and effluent discharge connections at edge of trailer to be 4-inch FPT for use with customer-supplied hoses.
- F. PUMPS: The feed (approximately 450 gpm maximum) is accomplished with two (2) Wilden stainless steel, M-15 pumps run in parallel.
- G. WALKWAYS, RAILINGS, AND STAIRS: Fabricated steel walkways, railings, toe plates and removable stairways will be included. Walkways will be of sufficient height to allow ease of operation of press. Walkways to be of FRP, retained with stainless steel hardware and clips.

Page 4

- H. DOUBLE-END FEED: 304 stainless steel piping with flexible hose which will allow press to be fed from both ends.
- I. COMPRESSOR: 40 HP, 176 CFM, 100 PSI Quincy air compressor.
- J. CONTROL PANEL: One (1) control panel, with all controls mounted in a NEMA 4 box, to control the compressor, lights, conveyor, conveyor extension/retraction device. To include step-down transformer, two (2) 230-volt outlets and two (2) 115-volt outlets.
- K. WATER WASH-DOWN DECK: Complete deck except for front of deck above fifth (5th) wheel to be sheathed with painted carbon steel. To include 5-inch-high, dam-style containment around periphery of deck with built-in, 3-inch drains in all four corners.
- L. FLUORESCENT LIGHTS: Eight (8) dual-bulb, 8-foot-long, NEMA 4 lights, mounted to trailer roof to provide sufficient lighting in the trailer.

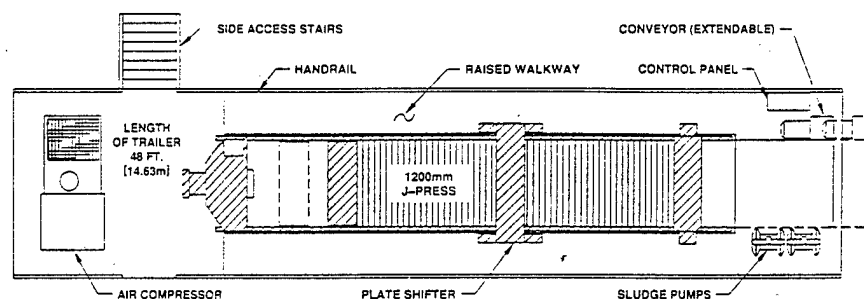
PRICE: \$258,000.00



Mobile/Trailer Mounted J-Press Dewatering Systems

SPECIFICATIONS	100 PSI STD		225 PSI STD		MEMBRANE	
	U.S. Standard	Metric	U.S. Standard	Metric	U.S. Standard	Metric
Total Volume (cu.ft./cu.m.)	98	2.78	84	2.38	117	3.31
Total Area (sq.ft./sq.m.)	2563	238	2415	224	1992	185
Model Number	1200N25-110-98SA		1200N25-100-84SA		1200M40-81-117SA	
Plate Size (inches/mm)	48	1200	48	1200	48	1200
Number of Chambers	110	110	100	100	81	81
Cake Thickness (inches/mm)	1	25	1	25	1.6 (pre-squeeze)	40 (pre-squeeze)
Area/Chamber (sq.ft./sq.m.)	23.3	2.17	24.2	2.24	24.6	2.29
Vol./Chamber (cu.ft./cu.m.)	0.89	.025	0.84	.024	1.45	.041
Height (inches/cm)	78	198	78	198	78	198
Length (approx. inches/cm)	396	1006	396	1006	396	1006
Width (inches/cm)	72	183	72	183	72	183

TRAILER OVERHEAD



Equipment to be supplied with JWI Portable Dewatering Trailer Mounted J-Press:

- | | |
|--|---|
| <ul style="list-style-type: none"> A. Filter Press with semi-auto plate shifter B. Trailer C. Cake Chutes D. Belt Conveyor E. Stainless Steel, cake washing, air blowdown manifold F. Walkways, Railings, Stairs G. Compressor H. Control Panel I. Water wash down deck J. Fluorescent lights mounted in Trailer K. Double end feed (100 PSI Standard) L. One (1) SS, air diaphragm, 3 fast fill pump (225 PSI Standard) | <ul style="list-style-type: none"> M. One (1) SS, air diaphragm. 2.1 ratio, 2" High pres. Pump (225 PSI Std.) N. Two (2) SS, air diaphragm 3" feed Pumps (Standard Membrane) O. Automatic-staged, air squeeze system (Standard Membrane) P. Appropriate to the model: lightweight polypropylene, non-gasketed, recessed chamber membrane plates, center feed, four corner alternating discharge type, complete with polypropylene filter cloths with latexed edges. Q. Air/hydraulic opening and closing system R. Cabinet to house air and hydraulic components S. Cleaning spatulas T. Operating manual |
|--|---|

Appendix C: Sharples Centrifuge

Phone Conversation

Company: Sharples

Contact Person: Ron Moody

phone #: (630) 571-6120

date: 3/20/97

The Sharples PM-38000 was recommended for the Western Corridor's needs. It has a capacity of 50 gpm. The centrifuge costs \$160,000. A trailer, which would include the feed pumps, polymer system, conveyors, etc., is an additional \$250,000.

Alfa Laval and Sharples®

Leaders in Advanced Separation Technology

Alfa Laval and Sharples products have been on the leading edge of separation technology for over 100 years each, establishing themselves as the dominant powers in the world market. By joining forces, the largest and most advanced separation company in the world was created — unmatched in applications experience, technical expertise, product quality and service. Our products represent the state of the art in separation technology. We manufacture the most versatile centrifuge line available today.

Wastewater Treatment and the Environment

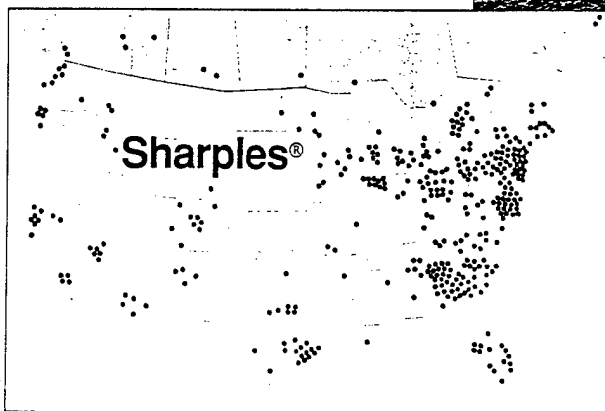
For over 30 years, Sharples products have provided wastewater treatment technology that not only meets the current needs of an expanding population but anticipates future environmental controls. Using new and innovative separation technologies, we have achieved the highest levels of wastewater treatment efficiency and cost effectiveness. We offer the high-performance alternative to older, less effective treatment methods.



Alfa Laval and Sharples® 300,000 square foot factory in Warminster, PA.



Sharples Global Product Center and headquarters in Warminster, PA.



Sharples wastewater and potable water installations in North America.



Advantages of Sharples® Centrifuges

Drier Cake Solids: Sharples® MaxiMizer® DS centrifuges have consistently provided cake of 30% to 35%, often 5 to 10 percentage points drier than competing technologies.

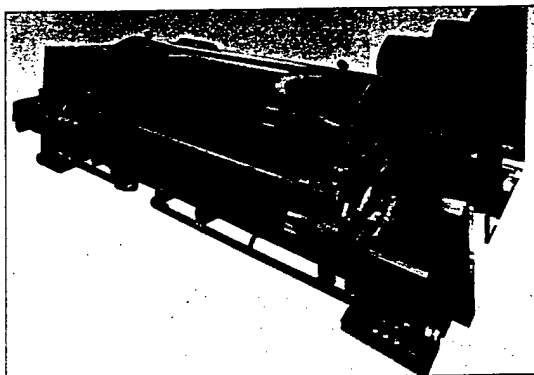
Low Maintenance: Sharples centrifuges provide years of nearly maintenance-free operation. Durable construction materials such as stainless steel, Sharples STC carbide and 480Urethane are used to limit corrosion and erosion.

Quality Construction Materials: Centrifugally cast stainless steel parts and STC carbide tile assemblies eliminate problems created by welding and provide superior corrosion and abrasion resistance.

Reliability: Proven, around-the-clock, on-line reliability is being demonstrated daily in more than 300 wastewater and potable water treatment plants, operating more than 1,500 centrifuges in North America.

Environmental Advantages: Containment of the process means aerosols and vapors are virtually eliminated, significantly improving the work environment.

The DS-406's enclosed design limits aerosols and spillage typical of filter systems. All DS Series centrifuges are equipped with the new rugged, reliable TRI frame.



Minimal Operator Attention: Equipped with automated controls, our centrifuges run virtually unattended. A full-time operator is not needed.

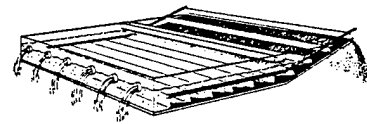
Housekeeping: Because the process is contained, the area around the centrifuge remains free of sludge and liquids. Plant housekeeping is quick and easy. A clean-in-place system is available for periodic cleaning or cleaning prior to maintenance.

Cost-Effective Performance: Sharples centrifuges provide cost-effective, high-G, low maintenance performance for thickening and dewatering applications. Our new dewatering centrifuges can operate at up to 4,000 G for plants of all sizes.

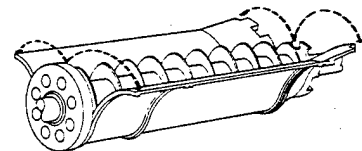
Rugged Design: Independent drive motor, backdrive, lubrication and vibration dampening systems combine with quality construction to provide reliable high-G operation.

Technical Support and Service: Sharples applications engineers are ready to respond to your needs. We maintain a multi-million dollar inventory of parts, ready for immediate delivery.

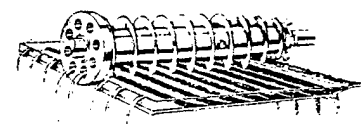
Understanding the Basics: How a Centrifuge Works



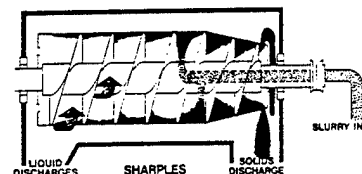
A centrifuge is like a clarifier whose base has been wrapped around a center line, so that its rotation generates G, or gravitational force.



The greater the G force, the more quickly the solids in the slurry are sedimented against the rotating bowl wall.



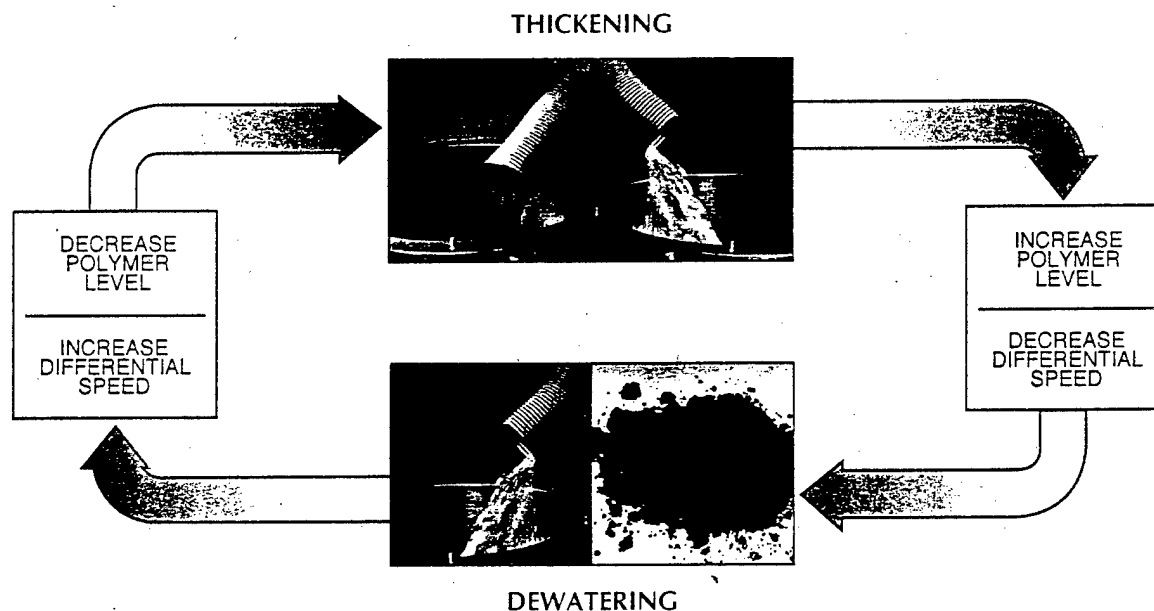
The less dense liquid forms a concentric inner layer which flows over adjustable plate dams, similar to a clarifier's weir, and is then discharged.



Pond depth and retention time in a Sharples centrifuge can be varied for maximum performance. The sedimented solid particles are compacted by the high-G force and are continuously removed from the bowl by the action of a helical screw conveyor or scroll, much like the scraper in a clarifier.

Sharples® PolyMizer®

The Answer to Your Thickening and Dewatering Needs



Sharples PolyMizer centrifuges add operational flexibility because they can both thicken and dewater.

Sharples PolyMizer centrifuges are designed to effectively thicken and dewater municipal sludge, and are available in various sizes and capacities to meet the needs of wastewater treatment plants from the smallest package plants to the largest plants in the world.

A Sharples PolyMizer centrifuge resolves the problems and expense associated with other methods of dewatering or thickening sludge. Sludge handling costs are minimized prior to final disposal or beneficial reuse. Installation of a PolyMizer for thickening can reduce the volume of sludge handled by digesters by up to 70 percent. When viewed from the standpoint

of long-term, around-the-clock operations, the proven economies of the PolyMizer centrifuge, compared to other methods of thickening and dewatering, are immediately evident.

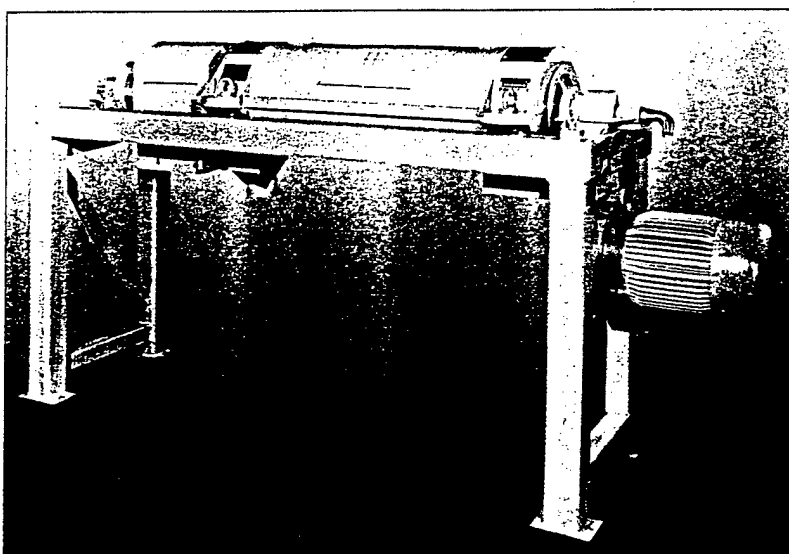
Made from superior materials, PolyMizer centrifuges have operated efficiently in the toughest environments, providing years of nearly maintenance-free performance.

When compared to competing technologies, the PolyMizer offers many tangible advantages. It contains process vapors and odors, easily handles fluctuations in the feed, and requires minimal operator attention.

Potable Water Applications

Sharples centrifuges are ideally suited to dewater sludge from surface and ground water. They effectively deal with lime, alum and other sludges in potable water facilities. Sharples centrifuges achieve 20 to 50 percent solids recovery at very low polymer doses.

When compared to pressure filtration systems, Sharples centrifuges produce lower sludge handling costs and decreased chemical costs without sacrificing cake dryness. Further, operator attention and required maintenance are both significantly lower than with pressure filtration systems.



The PM-38000 is specially designed for plants processing up to 5 MGD.

Small Plant Operations

The modular Sharples® PolyMizer® PM-38000 centrifuge is a compact, dynamic machine designed to provide both thickening and dewatering for wastewater treatment plants processing 5 MGD or less. It offers all the advantages, cost effectiveness and innovation of centrifuges for about the price of a belt filter press.

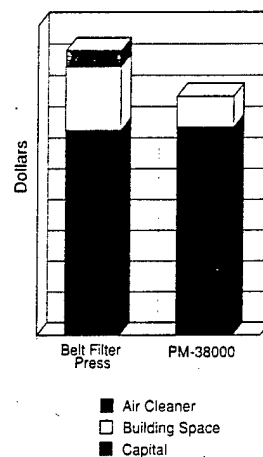
It can switch from thickening to dewatering, or vice versa, in a matter of minutes without interrupting the feed. Its compact size requires roughly one third the floor space of a belt filter press, while incorporating the high-tech materials and engineering innovations that have established Sharples centrifuges as world leaders in reliability and performance.

PM-38000 Doubles Screw Press Performance

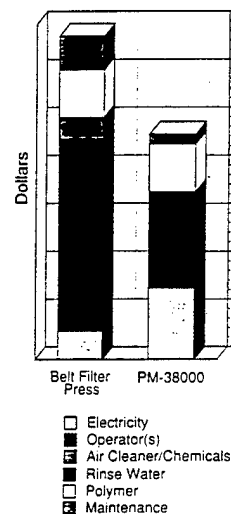
A Sharples® PM-38000 was tested against a screw press processing oxidation ditch Waste Activated Sludge. The screw press averaged 8%-9% cake, not dry enough for trucking or land application. The PM-38000 achieved cake of more than 16% with 98% recovery. The number of truck-loads was halved, difficulties with land application disappeared and the plant work environment improved significantly.

TYPICAL 3 MGD PLANT Lower Costs than a Belt Filter Press

TYPICAL 3 MGD PLANT INSTALLATION COSTS



OPERATING COSTS



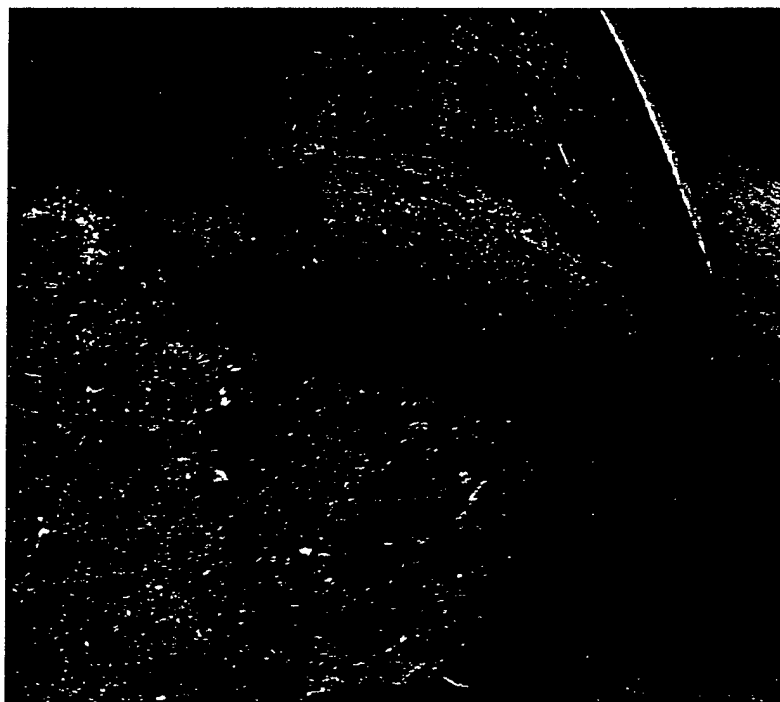
Sharples® MaxiMizer® DS

For Dewatering to 30+% Solids

Traditional centrifuge and belt filter press systems, using technology available for the last two decades, are able to produce cake in the 18% - 22% range. Recognizing the advantages of drier cake, Sharples pioneered a new "Dry Solids" technology which produces cake that consistently exceeds 30%, even when dewatering difficult sludges. In fact, cake dryness above 35% has been achieved in several installations. The Sharples MaxiMizer DS produces solids that are often 10 percentage points drier than cake produced by other technologies.

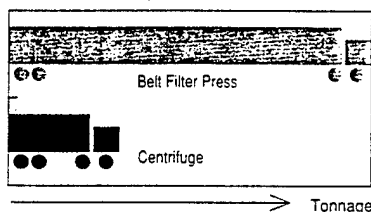
Significant Savings

Drier cake has a profound impact on sludge handling and disposal costs, whether the solids are incinerated, land-filled, composted or ground-applied. Drier solids mean less weight to transport, fuel-efficient incineration, and a cleaner centrate.

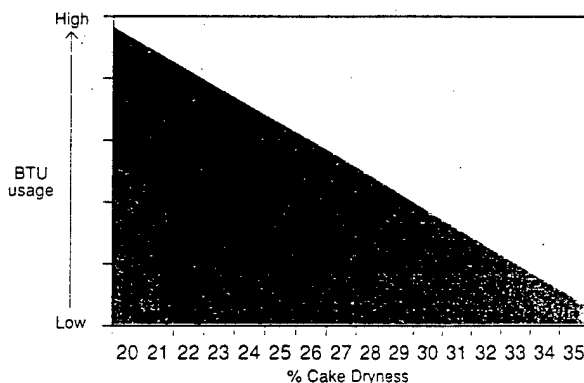


Cake dryness above 35% has been achieved with the MaxiMizer DS on mixed primary and waste activated sludges.

HAULING COSTS

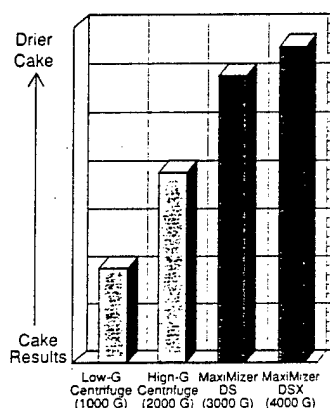


INCINERATION COSTS





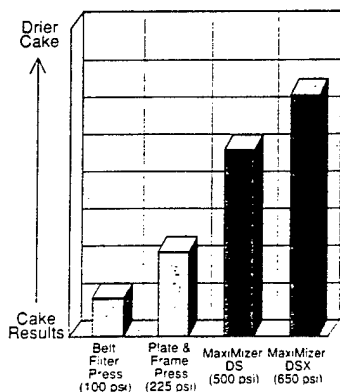
IMPROVED CENTRIFUGE PERFORMANCE



Higher Pressure, Greater Dryness

Filtration devices use gravity, vacuum or pressure to separate solids out of liquids. Belt filter presses can generate up to 100 pounds per square inch (psi) to squeeze liquids from solid, while plate and frame presses can exert up to 225 psi. High-G cen-

PSI COMPARISON



trifuges such as the MaxiMizer DSX generate the equivalent of 650 psi, producing a cake of more than 30% dryness with small polymer dosages.

Ease of Operation

Sharples centrifuges are easy to operate. Once the operator has chosen the feed rate, he can easily optimize performance by adjusting the back-drive and the polymer rate. Alternate methods of dewatering often require continuous, multiple adjustments and constant operator attention.

MaxiMizer DSX

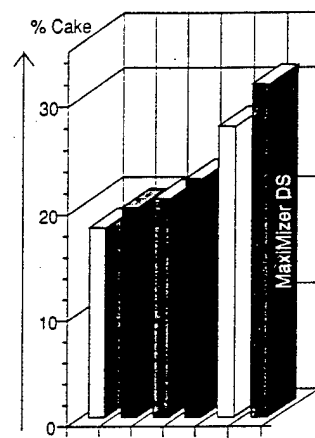
Sharples MaxiMizer DSX centrifuges provide 30 percent greater throughput and use 20 percent less polymer than current Dry Solids centrifuges. The DSX units operate at 4000 G, resulting in cake dryness of 35 percent or better when processing most municipal sludges.

The advanced design results in power usage savings of up to 20 percent and significantly lower noise levels during operation. A new and improved abrasion resistance package results in even less wear and lower maintenance than the low levels already achieved by Sharples centrifuges.

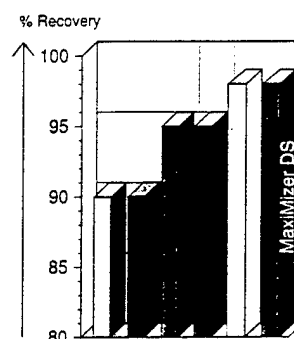
Sharples® MaxiMizer® DS Centrifuges Outperform Competitive Technologies

For ease of operation, cake dryness, and recovery rate, Sharples MaxiMizer DS is the clear choice.

CAKE DRYNESS



RECOVERY



- ☐ Vacuum Filter Press
- ☐ Screw Press
- ☐ Belt Filter Press
- ☐ Centrifuge
- ☐ Plate & Frame Press

Statistical information on above categories from article by Jeannette A. Semon, City of Stamford.

MaxiMizer DS information from actual field operation.

Sharples® MaxiMizer® XM

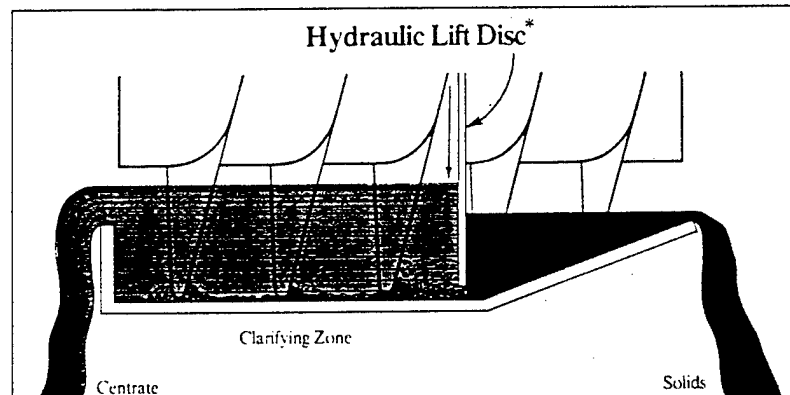
For Thickening Without Polymer

The MaxiMizer XM centrifuge was originally developed for thickening Waste Activated Sludge (W.A.S.) to 3 - 7% solids without the use of polymer. Even today the MaxiMizer XM provides the most effective approach to thickening waste activated sludge.

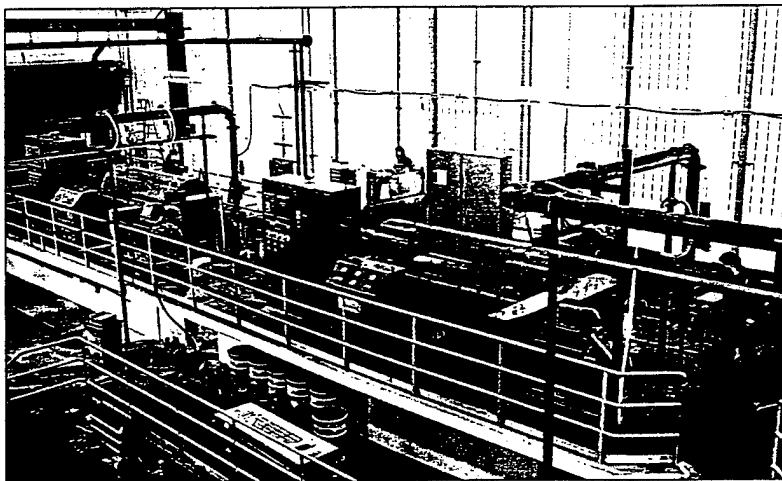
The MaxiMizer XM combines an efficient feed zone for gentle acceleration with minimal energy requirements, with a hydraulic lift disc that reduces turbulence and improves conveying efficiency. An advanced weir design provides an even flow of liquids through the hub. The 360° solids discharge ports have been designed to provide a higher solids discharge rate.

The MaxiMizer XM is an excellent option when expanding plant facilities. Capital equipment expendi-

tures can be held to a minimum because just one MaxiMizer XM can significantly increase sludge handling capacity without additional digesters and dewatering equipment.



The Sharples hydraulic lift disc reduces turbulence and improves conveying efficiency.



MaxiMizer XM-706 Saves Plant \$3,000+ Per Day

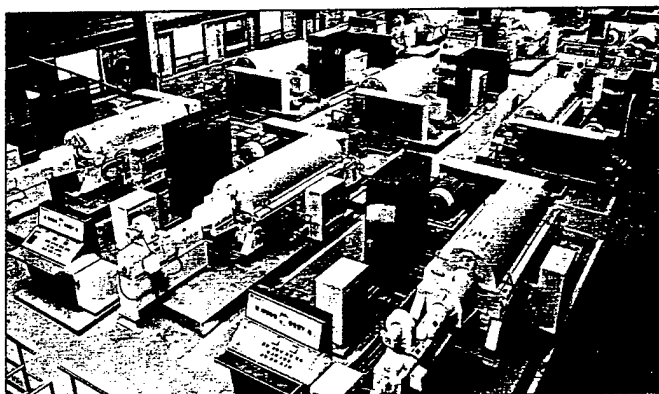
A northern New Jersey authority's 75 MGD advanced secondary wastewater treatment facility faced thickening capacity problems. A Sharples MaxiMizer XM-706 resulted in a savings well in excess of \$3,000 per day versus gravity thickening lagoons. Payback took less than 15 months.



Proven Technology

Technology Leader

The wastewater treatment plant in a large midwestern city had centrifuges equipped with fixed speed backdrives, which were producing 15% cake at 85% recovery. Sharples® Dry Solids centrifuges, equipped with direct current, torque-controlled backdrives increased cake dryness to 30%, with a recovery of more than 97 percent.



60% Drier Cake

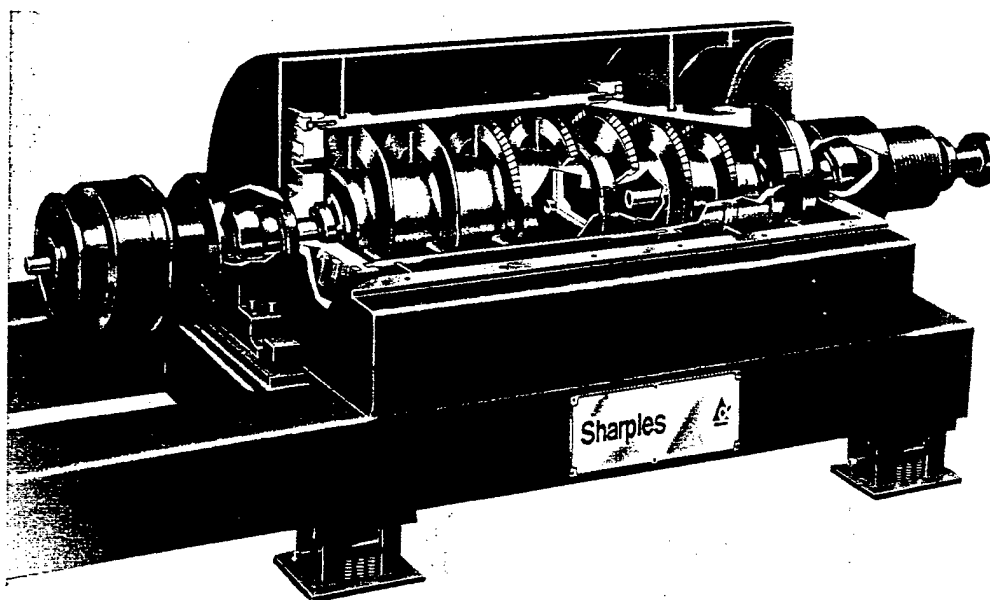
The goal of a northwestern United States primary and conventional W.A.S. treatment plant was to improve cost effectiveness. It was producing 17% cake with existing low-G centrifuges. A high-G stainless steel Sharples centrifuge increased dryness to 27%-32% with 95+% recovery. Incineration costs decreased by more than 45 percent.

Major Annual Savings

A northeastern city put four DS-706 stainless steel centrifuges in operation to dewater a mixed sludge. The DS-706s have routinely produced cake solids of over 30% from the 2 1/2% feed. Recovery has averaged over 98%. Annual savings of over \$130,000 have been achieved for every percent gain in dryness.



Superior Construction Materials Provide Unmatched Performance



Sharples® experience and extensive research and development, has led to the design and manufacture of the world's best centrifuges. Sharples centrifuges outperform competitive centrifuges in terms of performance, reliability and long life.

Centrifuges vary greatly in design, materials and manufacturing methods, factors that have a profound effect on long-term performance and cost effectiveness.

Superior Construction

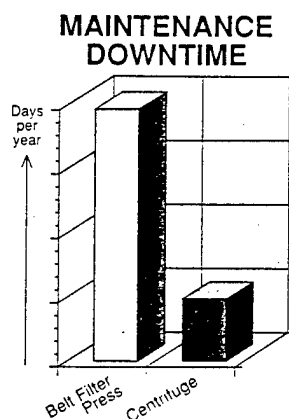
Sharples centrifuges are unsurpassed in design and construction, including centrifugally cast stainless steel components and superior abrasion and corrosion resistant materials. Proven starter systems and backdrives are specifically designed for maximum performance and economy. Proprietary design and engineering breakthroughs

provide reliability and economy of operation. Sharples centrifuges are built to last. Millions of hours of service in plants around the world attest to it.

Advanced Design

Sharples centrifuges are products of continuous development and techno-

logical advancement, and feature innovative design features not found in competitive centrifuges. Sharples centrifuges have unrestricted 360° discharge of solids from the bowl, utilizing a special high-efficiency port configuration. We use a high molecular weight engineering plastic accelerator in the feed zone to reduce turbulence and decrease the time needed to separate solids from liquids. Our unique helical screw conveyor features flow stabilization channels that further enhance laminar flow and allow solids to settle more rapidly. The patented Sharples weir design is the most efficient ever developed and acts to further reduce turbulence. The bowl design keeps protrusions to a minimum, resulting in an aerodynamic profile that keeps power usage and noise levels low.





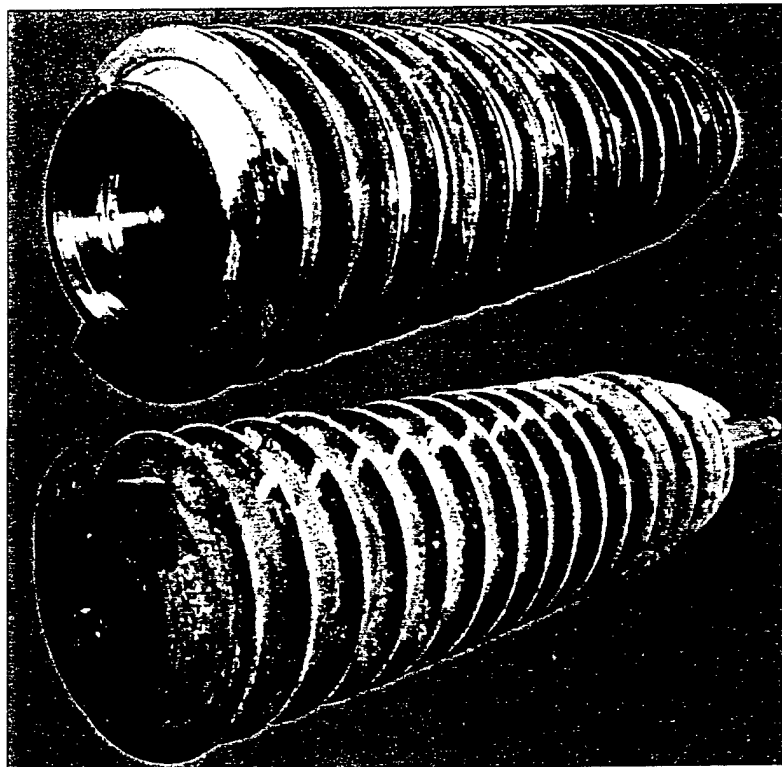
Stainless Steel

Municipal waste applications are not generally thought of as being highly corrosive, but variable pH, ferric chloride, polymers, solids and other materials found in the influent combine to create corrosion. Therefore, Sharples® centrifuges are designed and built using stainless steel for critical wetted surfaces.

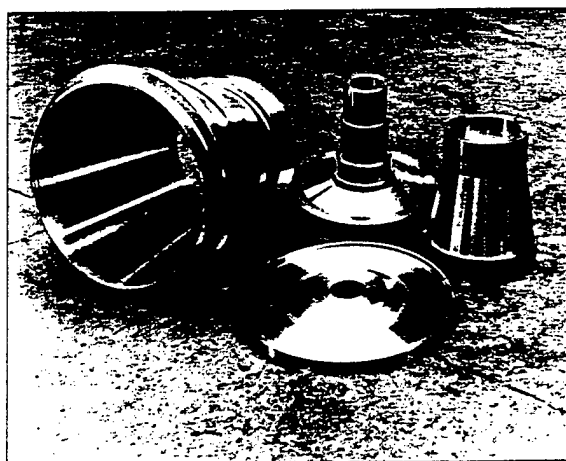
For reliable, high-G centrifuge performance, 316 stainless steel is far superior to carbon steel in environmental applications. Sharples decanters use 316 and Duplex 317 stainless for the wetted parts of its large, high-G decanters. Tightly controlled metallurgy results in yield strengths far in excess of those found in rolled 316 and 317. The 316 and 317 stainless steel parts used in Sharples centrifuges offer a unique blend of high strength, corrosion resistance, ductility and weldability. The result is reliable, long-term centrifuge performance, low maintenance, and easy serviceability.

Sharples stainless steel centrifuges provide superior performance, dramatically reduced maintenance costs, faster and easier service, and a much longer productive life. Sharples high-G stainless steel centrifuges have been in continuous operation for over 20 years.

Conversely, the use of carbon steel leads to multiple problems. Carbon steel rusts. Rust causes alignment problems, creating bearing failure and excessive vibration. Rust makes disassembly difficult, sometimes taking up to three times as long. Also, the combination of corrosion and erosion accelerates additional wear on carbon steel parts, reduces performance, increases maintenance and shortens centrifuge life.



Stainless steel components (top) showed no deterioration after four years of operation, unlike the carbon steel (bottom).



Centrifugally cast stainless steel parts are virtually free from flaws, internal defects and welds.

Advanced Technology in Corrosion and Abrasion Resistance, Automation

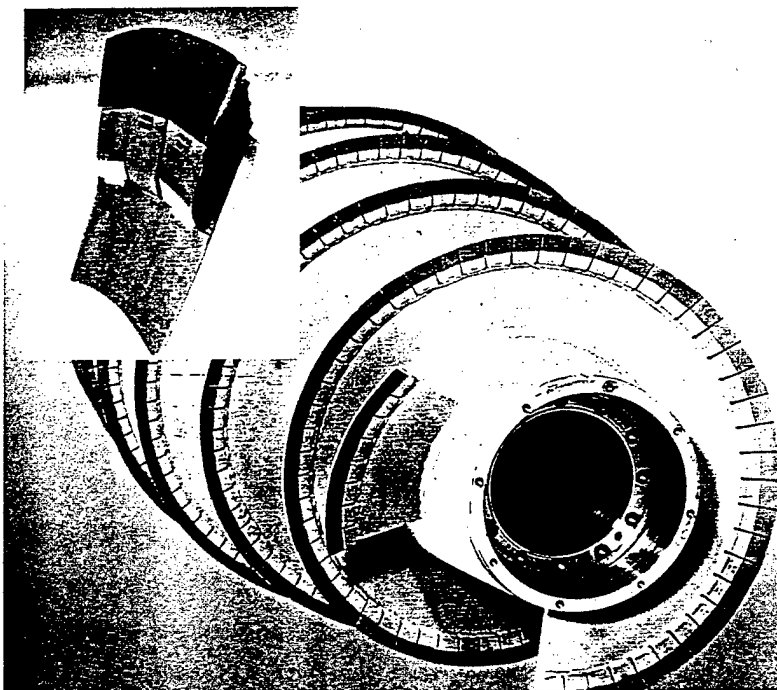
Centrifugal Castings

All high stressed rotating parts in Sharples® centrifuges are manufactured from quality, stainless steel centrifugal castings. Centrifugal castings provide truer uniformity and greater overall strength than any competing method.

Centrifugal castings are more corrosion-resistant and are virtually free of flaws and internal defects. Further, this type of construction eliminates metallurgical notches (welds). Welds are more subject to both corrosion and stress. The elimination of welds translates directly to a stronger, more reliable and longer-lasting centrifuge.

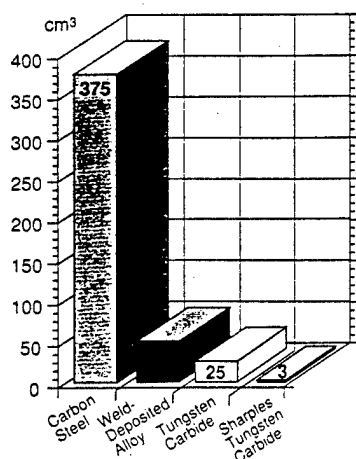
Abrasion Resistance

Sharples centrifuges' abrasion technology is recognized throughout the



Sintered tungsten carbide assemblies protect Sharples conveyors from abrasion.

ABRASION LOSS



Based on a standard ASTM test measuring volume loss from materials under abrasion.

industry. We were the first to develop and use a proprietary grade of sintered tungsten carbide on erosion-prone areas, and the first to develop the technology to attach the tiles to the scroll. Our STC carbide tile assemblies protect the scroll in our centrifuges. Continually improved by Sharples engineers, these tiles provide superior protection, with more than four times the life of the best conventional tiles. Materials such as ceramics, stellite, and other grades of tungsten carbide or tungsten carbide coatings do not offer the abrasion resistance protection afforded by Sharples tile assemblies.

Sharples engineers have studied the effects of abrasion and developed special technologies to meet different needs. Where the abrasion is in the form of scratching, grinding or gouging, for example, we use STC carbide tiles, inserts or wear rings. Where the abrasion is caused by impact or high velocities of solids, high molecular weight engineering plastic liners are used to limit wear.

All parts that may be subject to abrasion or erosion are field replaceable to minimize any possible downtime.



Mechanical and Electrical Advances

The performance of Sharples® centrifuges is optimized by a backdrive and a planetary gearbox system that allows precise control of the differential speed between the centrifuge bowl and its internal conveyor. This differential controls the flow rate of solids through the centrifuge and is essential to achieve maximum cake dryness.

Our Dry Solids centrifuges are equipped with efficient, variable speed electronic backdrives which use a feedback circuit to measure speed and other parameters. The electrical backdrives are available as eddy current brakes, DC backdrive systems or AC variable speed systems and provide excellent central overall operating ranges.

In addition, Sharples decanters are available with backdrives that regenerate electricity. This electricity is fed back into the power lines, further reducing operating costs.

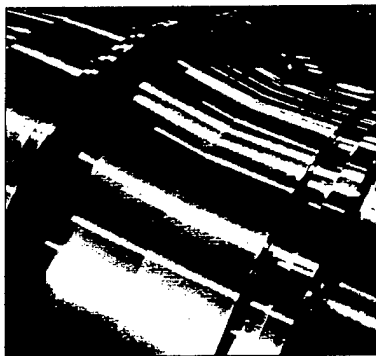
Hydraulic backdrives used on non-Sharples centrifuges, tend to be inefficient, high pressure devices that require significant maintenance.

Reliable Starts

Sharples centrifuges use a specially designed, maintenance-free starting system. The wye delta starter is a soft starting system that reliably starts high inertial loads. The wye delta starter eliminates high maintenance fluid coupling starter systems found on other centrifuges.

Power Usage

With the use of a regenerative backdrive, the power is fed back into the system, making Sharples centrifuges more power efficient.



The Sharples noise ring system results in lower power usage and quieter operation.

In addition, the aerodynamically designed profile of the bowl, with its recessed fasteners and noise ring, results in less "windage," creating lower power usage and quieter operation.

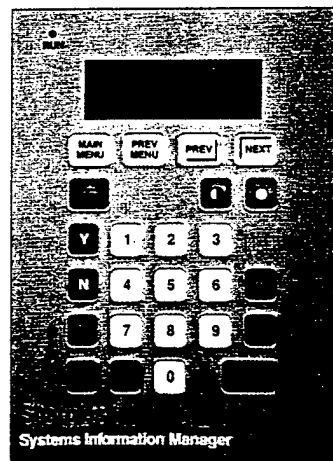
Automation

Sharples Automated systems provide extended operational flexibility and insure maximum performance efficiency.

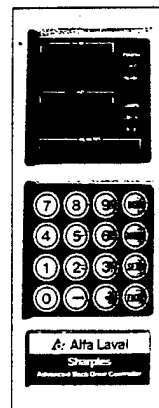
The Sharples Automatic Backdrive Controller (ABC) is a dedicated microprocessor that digitally displays information such as bowl speed, pinion speed, torque, and differential RPM. It can be interfaced with other network or desktop computers for remote readout and control. Used in conjunction with the Sharples backdrive system, it senses conditions inside the centrifuge and constantly optimizes performance by adjusting for changes in flow rates, influent quality and cake solids. Staffing requirements are significantly reduced.

The Sharples Decanter Manager is a system that monitors the operation of the entire centrifuge, including vibration, bearing temperatures, main motor

performance and backdrive motor performance. Any deviation from normal is instantly relayed to the operator. Both the Decanter Manager and the ABC can be connected, via modem, to the computer at our Warminster, PA plant to provide immediate technical process and diagnostic support. Features include a specially-designed high-tech electronic control panel that insures easy and efficient startup.

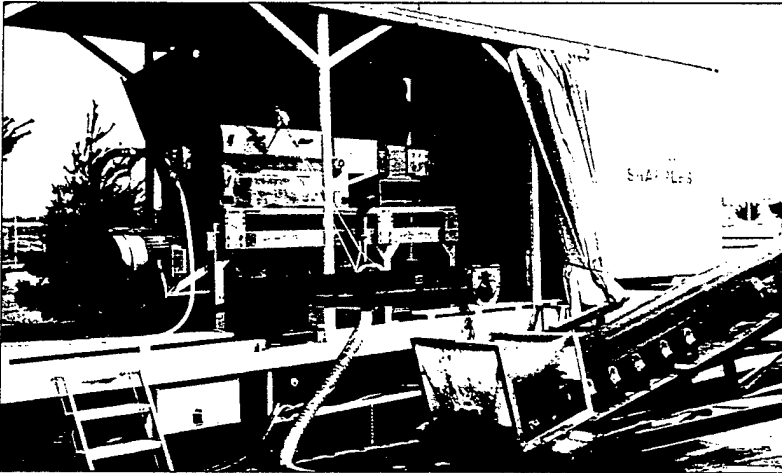


The Sharples Decanter Manager monitors all operating functions.



The Sharples ABC controller automatically adjusts for changes in feed without operator input.

Quality Testing, Training and Service

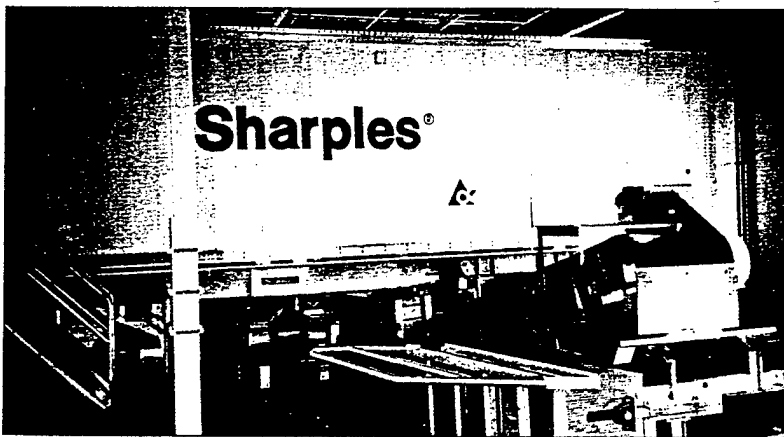


The Sharples trailer is available for on-site sludge processing tests.

Testing and Training

Sharples® engineers recognize the unique characteristics of sludges and the need to accurately predict performance before making a purchase decision. The Sharples test trailer is available to conduct a test in your plant to accurately gauge the thickening or dewatering results possible on your sludge.

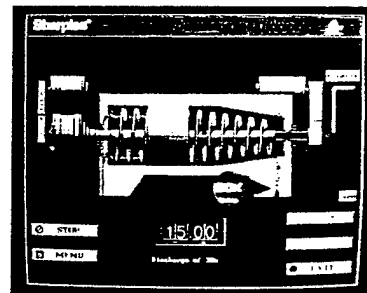
In addition, we provide a professionally prepared, on-site training program for your staff, led by qualified field service engineers. Field service engineers will review your process practices, work with you to optimize your performance, and review your preventive maintenance practices.



Trailer mounted units offer you flexible processing capabilities.

Service

Superior after-sales support is a major priority of Alfa Laval Separation Inc. As the world's largest, most advanced separation company, we provide quality service for Sharples products, worldwide. Our experienced technical sales and customer service engineers are always available to provide answers and assistance. A multi-million dollar parts inventory is stocked at our Warminster, PA headquarters, ready for immediate shipment. Our repair facilities offer equipment upgrades to keep pace with advancing technology. Factory trained field service engineers are on call to provide preventive maintenance as required.



Training programs with computer simulations are available for you staff.



Sharples® Centrifuges:






































The Economic Choice for Dewatering

When all cost factors are evaluated (capital investment, labor, power and other operational expenses), a centrifuge installation is frequently 25 - 30 percent less expensive than filter installations. The capital cost of a Sharples® PM-38000 modular centrifuge, for example, is typically the same as a belt filter press, while the total present worth may be 25% less. Sharples fully-automated centrifuges are the practical choice of plant engineers and supervisors who want

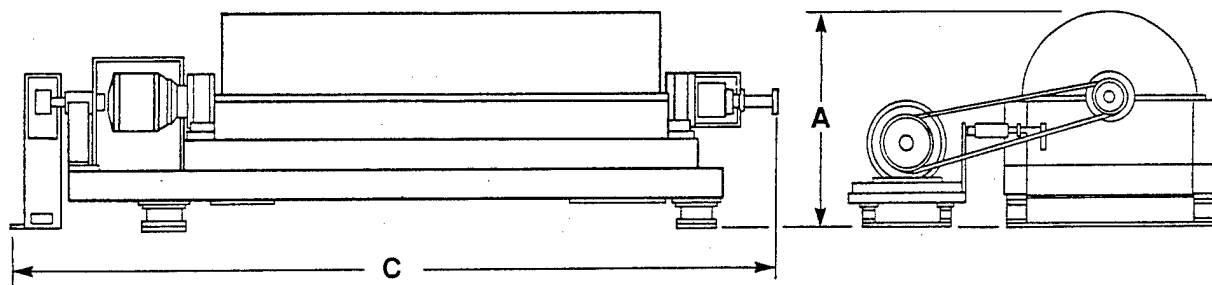
proven, reliable, around-the-clock performance, year-in and year-out in all areas of wastewater treatment.

More than 1,500 Sharples centrifuges are operating successfully in over 300 water and wastewater treatment plants in North America. Sharples centrifuges perform effective dewatering and thickening duties in facilities from the smallest package plants to the largest plants in the world.

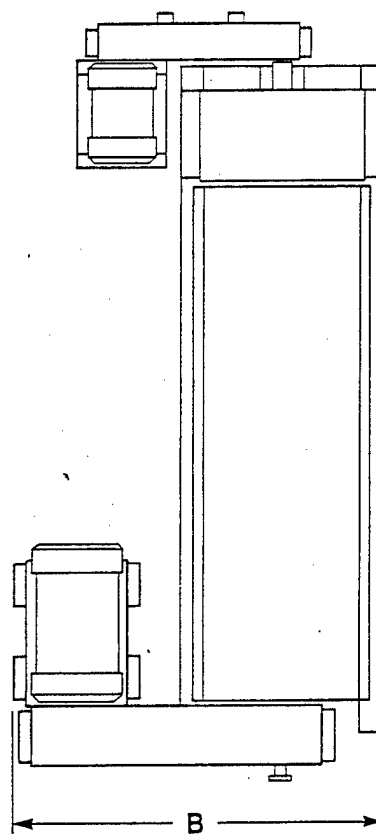
Dewatering Cost Comparison

	Dry Solids Centrifuge	Belt Filter Press	Plate & Frame Press
Installation	\$ \$	\$ \$ \$	\$ \$ \$ \$ \$ \$
Building		 	  
Maintenance		  	   
Solids Disposal	\$	\$ \$ \$	\$ \$
Ventilation		  	 
Water		     	  
Labor		 	   

The figures provide an estimated proportional representation of the savings available to centrifuge users. e.g. maintenance costs for a Belt Filter Press are estimated at three times the cost of a Sharples DS centrifuge. Actual comparisons may vary based on specific installations. Installation figures are indicative of total costs, including capital and auxiliary equipment.



MODEL NUMBER	A HEIGHT	B WIDTH	C LENGTH
PM-35000	39"	76"	92"
PM-38000	72"	42"	146"
PM-46000	45"	146"	189"
PM-75000	56"	151"	212"
PM-76000	56"	151"	240"
PM-95000	70"	185"	260"
PM-96000	70"	185"	296"
DS-305	39"	76"	131"
DS-306	72"	42"	146"
DS-406	45"	146"	189"
DS-705	56"	151"	212"
DS-706	56"	151"	240"
DS-906	70"	185"	296"
XM-505	39"	76"	131"
XM-705	56"	151"	212"
XM-706	56"	151"	240"
XM-905	70"	185"	260"
XM-906	70"	185"	296"
XM-1006	82"	207"	330"



Sharples®

Environmental Business Unit of
Alfa Laval Separation Inc.
955 Mearns Road
Warminster, PA 18974
Telephone (215) 443-4222
(800) 782-3751
FAX (215) 443-4139
Control #700-105

Novato, CA
(415) 883-8520
Stanton, CA
(714) 527-9285
Atlanta, GA
(404) 393-2087

Sales Offices

Oak Brook, IL
(708) 571-6120
Wayne, PA
(610) 254-8500
Houston, TX
(713) 586-0454

Scarborough, Canada
(416) 297-6345
Mexico
011-525-398-8760



Appendix D: TRIMAX Environmental

Phone Conversation

Company: Trimax Environmental

Contact Person: Blake Dermott

phone #: (800) 465-2115

date: 4/24/97

Trimax Environmental buys old machines and reconditions them. The machines are retrofitted to achieve drier sludge than originally intended. Most machines they have are Sharples PC81000, which is a 1975 model. The centrifuge can handle 20 to 25 dry tons/day on a 24-hour day. They achieve 30 to 35 percent solids. Trimax itself owns and operates 95 percent of the systems they have built. However, they can custom-make a system to be purchased and run by someone else with a guarantee of workmanship and a service contract. They also are able to test the sludge and, dealing with the characteristics of the sludge, make the machine specifically for that sludge. For example, they will purchase a belt filter press and install it if it works better with the sludge in question.

The standard trailer is 45-ft long. It contains front end equipment that removes rocks, plastic, rubber, hair and other items that may clog or damage the centrifuge. The trailer also contains a polymer system and the centrifuge. For a system as small as the one required for the Western Corridor, a 5-ton truck or a van that contains the equipment in the back may be more cost effective.

Typically, the centrifuge costs between \$50,000 and \$100,000. The trailer is an additional \$10,000 to \$20,000. The entire system including pumps, polymer system, etc. costs between \$150,000 and \$200,000.

They will provide CERL with information including a video.



April 24, 1997

Amy Swanson
USA CERL
P.O. Box 9005
Champaign, IL
61826

Dear Amy:

Thank you for your request for more information about the services that TRIMAX Environmental has to offer. I am forwarding to you our company brochure. I hope that you find this information useful and I would appreciate your feedback regarding this.

TRIMAX is an environmental services company with offices in both the United States and Canada. We provide mobile mechanical dewatering services using large high speed decanter centrifuges to process various sludges from spill basins and sedimentation ponds. We currently have a large fleet of Sharples horizontal decanter centrifuges which include PC 81,000 B, PM 75000 and new Sharples DSX 706 machines that operate at 4000+ "G". These new machines will allow us to supply the driest cake solids in the industry. All of our machines are one hundred percent mobile. TRIMAX can provide all the services required to facilitate a turnkey project. This would include dredging services, portable electrical supply and dewatered sludge transfer trucks as well as fully trained personnel.

The mechanical dewatering process virtually eliminates leachate problems associated with sludge disposal in landfills as well as increasing the landfill life by reducing volumes of sludge for disposal. The services provided by TRIMAX minimize the handling of sludge thus reducing the potential for spills. Additionally, a geotextile liner is installed by TRIMAX under the process and truck loading equipment during the execution of our services, thus eliminating any possible ground contamination during the sludge dewatering.

We have recently added to our list of equipment a complete sludge processing system which is trailer mounted. This self contained unit has shown a drastic reduction in mobilization and demobilization costs and is ideal for pilot programs as well as small budget jobs. The trailer mounted unit has proven to be a great addition to our fleet of centrifuges. We have recently added two more trailers to house one of our new DSX 706 machines as well as our recently purchased Sharples PM 75000 and are in the process of

TRIMAX ENVIRONMENTAL SERVICES LTD.

9440 - 60 Avenue, Edmonton, Alberta T6E 0C1 • Tel: (403) 433-7373 • Fax: (403) 433-5577 • Toll Free: 1-800-465-2115



building our fourth. These new trailers will give us different process capabilities of approximately 2000, 3000, and 4000 "G"s. In our discussions I had mentioned our interest in designing and manufacturing a custom system for your needs. We have been approached by Sharples to consider the potential to manufacture trailers for them. We can use all new or reconditioned equipment.

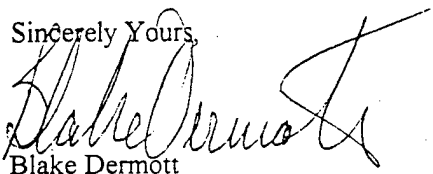
We also offer consulting on a individual project basis. This could include everything from design, to purchasing of all equipment including centrifuges and pumps etc., to the complete set up and management of your dewatering program. This type of program is evident in the longterm contracts we have with the cities of Vancouver and Kelowna in BC Canada.

I have enclosed our literature in a brochure form as well as a video which illustrates some of our successful projects. We would be pleased to forward to you a list of references upon request.

If any further information is required, please feel free to contact me at your earliest convenience.

In the near future, I will be contacting you to further discuss the above. Thank you once again for your interest.

Sincerely Yours,



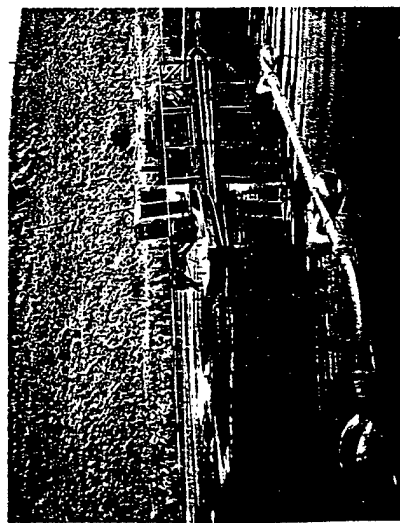
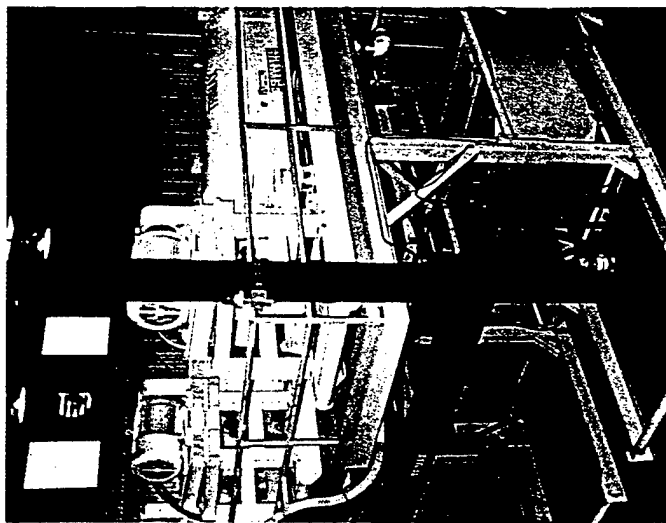
Blake Dermott

Manager of Marketing And Sales

TRIMAX

Turnkey Projects

TRIMAX offers complete dewatering, dredging and hauling services. We also have experience in the set up and management of long term and permanent dewatering sites.



- Largest fleet of high speed decanter centrifuges in the world
- Complete dredging services
- Offices in Canada and the U.S.A.
- Driest cake solids on primary or secondary biosolids
- Sharples DSX 4000+ "G" technology
- Less polymer consumption
- Emergency response capability
- Trained and experienced personnel
- Short or long term projects

Other Sludges Processed

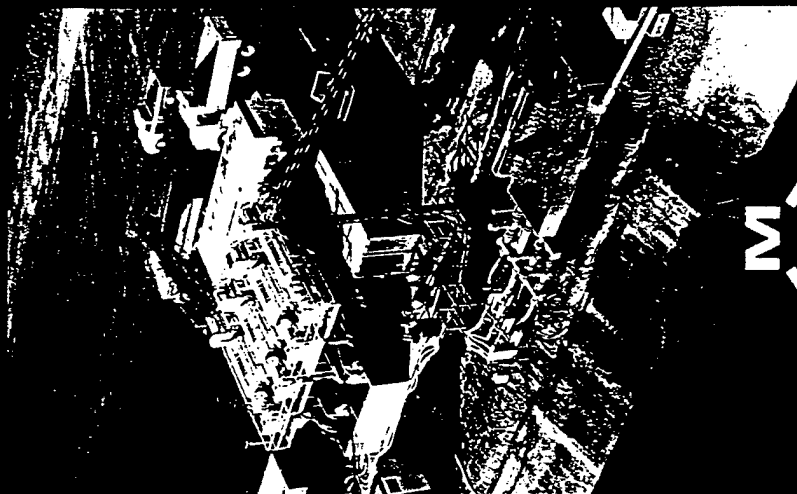
- Aerobic and Anaerobic
- Alum
- Lime
- API Separator
- Municipal
- Pulp and Paper
- Primary and Secondary Water Treatment



TRIMAX

Environmental Services Ltd.
U.S.A. or Canada
1-800-465-2115

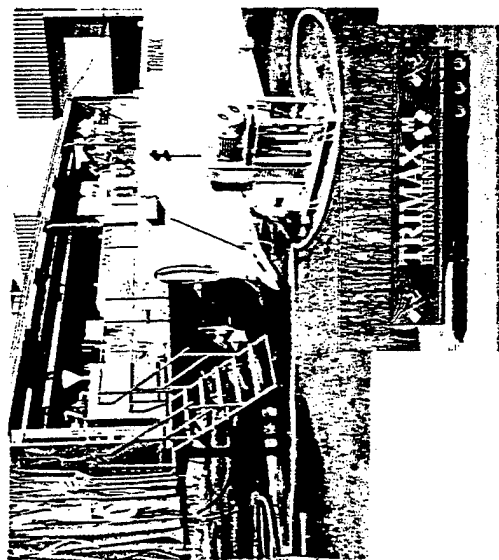
Mobile Mechanical Dewatering



TRIMAX
Environmental Services Ltd.

Digester and Clarifier Maintenance

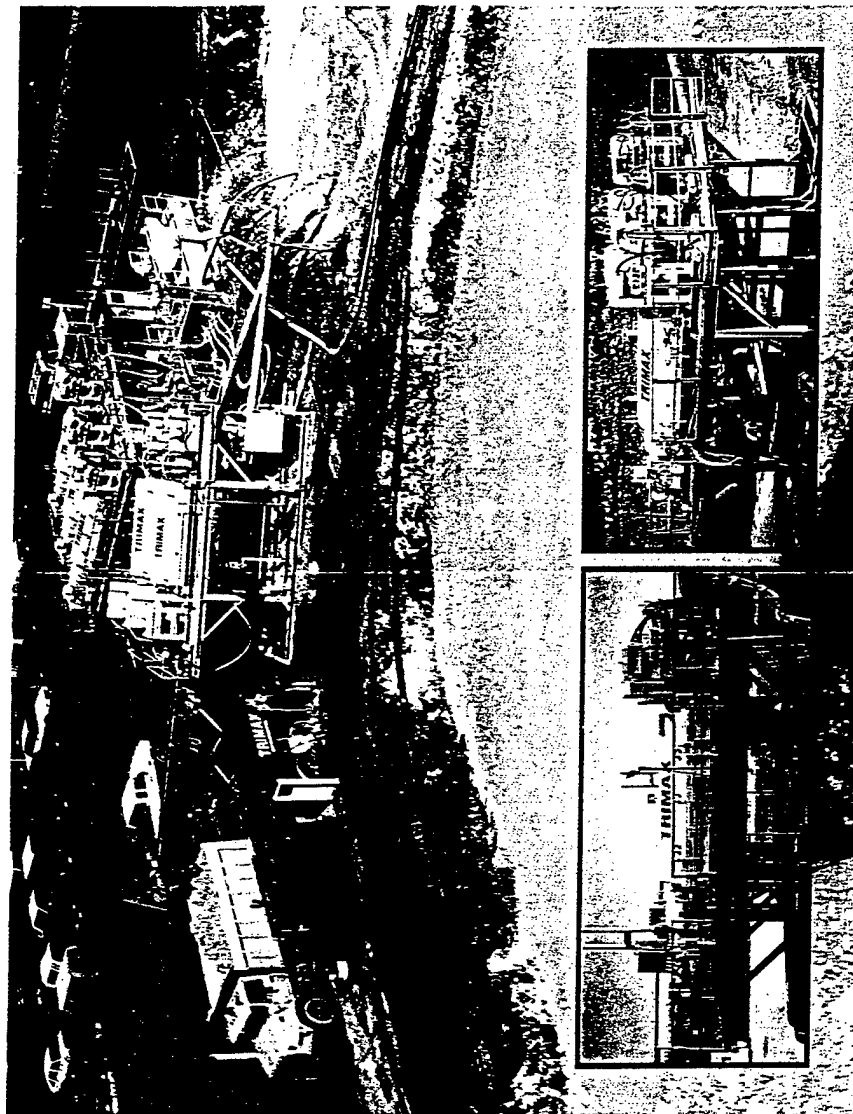
The TRIMAX fleet of trailer units are the perfect answer to any size project. These units are self contained, complete with pumps, grinders and polymer make-down systems. With up to 4000 + "G", our VFD controlled high speed decanter centrifuges are capable of producing the driest cake solids in the industry on primary and secondary sludges. Emergency or regular maintenance, the trailer units are a cost effective method of handling any dewatering requirements.



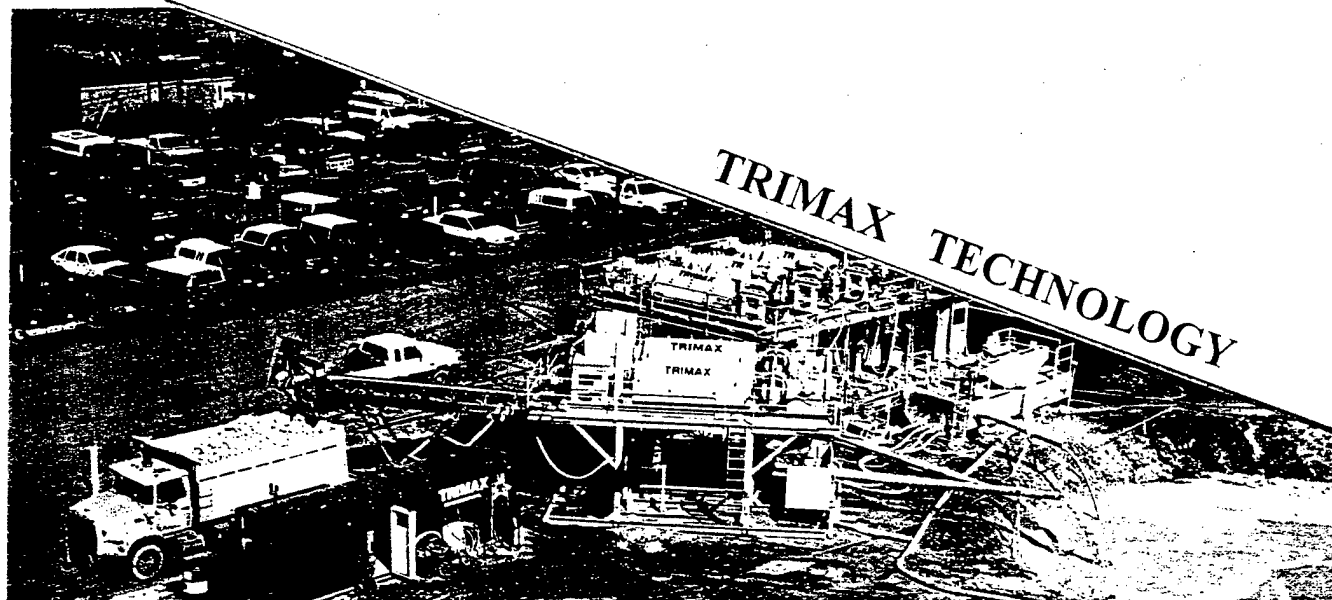
Mobile trailer units can respond quickly and help keep project costs low.

Flexibility

All of the TRIMAX equipment is mobile and modular. Every project has different requirements and our system is designed to adapt. Time, space and economics are key factors to most TRIMAX clients. Single or multiple machine set-ups give TRIMAX the flexibility to meet our customers varied dewatering needs and project schedule. Trained, experienced personnel allow TRIMAX to make quick adjustments to changing conditions.



Multiple unit installations add flexibility while increasing production.



Centrifuge turnkey project

TRIMAX utilizes high speed horizontal decanter centrifuges equipped with Variable Frequency Drives (VFD's) to supply its mobile dewatering service. This along with all the ancillary equipment allows TRIMAX the ability to supply a turnkey project. The centrifuge technology is not new, however for some of its applications it is. The VFD's allow our technicians to achieve optimal cake dryness on a variety of different types of sludges. The high "G" force generated by the centrifuges produces a cake up to 25% greater than other technologies.

High throughput along with stainless steel bowls and sintered tungsten carbide conveyor flygting enable TRIMAX to keep production and maintenance costs low while reducing sludge volumes and odour.

The solids are continuously separated from the liquid in the centrifuge which virtually eliminates any handling by our personnel. The number of machines in our fleet enable TRIMAX to process with multiple machine installations that result in a clean, fast and economical project.



TRIMAX advantage:

- advanced technology
- dryer cake
- less time
- more economical

TRIMAX ENVIRONMENTAL Services Ltd. 1-800-465-2115

Appendix E: N-Viro

Design Criteria		
5/12/97		
1 Dry Tons Per Day - Windrow Technology		
20% TOTAL SOLIDS, 5 DAYS/WEEK, 8 HRS/DAY		
		120 DT/DAY
Sludge Production (wet tons per day)		5
Sludge Cake (Percent Total Solids)		20%
Sludge Production (dry tons per day)		1
Percent Total Solids of Mixture (%TS) (1)		48
Alkaline Admixture Dosage (%)		54
Alkaline Admixture Usage(Tons per Day)		2.69
(Tons of mixture per hour per mixer)		3.85
Dryer Feed (Tons per Day)	NA	8
(Tons per hour per dryer)	NA	3.85
Operating Hours per Day		1
Average Product (%TS) (2)		62
Product Amount (Wet Tons per Day)		5.96
Water Evaporated (Lb per Hour per Dryer)	NA	1,737
Total BTU Consumption (Million BTU per Day)	NA	5
Air Flow per dryer (Cubic Feet per Minute)	NA	40,000
CKD Density (lb/ft ³)		55
CKD Silos (ft ³)		294
Silo capacity each (6 silos) (ft ³)		49
Number of days of CKD storage		3.00
Mixer and Dryer Sizing		1-CSP-10
NOTES:		
(1) Can range from 42-48% TS feed to dryer.		
(2) Can range from 62-68% TS product.		

Cost Summary 5/12/97 1 Dry Tons Per Day - Windrow Technology 20% TOTAL SOLIDS, 5 DAYS/WEEK, 8 HRS/DAY		
CAPITAL COSTS	Cost (\$)	
1. Building and Sitework		\$255,946
2. Stationary Equipment		\$438,340
3. Air Treatment Venturi and Duct		\$0
4. Mobile Equipment		\$87,000
5. Engineering		\$50,000
6. Contingencies (6.5%)		\$56,155
7. Technology Fees (1-Time Payment)		\$80,000
Total Estimated Capital Costs		\$967,441
Amortized Capital Costs @ 9% over 20 Years	\$407.61	\$105,980
ANNUAL O&M COSTS	Unit cost (\$/DTsludge)	Cost (\$)
Facilities Manager	\$0.00	\$0
Operating Labor (\$20/hr)	\$120.00	\$31,200
Equipment Maintenance	\$50.58	\$13,150
Natural Gas for Dryer (\$4.5/mmbtu)	\$0.00	\$0.00
Natural Gas for Building	\$7.69	\$2,000
Electricity (\$0.08/kwh)	\$138.46	\$35,999
Product Distribution (\$5/ton)	\$35.73	\$9,290
CKD (\$10/ton)	\$26.92	\$7,000
Fuel, Lubricants,Misc	\$6.25	\$1,625
Scrubber Chemicals	\$0.00	\$0
QA/QC	\$10.00	\$2,600
Sludge Delivery (\$0/Wet Ton)	\$0.00	\$0
Total Estimated O&M Costs	\$395.63	\$102,864
UNIT COSTS	9% Interest 20 Year Payback	
Wet Tons of Sludge per Year		1,300
Total Cost per Wet Ton		\$160.65
Dry Tons of Sludge per Year		260
Total Cost per Dry Ton		\$803.25
Product Tons per Year		1,548

Capital Cost Estimating Worksheet					
4/15/97					
1 Dry Tons Per Day - Windrow Technology					
20% TS, 5 DAYS/WEEK, 8 HRS/DAY					
DESCRIPTION	UNIT	UNIT COST (\$/LOT)	LOT	CONTRACT MARKUP	TOTAL (US \$)
1. Process Building (40x50)(See Note 1)	sf	\$25.00	2,000	1.1	\$55,000.00
(a) Control Room	ls	\$0.00	0	1.1	\$0.00
(b) Site Preparation and Access Roads	sf	\$10.00	2,300	1.1	\$25,300.00
(c) Offices and restrooms	ls	\$10,000.00	1	1.1	\$11,000.00
(d) HVAC	sf	\$6.00	3,200	1.1	\$21,120.00
(e) Windrow Building (60 x 50)	sf	\$12.00	3,000	1.1	\$39,600.00
(F) Product Storage (60x50)(90 days)	sf	\$12.00	3,000	1.1	\$39,600.00
2. Reinforced Concrete					
(a) Equipment Foundations	yd ³	\$250.00	20	1.1	\$5,500.00
(b) Heat Pulse Cells (6 cells @ 10x10x2)	yd ³	\$250.00	10	1.1	\$2,750.00
(c) Sludge Unloading Ramp	yd ³	\$250.00	0	1.1	\$0.00
(d) Windrow and Storage bldg perimeter wall	yd ³	\$250.00	0	1.1	\$0.00
3. Site utilities					
(a) Electric Service	ls	\$2,000.00	1	1.0	\$2,000.00
(b) Natural Gas	ls	\$2,000.00	1	1.1	\$2,200.00
(c) Telephone	ls	\$2,000.00	1	1.1	\$2,200.00
(d) Water	ls	\$2,000.00	1	1.1	\$2,200.00
4. Sanitary Sewer Service					
(a) Sanitary Sewers	lf	\$50.00	100	1.1	\$5,500.00
(b) Storm Sewers	lf	\$40.00	200	1.1	\$8,800.00
5. Live bottom bin(40 cyd)	ea	\$115,000.00	0	1.1	\$0.00
(a) Installation (20%)	ea	\$0.00	1	1	\$0.00
6. Belt Conveyor to Mixer					
(a) Equipment	lf	\$600.00	40	1.1	\$26,400.00
(b) Installation (30%)	ea	\$7,920.00	1	1	\$7,920.00
7. Mixer (10 WT per hour)	ea	\$150,000.00	1	1.1	\$165,000.00
(a) 1200 ft3 silos	ea	\$48,000.00	2	1.1	\$105,600.00
(b) 2100 ft3 silo	ea	\$31,000.00	0	1.1	\$0.00
(c) Transfer Augers	ea	\$10,700.00	2	1.1	\$23,540.00
(d) Portable Platform	es	\$2,000.00	2	1.1	\$4,400.00
(e) Mixer Installation @15 %	ea	\$24,750.00	1	1	\$24,750.00
(f) Silo Installation @25 %	ea	\$26,400.00	1	1	\$26,400.00
8. Truck Scale					
(a) Equipment	lf	\$110,000.00	0	1.1	\$0.00
(b) Installation (40%)	ea	\$0.00	1	1	\$0.00
9. Belt Conveyor to Dryer					
(a) Equipment	lf	\$600.00	0	1	\$0.00
(b) Installation (40%)	ea	\$0.00	1	1	\$0.00
10. Belt Conveyor to Heat Pulse Cells	lf	\$600.00	40	1.1	\$26,400.00
(a) Installation (40%)	ea	\$10,560.00	1	1	\$10,560.00

11. Dryer (CSD-10,000)	ea	\$442,250.00	0	0	\$0.00
(a) Installation (15%)	ea	\$0.00	0	0	\$0.00
12. Product stacking conveyor	ea	\$22,500.00	0	1.1	\$0.00
13. Odor Control					
(a) Windrow Building	cfm	\$6.00	0	1.1	\$0.00
Scrubber installation (20%)		\$0.00			\$0.00
(b) Storage Building	cfm	\$6.00	0	1.1	\$0.00
Scrubber installation (20%)	ls	\$0.00		1	\$0.00
14. Dryer Odor Control (30,000 cfm from dryer)					
(a) Condenser/Venturi/drop out vessel	cfm	\$8.00	12,000	0	\$0.00
(b) 2-stage scrubber	cfm	\$13.00	65,000	0	\$0.00
(c) Ductwork	lf	\$500.00	200	0	\$0.00
(e) Scrubber/Duct/ Venturi Install.(20%)	ls	\$191,000.00	1	0	\$0.00
15. On-site Electrical and Lighting					
(a) Service Entrance and Feeders	ea	\$60,000.00	0	1.1	\$0.00
(b) Switchgear	ls	\$80,000.00	0	1.1	\$0.00
(c) Lighting (Process Bldg)	sf	\$5.00	1,000	1.1	\$5,500.00
(d) Lighting (Storage area)	sf	\$1.00	500	1.1	\$550.00
(e) Motor Wiring					
5 hp motors	ea	\$2,080.00	1	1.1	\$2,288.00
10 hp motors	ea	\$2,250.00	0	1.1	\$0.00
20 hp motors	ea	\$2,980.00	1	1.1	\$3,278.00
50 hp motors	ea	\$4,800.00	1	1.1	\$5,280.00
100 hp motors	ea	\$6,500.00	1	1.1	\$7,150.00
200 hp motors	ea	\$8,300.00	1	1.1	\$9,130.00
(f) Central control system	ls	\$100,000.00	0	1.1	\$0.00
(g) MCC Panels	ls	\$30,000.00	0	1.1	\$0.00
16. Freight	load	\$10,000.00	3	1	\$30,000.00
17. Mobile Equipment					
(a) Front end loader	ea	\$50,000.00	1	1	\$50,000.00
(b) Bobcat	ea	\$25,000.00	1	1	\$25,000.00
(c) Scarrab Windrow	ea	\$12,000.00	1	1	\$12,000.00
18. Lab Equipment	ls	\$20,000.00	1	1	\$20,000.00
19. Engineering (Design and Const. Mgmt.)					\$50,000.00
SUBTOTAL					\$863,916.00
20. Contingency (6.5%)					\$56,154.54
21. N-Viro Technology Fee (1-time payment)	dt/yr	\$80,000.00	1	1	\$80,000.00
22. Equipment Replacement	ls		1	1	\$0.00
TOTAL (U.S. DOLLARS)					\$1,000,070.54
Stationary, Odor Control, Mobile Equipment					\$438,340
Notes:					
(I) Includes pre-engineered, insulated metal building, two overhead doors, foundations, excavation and 6" thick floor slab. Storage building costs include enclosed building with asphalt floors and two overhead doors.					

Operating Cost Estimate

5/12/97

1 Dry Tons Per Day - Windrow Technology
20% TOTAL SOLIDS, 5 DAYS/WEEK, 8 HRS/DAY

INPUT DATA:		
1.00		DRY TONS PER DAY
20%		% TOTAL SOLIDS OF CAKE SLUDGE
5.00		# OF WET TONS PER DAY
260		# OF PROCESSING DAYS
260		# OF DRY TONS PER YEAR
1,300		# OF WET TONS PER YEAR
0.00		\$/MILLION BTU NATURAL GAS
0.08		\$/KWH (INCLUDES USAGE AND DEMAND CHARGES)
1		NUMBER OF EMPLOYEES
-		1000 FT3 OF DIGESTER GAS AVAIL./YR
0		BTU/FT3 OF DIGESTER GAS
10		\$/TON FOR FLYASH
10		\$/TON FOR CKD
70		\$/TON FOR CaO
0		\$/WT FOR SLUDGE DELIVERY
6		\$/WT FOR PRODUCT DISTRIBUTION
10		\$/DT FOR QA/QC
48%		% TOTAL SOLIDS OF MIXTURE
62%		% TOTAL SOLIDS OF PRODUCT
1,548		# OF TONS PER YEAR OF PRODUCT
8		DAILY HOURS OF OPERATION FOR EQUIPMENT
8		DAILY HOURS PER SHIFT
1400		BTU REQUIRED TO EVAP. ONE POUND OF WATER
15		\$/HR FOR OPERATING LABOR
2080		WORKING HOURS PER YEAR PER EMPLOYEE
\$438,340		EQUIPMENT CAPITAL COSTS
3%		%OF EQUIPMENT CAPITAL COST USED FOR MAINTENANCE

CALCULATIONS:

$$\text{VOL. OF AA (TONS/day)} = \frac{(\text{WTsl} * (\% \text{TSmix}/100) - \text{DT/DAYSsl})}{(1 - (\% \text{TSmix}/100))}$$

	TONS/DAY	DOSAGE
	2.69	54%
ASH	0.00	
CaO	0.00	
CKD	2.69	

$$\text{DRYER FEED RATE (LBS/hr)} = \frac{(\text{WT/DAYSsludge} + \text{Tons/dayAA}) * (2000\text{lbs/ton})}{\text{operating hrs/day}}$$

1,923

$$\text{PRODUCT (TONS/day)} = \frac{(\text{WT/DAYsludge} + \text{TONS/DAYAA}) * (\% \text{TSmix} / \% \text{TSpro})}{5.96}$$

$$\text{WATER LOSS (LBS/hr)} = \frac{(\text{WT/Dsl} + \text{TONS/DAYAA} - \text{TONS/DAYpro}) / (\text{HRS/DAY}) * 2000}{434.24}$$

$$\text{DRYER ENERGY REQD (MMBTU/DAY)} = \frac{\text{LBS/hrwater loss} * \text{BTU/LBwater} * \text{HRS/DAY OPER}}{10^6} = 4.86$$

$$\text{BTU/YEAR} = 1.26\text{E}+09$$

$$\text{BTU DIGESTER GAS AVAIL. PER YEAR} = 1000 \text{ FT}^3/\text{YEAR AVAIL.} * 1000 * 600 \text{ BTU/FT}^3 = 0.00\text{E}+00$$

PLANT ELECTRICAL REQUIREMENTS		
N-VIRO PROCESS		
ITEM		MOTOR HP
DRYER DRUM DRIVE	2@50	0
BURNER AIR SUPPLY FAN	2@15	0
MAIN FAN	2@ 200	0
ROTARY AIR LOCK	2@3	0
MIXER	2@75	150
ODOR CONTROL FANS	2@200	0
ODOR CONTROL PUMPS	6@15	0
LIVE BOTTOM BINS	2@30	0
CONVEYOR MOTORS	12@7.5	90
MISCELLANEOUS		50

TOTAL DEMAND 290

OPERATING COSTS	\$/YEAR	\$/DT	\$/WT
FACILITIES MANAGER	\$0	0.00	0.00
OPERATING LABOR	\$31,200	120.00	24.00
EQUIPMENT MAINTENANCE	\$13,150	50.58	10.12
NATURAL GAS FOR DRYER	\$0	0.00	0.00
NATURAL GAS FOR PROCESS BUILDING	\$2,000	7.69	1.54
ELECTRICITY	\$35,999	138.46	27.69
PRODUCT DISTRIBUTION	\$9,290	35.73	7.15
CKD	\$7,000	26.92	5.38
FUEL, LUBRICANTS, MISC	\$1,625	6.25	1.25
SCRUBBER CHEMICALS	\$0	0.00	0.00
QA/QC	\$2,600	10.00	2.00
SLUDGE DELIVERY	\$0	0.00	0.00
ESTIMATED ANNUAL OPERATING COSTS	\$102,864	395.63	79.13

N/I - NOT INCLUDED

<p align="center"> Capital Cost Estimating for Western Corridor (from N-Viro quote) 6/3/1997 0.37 Dry Tons per Day - Windrow Technology 20% TS, 5days/week, 8 hrs/day </p>					
DESCRIPTION	UNIT	UNIT COST (\$/LOT)	LOT	CONTRACT MARKUP	TOTAL (US\$)
1. Process Building	sf	\$25.00	740	1.1	\$20,350.00
(a) Control Room	ls	\$0.00	0	1.1	\$0.00
(b) Site Preparation and Access Roads	sf	\$10.00	850	1.1	\$9,350.00
(c) Offices and restrooms	ls	\$10,000.00	0	1.1	\$0.00
(d) HVAC	sf	\$6.00	1185	1.1	\$7,821.00
(e) Windrow Building	sf	\$12.00	1110	1.1	\$14,652.00
(f) Product Storage (90 days)	sf	\$12.00	1110	1.1	\$14,652.00
2. Reinforced Concrete					
(a) Equipment Foundations	yd ³	\$250.00	8	1.1	\$2,200.00
(b) Heat Pulse Cells (3 cells @ 10x10x2)	yd ³	\$250.00	5	1.1	\$1,375.00
(c) Sludge Unloading Ramp	yd ³	\$250.00	0	1.1	\$0.00
(d) Windrow and Stoage bldg perimeter wall	yd ³	\$250.00	0	1.1	\$0.00
3. Site Utilities					
(a) Electric Service	ls	\$2,000.00	1	1	\$2,000.00
(b) Natural Gas	ls	\$2,000.00	1	1.1	\$2,200.00
(c) Telephone	ls	\$2,000.00	1	1.1	\$2,200.00
(d) Water	ls	\$2,000.00	1	1.1	\$2,200.00
4. Sanitary Sewer Services					
(a) Sanitary Sewers	lf	\$50.00	40	1.1	\$2,200.00
(b) Storm Sewers	lf	\$40.00	75	1.1	\$3,300.00
5. Live bottom bin (40 cyd)	ea	\$115,000.00	0	1.1	\$0.00
(a) Installation (20%)	ea	\$0.00	1	1	\$0.00
6. Belt Conveyor to Mixer					
(a) Equipment	lf	\$600.00	15	1.1	\$9,900.00
(b) Installation (30%)	ea	\$2,970.00	1	1	\$2,970.00
7. Mixer (10 WT per hour)	ea	\$150,000.00	1	1.1	\$165,000.00
(a) 1200 ft ³ silos	ea	\$48,000.00	1	1.1	\$52,800.00
(b) 2100 ft ³ silo	ea	\$31,000.00	0	1.1	\$0.00
(c) Transfer Augers	ea	\$10,700.00	1	1.1	\$11,770.00
(d) Portable Platform	ea	\$2,000.00	1	1.1	\$2,200.00
(e) Mixer Installation (15%)	ea	\$24,750.00	1	1	\$24,750.00
(f) Silo Installation (25%)	ea	\$13,200.00	1	1	\$13,200.00
8. Truck Scale					
(a) Equipment	lf	\$110,000.00	0	1.1	\$0.00
(b) Installation (40%)	ea	\$0.00	1	1	\$0.00
9. Belt Conveyor to Dryer					
(a) Equipment	lf	\$600.00	0	1	\$0.00
(b) Installation (40%)	ea	\$0.00	1	1	\$0.00

10. Belt Conveyor to Heat Pulse Cells	lf	\$600.00	15	1.1	\$9,900.00
(a) Installation (40%)	ea	\$3,960.00	1	1	\$3,960.00
11. Dryer (CSD-10,000)	ea	\$442,250.00	0	0	\$0.00
(a) Installation (40%)	ea	\$0.00	1	1	\$0.00
12. Product stacking conveyor	ea	\$22,500.00	0	1.1	\$0.00
13. Odor Control					
(a) Windrow Building	cfm	\$6.00	0	1.1	\$0.00
Scrubber Installation (20%)		\$0.00	1	1	\$0.00
(b) Storage Building	cfm	\$6.00	0	1.1	\$0.00
Scrubber Installation (20%)		\$0.00	1	1	\$0.00
14. Dryer Odor Control					
(a) Condenser/Venturi/drop out vessel	cfm	\$8.00	4440	0	\$0.00
(b) 2-stage scrubber	cfm	\$13.00	24050	0	\$0.00
(c) Ductwork	lf	\$200.00	75	0	\$0.00
(d) Scrubber/Duct/Venturi Installtn (20%)	ls	\$0.00	1	0	\$0.00
15. On-site Electrical and Lighting					
(a) Service Entrance and Feeders	ea	\$60,000.00	0	1.1	\$0.00
(b) Switchgear	ls	\$80,000.00	0	1.1	\$0.00
(c) Lighting (Process Bldg)	sf	\$5.00	370	1.1	\$2,035.00
(d) Lighting (Storage Area)	sf	\$1.00	185	1.1	\$203.50
(e) Motor Wiring					
5 hp motors	ea	\$2,080.00	1	1.1	\$2,288.00
10 hp motors	ea	\$2,250.00	0	1.1	\$0.00
20 hp motors	ea	\$2,980.00	1	1.1	\$3,278.00
50 hp motors	ea	\$4,800.00	1	1.1	\$5,280.00
100 hp motors	ea	\$6,500.00	1	1.1	\$7,150.00
200 hp motors	ea	\$8,300.00	1	1.1	\$9,130.00
(f) Central control system	ls	\$100,000.00	0	1.1	\$0.00
(g) MCC Panels	ls	\$30,000.00	0	1.1	\$0.00
16. Freight	load	\$10,000.00	2	1	\$20,000.00
17. Mobile Equipment					
(a) Front end loader	ea	\$50,000.00	0	1	\$0.00
(b) Bobcat	ea	\$25,000.00	1	1	\$25,000.00
(c) Scarrab Windrow	ea	\$12,000.00	1	1	\$12,000.00
18. Lab Equipment	ls	\$20,000.00	1	1	\$20,000.00
19. Engineering (Design and Const. Mgmt.)					\$50,000.00
SUBTOTAL					\$537,314.50
20. Contingency (6.5%)					\$34,925.44
21. N-Viro Technology Fee (1-time payment)	dt/yr	\$80,000.00	0.37	1	\$29,600.00
22. Equipment Replacement	ls		1	1	\$0.00
TOTAL (U.S. DOLLARS)					\$601,839.94

**O&M COST ESTIMATING FOR WESTERN CORRIDOR
(from N-Viro quote)**

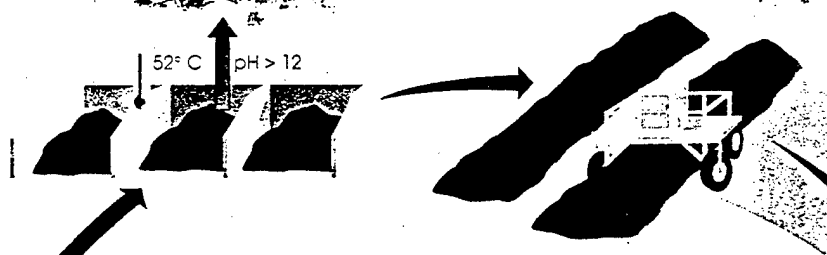
ANNUAL O&M COSTS	Unit cost (\$/DT sludge)	Cost (\$)
Facilities Manager	\$0.00	\$0
Operating Labor (\$20/hr)	\$120.00	\$11,544
Equipment Maintenance	\$50.58	\$4,866
Natural Gas for Dryer (\$4.5/mmbtu)	\$0.00	\$0
Natural Gas for Building	\$7.69	\$740
Electricity (\$0.08/kwh)	\$138.46	\$13,320
Product Distribution (\$5/ton)	\$35.73	\$3,437
CKD (\$10/ton)	\$26.92	\$2,590
Fuel, Lubricants, Misc	\$6.25	\$601
Scrubber Chemicals	\$0.00	\$0
QA/QC	\$10.00	\$962
Sludge Delivery (\$0/Wet ton)	\$0.00	\$0
Total Estimated O&M Costs	\$395.63	\$38,060

A Process So Simple...

The N-Viro Process

1a. and b. Mixing

Dewatered sludge, between 16 and 35 percent solids, is mixed with N-Viro's alkaline admixture composed of cement kiln dust and other alkaline by-products. The admixture's extremely fine particle size and high surface area promote odor absorption, granularity and structure.



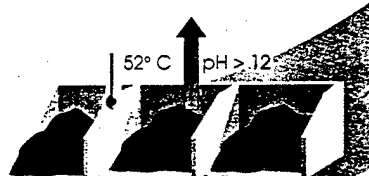
2a. Chemical Heat Pulse

A chemical reaction, or heat pulse, occurs between the sludge and the alkaline admixture raising the temperature and pH level. This reaction, combined with other stresses,

kills disease-causing bacteria and pathogens and eliminates noxious odors.

Strict temperature control ensures the survival of valuable and useful microflora.

3b. Chemical Heat Pulse



2b. Accelerated Mechanical Drying

When utilizing the Accelerated Mechanical Drying option, the blended material is fed directly into the dryer, prior to the heat-pulse phase. In the dryer, excess moisture is removed in a matter of minutes, while stringent process control is maintained. After exiting the dryer, the material undergoes the normal heat-pulse step.

This mechanical drying system is completely enclosed, dramatically reducing processing time, and uses a fraction of the floor space.

b.



3a. Traditional Windrow Drying

After the 12-hour Chemical Heat Pulse, the mixture is arranged in neat windrows for turning. Typically, windrow drying takes 3 - 7 days, depending on the characteristics desired in the finished product.

N-Viro International Corporation's patented pasteurization technology recycles wastewater sludge and other waste streams rich in organics into a safe, valuable product that can be beneficially reused in many ways. That product, N-Viro Soil™, is a granular, soil-like, material that has excellent appearance, physical and biological characteristics.

The N-Viro Process, or Advanced Alkaline Stabilization with Subsequent Accelerated Drying (AASSAD), is a straight-forward methodology recognized around the world. The process flow diagram above illustrates the basic steps involved in N-Viro's

technology, including the two methods for achieving Accelerated Drying: windrowing, the traditional approach, and N-Viro's mechanical drying option.

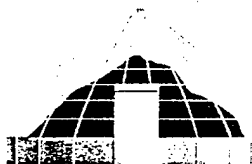
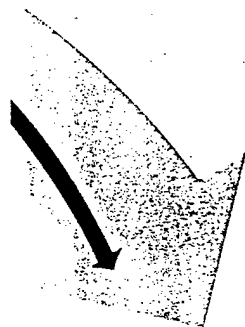


...A Product So Valuable!

ACCELERATED DRYING

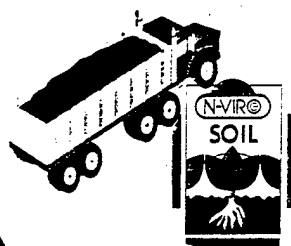
Accelerated Drying is an integral part of producing a marketable, soil-like product. The primary objective of this phase is to remove excess moisture and promote the granularity and physical stability of the final product. In addition, Accelerated Drying provides for continued mixing, carbonation of residual calcium hydroxide and the removal of volatile emissions in a controlled environment.

N-Viro's technology offers two drying options that reduce sludge volume, promote granularity and the physical stability of the final N-Viro Soil product. These two options are traditional Windrow Drying and Accelerated Mechanical Drying.



4a. and b. Storage

The ability to store product is critical to the success of any distribution program for large volumes of organic materials. Because of its stability, N-Viro Soil can be safely stored for extended periods in the open or under roof, making it ideal for seasonal use.



5a. and b. Distribution/Use

When needed, N-Viro Soil is easily shipped in bags or by the truckload. N-Viro Soil's physical characteristics are tailored to its utilization in standard materials handling equipment.

N-Viro's patented process is a simple, cost-effective approach to the beneficial reuse of wastewater sludge and other organic waste streams. The final product, N-Viro Soil, is accepted and marketed in countries around the globe.

N-Viro Soil meets one of the world's most stringent regulations for disinfection of sludge-derived products. United States Environmental Protection Agency 40 CFR, part 503. These guidelines establish criteria for "Exceptional Quality Sludge" products.

Around the world, communities are implementing successful reuse programs using N-Viro's technology.

N-Viro Soil is ideal for use in agricultural and horticultural projects because it is safe, inexpensive and achieves the highest level of odor control.

SAFE

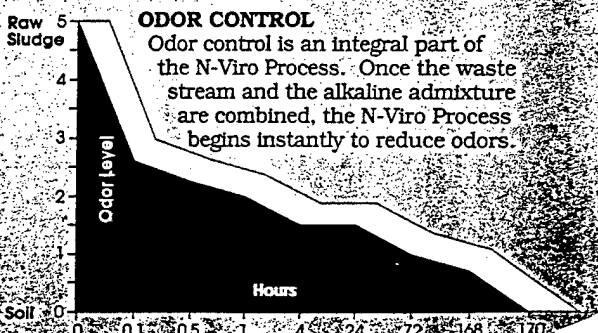
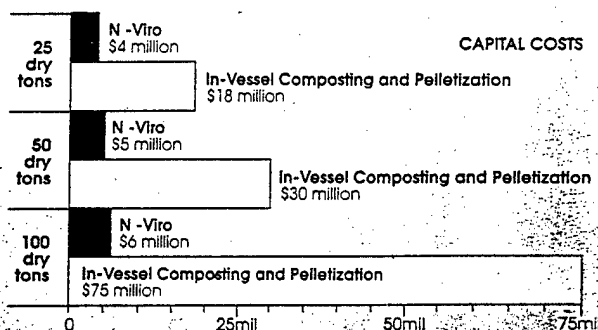
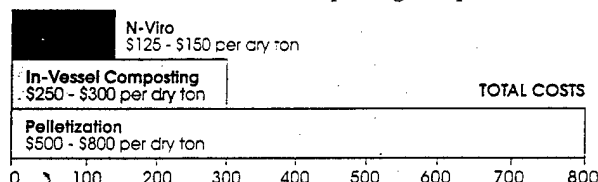
The N-Viro Process yields a product that meets the U.S. EPA's "Exceptional Quality Sludge" criteria, achieving the highest level of pathogen kill while maintaining valuable indigenous microflora.

Untreated Sludge*	PSRP Treated**	PFRP Treated*** (N-VIRO®)
1 million/100 ml	Fecal Coliforms 100,000/100 ml	≤ 3/100 ml
500 CFU/100 ml	Salmonella Species 5 CFU/100 ml	≤ 3 CFU/100 ml
1,000 PFU/100 ml	Animal Virus 100 PFU/100 ml	≤ 1 PFU/100 ml
10 Viable eggs/100 ml	Helminth Eggs (Ascaris) 10 Viable eggs/100 ml	< 1 Viable eggs/100 ml

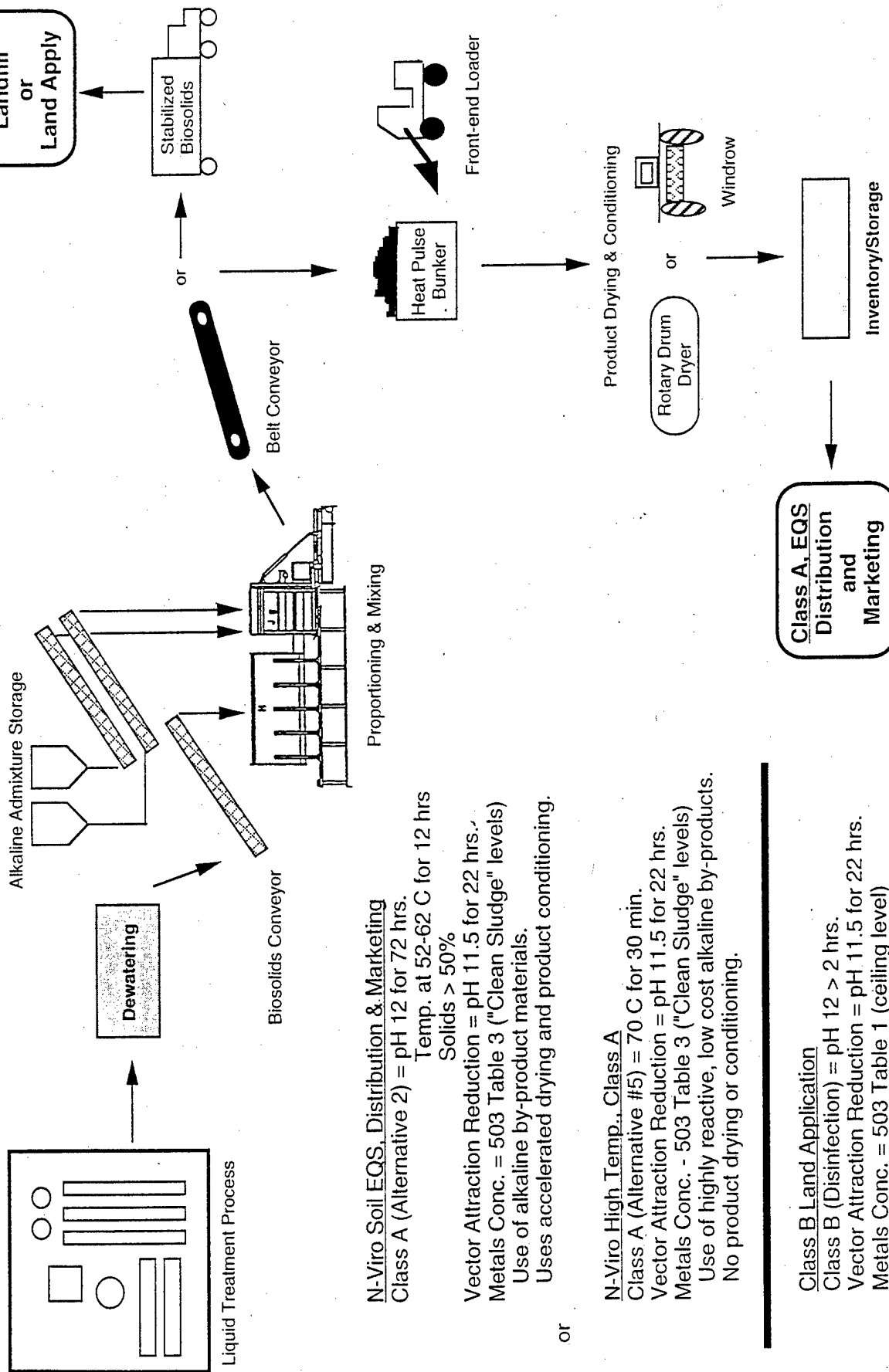
*Untreated Sludge = 100% average level of pathogen reduction. **PSRP = Process to Significantly Reduce Pathogens. ***PFRP = Process to Further Reduce Pathogens. CFU = Colony Forming Units. PFU = Plaque Forming Units.

INEXPENSIVE

N-Viro's capital and operating costs have been demonstrated to be considerably lower than other EQS processes, such as in-vessel composting and pelletization.



Process Schematic for a Typical N-Viro Processing Facility



or

N-Viro High Temp., Class A

Class A (Alternative #5) = 70 C for 30 min.

Vector Attraction Reduction = pH 11.5 for 22 hrs.

Metals Conc. - 503 Table 3 ("Clean Sludge" levels)

Use of highly reactive, low cost alkaline by-products.

No product drying or conditioning.

Class B Land Application

Class B (Disinfection) = pH 12 > 2 hrs.

Vector Attraction Reduction = pH 11.5 for 22 hrs.

Metals Conc. = 503 Table 1 (ceiling level)

Appendix F: CemenTech

cemen tech

Leaders In Volumetric Proportioning
And Continuous Mixing Systems
1100 North 14th Street • Indianola, Iowa 50125
Phone: 800 / 247-2464 or 515 / 961-7407 • FAX 515 / 961-7409

March 24, 1997

Ms. Amy Swanson
USA-CERL
PO Box 9005
Champaign, IL 61826

(800)USA-CERL X4464

Dear Amy:

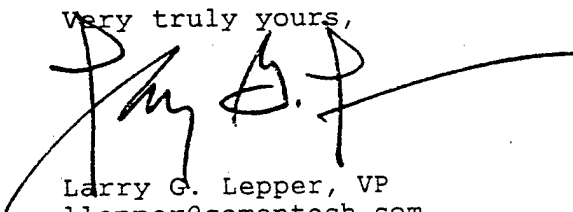
Attached is the information you requested on our smallest class A lime stabilization system, the Model CSP-5 CAKE SLUDGE PROCESSOR. The system is capable of processing up to 5 total tons per hour of dewatered cake sludge and alkaline material. I am making a few assumptions which are:

1. You will do a lime/high heat class A stabilization process. This involves raising the temperature of the sludge to 70°C for 30 min.; and raising the pH to 12 for 2 hours and 11.5 for an additional 22 hours.
2. Because of the very small quantity you will be processing, manual operating controls are quoted.
3. No bulk material silo is quoted. You would use bagged lime in Korea.
4. The quantity of sludge to be processed is 0.365 dry tons per day dewatered to 20% dry solids content. This equates to 1.83 wet tons per day.

The only concern I have is the method you will be using to load the sludge hopper on the CSP-5. I assume you plan on having a belt filter press in conjunction with the CSP. The liquid would be hauled to this site for dewatering and the discharge of the belt filter press would be onto a conveyor that discharges into the sludge hopper on our unit.

Budget pricing for a CSP-5 unit as above and attached is \$59,877 fob factory. Freight, start up, etc. would be additional. If you have any questions, feel free to contact me.

Very truly yours,



Larry G. Lepper, VP
llepper@cementech.com
www.cementech.com

ce-men tech

Leaders In Volumetric Proportioning
And Continuous Mixing Systems

1100 North 14th Street • Indianola, Iowa 50125

Phone: 800 / 247-2464 or 515 / 961-7407 • FAX 515 / 961-7409

Page 1 of 3

CAKE SLUDGE PROCESSOR MODEL CSP-5 PURCHASE INFORMATION

1996

STANDARD EQUIPMENT

- * Sludge Processing Dispenser unit designed to proportion and mix cake sludge and alkaline admixtures. These sludges will typically be in the range of 12 to 30% solids content.
- * Maximum production rate of 1-5 total tons per hour. Maximum production rate will depend upon physical characteristics of the particular sludge being processed.
- * Hydraulic operation of sludge feed and mixer by multi-section fixed displacement hydraulic pump. All functions variable speed. 50 gal. hydraulic oil reservoir. Water to oil hydraulic oil cooler. Adjustable thermostatically controlled water on/off valve for standard shell and tube type cooler.
- * 4 ft. long, 62 cu. ft. capacity sludge bin. Single agitator assembly in bins to promote positive flow of cake sludge to the metering auger. Variable output up to 4 wet tons per hour. 9" diameter variable speed sludge metering auger. Calibration chute included.
- * 12" diameter steel flighting in 7 ft. long mixer assembly with bolt on NI-HARD cast steel wear blades for extended wear life. Hydraulic cylinder hoist. Variable speed up to 300 rpm.
- * 55 cu. ft. dry alkaline materials bin. Automatically controlled air "diffusion" system with adjustable cycle times. Bin level indicators to control feed auger from silo. Visual level windows. The alkaline materials bin(s) is equipped with a manually controlled pneumatic vibrator. Calibration chute included. Metering by 1 HP variable frequency electric drive.
- * 25 HP, 3 phase, 460 V. electric motor. Includes main disconnect, motor starter, and control circuit transformer. Digital readout of both rate (lbs./min.) and total (lbs.) for sludge and alkaline materials.
- * Jib Crane (500 lbs. capacity) mounted above mixer for removal of mixer for calibration. Hand operated. 170 degrees swing.

Page 2 of 3

CSP-5 Purchase Information

OPTIONAL EQUIPMENT

- () SECOND ALKALINE MATERIAL SILO, BIN AND METERING SYSTEM consisting of:

1000 cu. ft. alkaline materials silo, 8 ft. diameter. Auger feed to unit with 15 ft. long, 6 in. dia. auger. (Other lengths available.) Silo includes 100 sq. ft. baghouse, fill pipe adapter, air pads, ladder & safety cage and visual fill level windows.

A second 27.5 cu. ft. dry alkaline materials bin is added by dividing the standard bin into two equal parts. Automatically operated air diffusion system with adjustable cycle times is included along with bin level indicators to control feed auger from silo. Visual level windows and a manually controlled air vibrator are included.

- () AIR COMPRESSOR with refrigerated air dryer. 3 hp, 3 phase, 460 Volt TEFC motor, air compressor with 30 gallon reservoir. Includes motor starter and controls. Free standing.
- () AIR TO OIL COOLER for hydraulic oil. Includes motor controls, mounting and piping. 50,000 btu capacity. Required in areas where water is not available for the standard water to oil cooler. Adjustable thermostatic control of cooler operation. This option is in lieu of standard water/oil cooler.
- () AUTOMATED FEED CONTROL (PLC) allows the operator to input production rates from a key pad. The system includes a PLC, proportional hydraulic valves, feedback loops, and password lockout. The system also includes potentiometer manual overrides and can be calibrated in English or Metric units.
- () COMPUTERIZED RECORDATION SYSTEM This system facilitates continuous recordation of materials usage. The system is configured for multiple inputs and outputs in ASCII code and visual formats and is readable by most standard word processing programs. The system includes a color monitor, full keyboard, CPU, hard drive, printer, and fifty feet of remote cable. The system must be housed in a controlled environment.

* OPTIONAL LARGER SILO UPGRADES:

- () 1200 cu. ft. capacity, 8 ft. diameter.

- () 2100 cu. ft. capacity, 10 ft. diameter.

For larger silos, contact factory.

- () Spread base to make silo free standing. (Not available on 10 ft. diameter silos)

Page 3 of 3

CSP-5 Purchase Information

- () Silo Trailer Package: Includes tongue and 2 axles for portability, electric brakes, brake controller, tail lights, spare tire and rim. (Not available on 10 ft. diameter silos.)
- () Self Erecting Silo System: Includes 5 HP gasoline engine, hydraulic pump & reservoir, 2 each hydraulic lift cylinders, tandem axle trailer, with electrical brakes, brake controller, tail lights, spare tire and rim, pintel hitch. (Not available on 10 ft. diameter silos.)
- () High Efficiency Baghouse: Reverse-Pulse baghouse for high usage applications or where spurious dust is undesirable. 243 sq. ft. filter area. Requires 2 cfm compressed air and 110V AC power. Provides continuous cleaning of filter media even while filling from pneumatic tanker.

SPARE PARTS:

- () Spare parts kit.
- () CSP-5 spare mixer assembly (Complete)

PATENT NO. 4,981,600, OTHER U.S. AND FOREIGN PATENTS PENDING"
9605_USA.PUR

Cake Sludge Processor Systems

Biosolids from Wastewater Cake Sludge

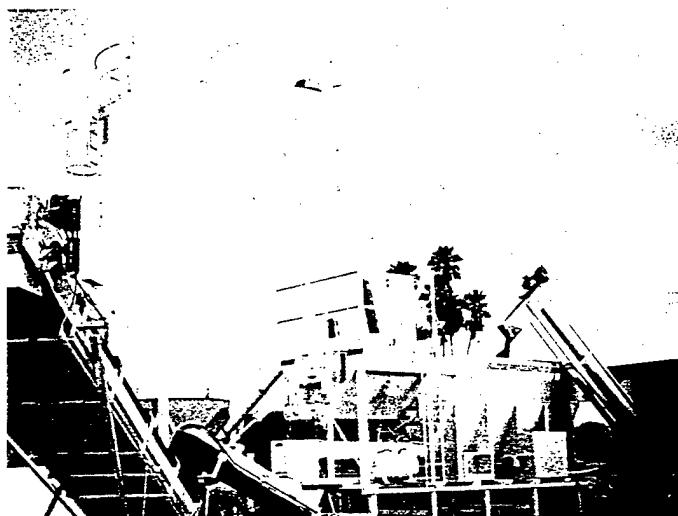
Cemen Tech Inc., a world leader in designing, manufacturing and marketing volumetric proportioning and continuous mixing systems has created a full line of biosolids processing equipment.

The Cake Sludge Processor (CSP) Series

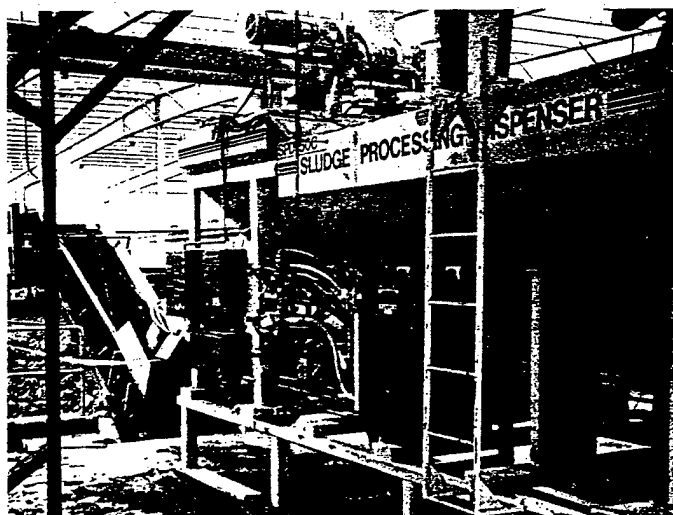
The CSP Series is designed to accurately proportion and blend wastewater cake sludge (ranging from 12 percent to 40 percent solids content) with any single alkaline material or any combination of alkaline materials at output rates of five to 50 tons per hour of total mixed material.

The CSP Series begins with the CSP-10 which is capable of blending up to 10 total tons per hour of wastewater cake sludge and alkaline material(s). The CSP-30 follows and will blend up to 30 total tons per hour. The CSP-50 completes the series and will blend up to 50 total tons per hour.

Cemen Tech designs and manufactures complete systems for processing cake and liquid sludge including bulk materials silos, conveying, proportioning and blending systems, sludge surge hoppers, and complete control and data recordation systems.



CSP-30
Florida



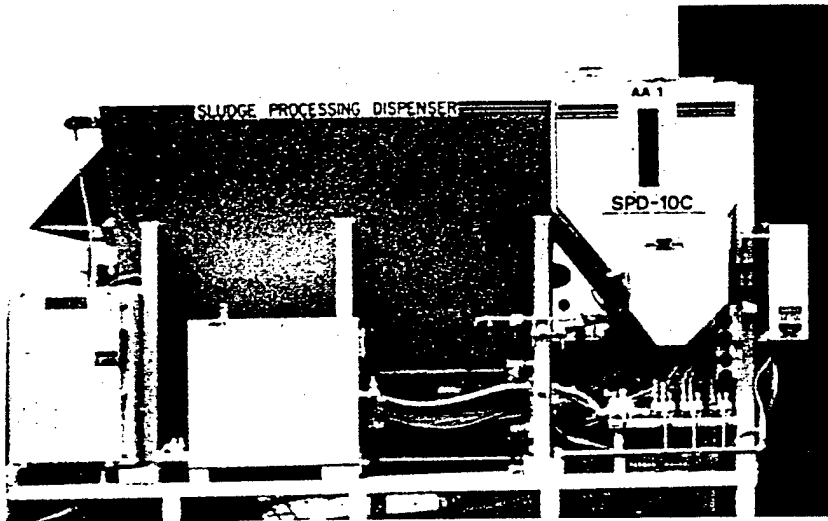
CSP-50
New Jersey

When your sludge management plan calls for alkaline stabilization and pasteurization rely on CEMEN TECH CAKE SLUDGE PROCESSORS.

ce-men-tech INC.

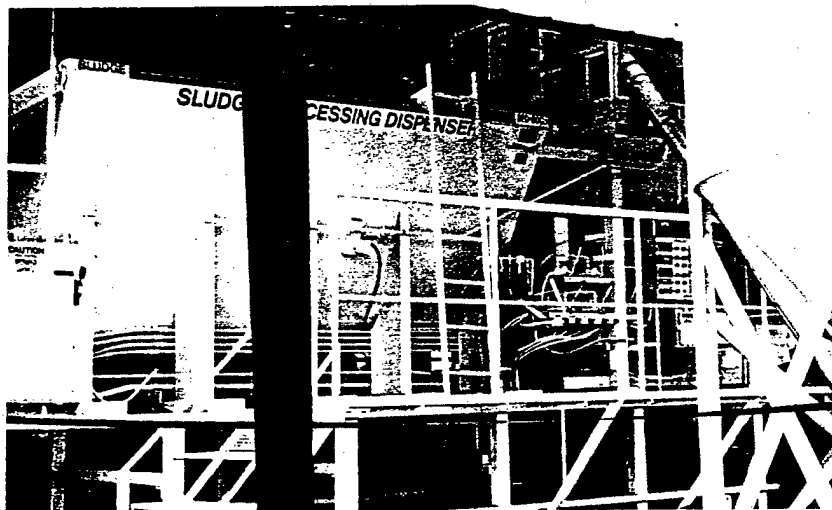
1100 North 14th Street, Indianola, IA 50125
Phone 515-961-7407 • Toll-free 1-800-247-2464 • FAX 515-961-7409

Features



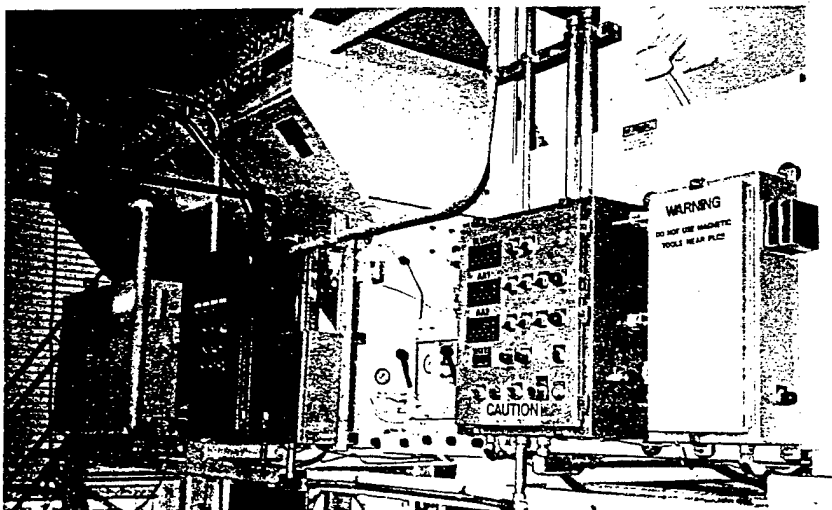
CSP-10

- Production rate of 2-10 total tons per hour.
- 125 cu. ft. capacity sludge bin.
- 50 gallon hydraulic oil reservoir.
- 9" variable speed sludge metering auger.
- 12" dia. 7 ft. long mixer assembly.
- 55 cu. ft. alkaline material bin.
- 30 hp, 3 phase, 460 V. electric motor.



CSP-30

- Production rate of 15-30 total tons per hour.
- 235 cu. ft. capacity sludge bin.
- 75 gallon hydraulic oil reservoir.
- 12" variable speed sludge metering auger.
- 12" dia. 7 ft. long mixer assembly.
- 75 cu. ft. alkaline material bin.
- 50 hp, 3 phase, 460 V. electric motor.

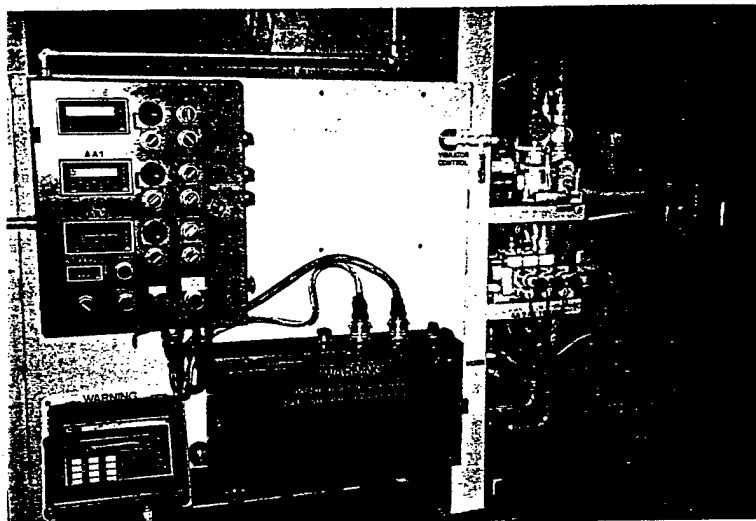


CSP-50

- Production rate of 15-50 total tons per hour.
- 250 cu. ft. capacity sludge bin.
- 85 gallon hydraulic oil reservoir.
- 16" variable speed sludge metering auger.
- 16" dia. 7 ft. long mixer assembly.
- 85 cu. ft. alkaline material bin.
- 100 hp, 3 phase, 460 V. electric motor.

Automatic Feed Control/Computerized Recordation

A programmable logic controller (PLC) with feedback control system is available on all models. The PLC System allows the operator to enter scale factors and production rates of alkaline materials and cake sludge through a Menu-driven calibration sequence. The system includes a PLC, proportional hydraulic valves, feedback loops and password lock-out. The system also has potentiometer and manual type overrides and control. The Computerized Recordation System allows daily recordation of the alkaline materials usage rates and sludge protection rates. The System is configurable for multiple inputs and outputs in ASCII and visual formats usable by most standard word processing programs. The System includes a color monitor, full keyboard, CPU, hard drive and printer.



Standard Equipment

- All hydraulic operation.
- All functions variable speed.
- Water to oil hydraulic oil cooler.
- Single agitator assembly in sludge bin to promote positive flow of cake sludge to the metering auger.
- Calibration chute.
- Bolt-on NI-HARD cast steel wear blades for extended mixer wear life.
- Hydraulic cylinder hoist.
- Automatically controlled air "diffusion" system.
- Bin level indicators to control feed auger from silo.
- Visual level windows.
- Manually controlled pneumatic vibrator.
- Safety cage with fixed kick plate and chain rails.
- Main disconnect, motor starter, and control circuit transformer.
- Push button control panel with digital readout for sludge and alkaline materials.
- 1000 cu. ft. alkaline materials silo, 8 ft. diameter.
- Safety Shut-Down Cable and Trip Switches.
- Jib Crane for removal of mixer during calibration.
- Ultrasonic level sensor for sludge bin.
- Programmable Logic Controller (PLC) integrates all relay outputs into control circuitry of CSP to provide automatic operation.

Special Features

- Independent hydraulic gearbox drives on sludge feed auger and agitator.
 - Ni-hard cast steel replaceable wear blades on mixer auger.
 - Homogenizing mixer to insure complete blending of sludge and alkaline materials.
 - Positionable pitch segments on sludge agitator allow custom configuration to increase controllability of your sludge.
- Uncollected product support from Camen Tech

Optionals

- Second alkaline material silo, bin and metering system
- Air compressor
- Trailer for portable application of sludge processor
- Air to hydraulic oil cooler
- Automated feed control (PLC)
- Computerized Recordation System
- Silos: 1200 cu. ft. capacity, 8 ft. diameter
2100 cu. ft. capacity, 10 ft. diameter
Spread base to make silo free standing.
- Silo Trailer Package
- Self Erecting Silo System
- High Efficiency Baghouse

Spare Parts

- Spare parts kit
- Spare mixer assembly (complete)

cemen tech

Leaders In Volumetric Proportioning
And Continuous Mixing Systems
1100 North 14th Street • Indianola, Iowa 50125
Phone: 800 / 247-2464 or 515 / 961-7407 • FAX 515 / 961-7409

US EPA APPROVED LIME STABILIZATION/STERILIZATION TECHNIQUES PERFORMED WITH A CEMEN TECH CAKE SLUDGE PROCESSOR

DEC. 20, 1995

GENERAL: A CAKE SLUDGE PROCESSOR is designed to receive dewatered cake sludge of 10% to 35% dry solids from a belt filter press, centrifuge, or similar device, and proportion/mix this sludge with one or more dry alkaline materials (lime), to produce a US EPA "Class A" or "Class B" BIOSOLID.

US EPA CLASSIFICATION	TEMP. REQUIREMENTS		PH REQUIREMENTS		DRY SOL. REQ.	TYPICAL ALKALINE MATERIALS USED FOR THE PROCESS*
	DEG. C.	HOURS	PH	HOURS		
CLASS A HIGH HEAT	70	1/2	12 11.5	2 22	NONE	CALCIUM OXIDE (QUICK LIME) SOME KILN DUSTS
CLASS A AASSAD	> 52	12	12	72	> 50%	FLY ASHES, KILN DUSTS, ETC.
CLASS B	NONE	N/A	12 11.5	2 22	NONE	KILN DUSTS, FLY ASH, CALCIUM HYDROXIDE, ETC.

*NOTE: USING SOME ALKALINE MATERIALS MAY BE COVERED BY PATENTS HELD BY N-VIRO INT.
CORPORATION OF TOLEDO, OH USA.

Appendix G: Davis Industries

U.S. FILTER

U.S. FILTER/DAVIS PROCESS

555 MILL INDUSTRIAL WAY P. O. BOX 1615
CANTON, GA 30114 CANTON, GA 30114
TELEPHONE 770-479-8074 FACSIMILE 770-479-7543

Tuesday, March 25, 1997

Amy Swanson
U.S. Army CERL
P.O. Box 9005
Champaign, IL 61826-9005

Subject: Biosolids Composting Project
U.S. Army- Korea
Sizing and Budget Estimate

Dear Amy:

Enclosed please find a preliminary budget estimate and sizing requirements for a Davis Composting System, **EconoBay** design, for a biosolids composting project to be located in Korea. This design is based on a composting plant to process 0.365 dry tons per day of biosolids at a dry solids content of 20% and using yardwaste as the carbon amendment. We have assumed 60 lbs. per cubic foot for biosolids density and 16 lbs. per cubic foot for yardwaste density in our sizing calculations.

The scope of supply for the compost equipment and a general description of that equipment is contained in the proposal. We anticipate that the building construction, all concrete work, electrical, and access, would be provided under a general contract. As you proceed with your evaluation, we can make scope adjustments as required.

BUDGETARY PRICING

The following is based on average cost for similar size systems:

DAVIS ECONOBAY COMPOST SYSTEM

<u>DTPD</u>	<u>%DS</u>	<u>Bays</u>	<u>Equipment Only</u>	<u>Constructed Cost</u>
0.37 (131TPY)	20%	1	\$ 410,000*	\$ NA

(* Does not include transport to Korea, startup and training)

The footprint of the required building to house the **EconoBay** compost system is shown in the proposal. This building can be either a fully enclosed "Butler" type building or a simple "pole" building depending on plant location, odor concerns, etc. We are unable to provide a constructed cost for the facility in Korea at this time. More information concerning what is included in the "constructed" scope of supply for the **EconoBay**

system is included in the proposal.

We are assuming that some type of vegetative waste from yard trimmings, etc., is available as a bulking agent. Generally speaking, any source of available carbon is acceptable as a bulking agent. As the finished compost will take the physical characteristics of the bulking agent, particle size of the amendment is important. A sawdust type material probably makes the best compost, but a wide variety of amendments are acceptable.

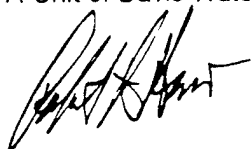
The following is a typical analysis of compost produced by U.S. Filter, Davis Process Composting Systems using sewage sludge (chemical constituents e.g.: copper, zinc, lead, etc., will vary dependent upon industrial contribution to the sewage system).

Moisture:	40 - 50%
pH:	5.5 - 6.5
Nitrogen:	1.0 - 1.7%
Phosphorous:	0.8 - 2.5%
Potassium:	0.1 - 0.4%
Bulk Density:	30 - 40 lbs/cu. ft.

amy, after reviewing this material, please call me with any questions you may have. We appreciate the consideration you have given us and would like to work with you on this project. Our local salesman is Mark McGuire, who can be reached at pager (800) 815-9883.

Very truly yours,

U.S. FILTER, DAVIS PROCESS
A Unit of Davis Water & Waste Industries



Robert H. Harris
Engineering & Operations Manager

Enclosures

cc: Mark McGuire

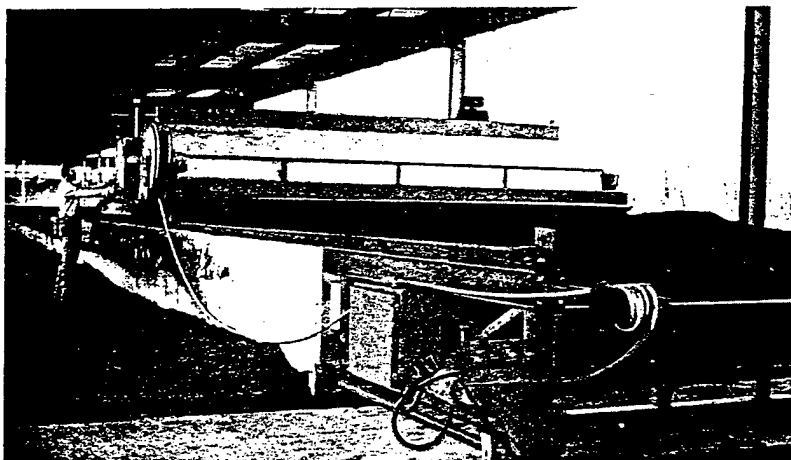
DAVIS
PROCESS div.

PROPOSAL

PREPARED ESPECIALLY FOR

U.S. ARMY, Korea

ENCLOSED MECHANICAL COMPOSTING SYSTEMS



Davis Residuals Management

U. S. FILTER, Davis Process Composting Systems

Enclosed Process Solutions for Waste Management

Composting of municipal wastes in this country has been practiced since the early 1970's. The first technologies employed the "open pile" method, simply mixing the correct ratios of materials and placing them in a windrow. Because this method allowed for very little control of the composting environment, a poor quality compost product was usually the result. The process also required 6 to 9 months to convert the waste product into compost.

In the last decade, "in-vessel or enclosed" composting has become the preferred method of composting. By confining or enclosing the process, the composting environment can be controlled by forced aeration and monitoring the process. This control over the biological composting process offers two distinct advantages over open pile composting. First, the time required for composting is reduced from 6-9 months to 30-40 days, thereby greatly reducing the land requirement and manpower requirement. Second, by controlling the composting process you are able to produce a compost product of a much higher quality and greater utility.

Since 1982, U.S. FILTER, Davis Process has established itself as the leader of enclosed vessel composting technology with over 50 plants presently operating worldwide. These composting plants operate on all types of sludges, digested and non-digested, primary and secondary, and waste activated. This level of expertise and full scale plant experience makes us the world's leading in-vessel composting system vendor for composting wastewater sludges.

To date, U.S. FILTER, Davis Process has supplied systems for twelve U.S. municipalities. These include plants located in Portland, Oregon; East Richland County, South Carolina; Dothan, Alabama; Clayton County, Georgia; Endicott, New York; Lancaster, Pennsylvania; Springfield, Massachusetts; Binghamton, New York; Musconetcong Sewerage Authority, New Jersey; Bristol, Tennessee; Geneva, New York and Guelph, Ontario. The U.S. Filter Davis system has been selected as the basis of design as the most cost effective alternative for sludge management by many municipalities, and several other municipalities have decided to build the Davis system as a part of a negotiated procurement process.

U.S. Filter, Davis Process EconoBay System

For communities producing smaller amounts of waste, the EconoBay agitated bed design composting system is more appropriate than a completely enclosed in-vessel system or the larger Agitated Bay design. In those cases, U.S. Filter, Davis Systems offers the same process technology that helped it become the leader in the design of in-vessel composting systems.

In the U.S. Filter EconoBay System, the composting process takes place in one or more parallel bays approximately 115 feet long. U.S. Filter, Davis process offers five different bay widths and five different compost turning devices to insure the most economical design and operation.

Each day, the organic waste material and amendment are mixed together with a loader and deposited into the loading end of the bay. Each day of operation, the transfer mechanism positions the compost turner at the discharge end of the first bay. The turner then moves through the bay, mixing and turning the material and moving it toward the discharge end, about 7 feet each time the turner is operated.

When the turner reaches the loading end, it mixes the new material and moves it into the first aeration zone. After completing the cycle in one bay, the turner travels back down the bay walls and moves onto the Transfer mechanism and then repeats the procedure in the next bay. The turning and transfer cycles are totally automatic, so the operator is free to load and unload material and to perform routine maintenance.

During the composting process, positive aeration is achieved by a series of blowers, which force air into the mixture through a gravel aeration bed in the bottom of each trough.

It takes approximately twenty days for the composting material to move from the loading end of the bay to the discharge end of the bay. Each time the turner is operated, compost is discharged from the system. After being stockpiled for about thirty additional days, this cured compost is ready to be used. Although it is recommended, it is not necessary for this curing compost to be stored on a paved surface or under cover. Faster curing can be achieved by simply adding one or more "curing" bays. This would produce a fully cured compost product in about thirty total composting days.

One of the benefits of this type system is that it is modular in design and its process capacity can be increased very easily by simply adding bays. Each compost turner has the capacity to work four bays each day.

U.S. Filter, Davis Process Composting

Sizing Data

Typical EconoBay Composting System

The following three pages are sizing requirements for a composting system to compost the organic wastes specified. The number of composting bays required is dictated by the number of days process retention time and the length of the bays. A standard bay length of 115 feet (105 feet process length) will allow for 21 days retention time if the plant is operated (loaded) 5 days per week. The material is moved and agitated five days per week. If longer retention is desired or if the plant operates 7 days per week, it may be preferable to increase the length of each bay rather than increase the number of bay. This eliminates the need for additional materials handling.

U.S. FILTER, DAVIS PROCESS ECONOBAY

Composting System

Project Data Input Assumptions

25-Mar-97

Project Name :

U.S. ARMY, Korea

Consulting Engineer :

Davis Project Number:

Wet Tons Per Year Biosolids:

Days Operated Each Week:

Wet Tons Biosolids Per Operating Day:

Dry Tons Biosolids Per Calendar Day:

Dry Tons Biosolids Per Operating Day:

Biosolids Percent Dry Solids:

Biosolids Bulk Density:

Amendment Selected:

Amendment Moisture:

Amendment Bulk Density:

Amendment Cost:

Use Recycled Compost as Mix Component?

Labor Rate:

Credit for Sale of Compost:

Power Cost:

Desired Mix Moisture @ Loading:

Days Process Retention in System:

Compost Curing Days Required:

Current Landfill Tipping Fee:

Round Trip Miles to Landfill:

97009	
133	Tons
5	Days
0.5	Wet Tons
0.365	Dry Tons
0.5	Dry Tons
20	% D.S.
60	Lbs/CF
Yardwaste	
45	% H2O
16	Lbs/CF
\$0.00	/Ton
Yes	
\$0.00	/Hr
\$0.00	/Cubic Yard
7	Cents/KwH
60	% Moisture
21	Days
30	Days
\$35.00	/Wet Ton
30	Miles

U.S. FILTER, DAVIS PROCESS, ECONOBAY COMPOSTING
SYSTEM SIZING

PROJECT: U.S. ARMY, Korea 25-Mar-97
CONSULTANT: PROJECT NO: 97009

DESIGN CRITERIA

Operating Days Per Week:	5
Primary Organic:	Biosolids
Dry Tons Per Calendar Day:	0.4
Dry Tons Per Operating Day:	0.5
Percent Dry Solids:	20%
Bulk Density:	60 lbs/cf
Secondary Organic:	Yardwaste
Percent Moisture:	45%
Bulk Density:	16 lbs/cf
Retention Days Required:	21
Curing days required:	30

BASIS OF DESIGN

Utilizing the design criteria as described above, the system design requirements are as follows:

Mix moisture of components into system:	60%
Volumetric ratio of components:	
Biosolids:	24.2%
Carbon Amendment:	24.2%
Recycled Compost:	51.6%
Volume of Biosolids:	85 cu. ft.
Volume of Amendment:	85 cu. ft.
Volume of Recycle:	182 cu. ft.
Volume Reduction After Mixing (Assumed):	15%

DESIGN DETAILS

Daily Volume of Mix Feed into System:	326 cu. ft.
Bay Length:	115.0 ft.
Bay Width:	16.3 ft.
Material Height:	3.3 ft.
Process Length:	105.0 ft.
Process Volume (each bay):	5614 cu. ft.
Days Material Agitated:	15
Days Retention in System:	21
Compost Production Each Day:	3 cu. yds.
 Number Bays Required:	 1
Plant Operations Each Day:	1.6 Hours

Amendment Requirements

Tons per Operating Day:	0.68
Tons per Year:	177
Amendment Cost @ \$0.00 per ton	\$0
Processing Cost @ \$0.00 per ton	\$0
 Building Footprint Required:	 36 ft. x 165 ft. 5,990 sq. ft.
 Biofilter Footprint Required:	 1,797 sq. ft.
 Curing Pad Footprint Required:	 1,297 sq. ft.

We estimate the electrical power required to be approximately: 243 KWH/work day
 We estimate the electrical power required to be approximately: 224 KWH/static day
 This would include all compost turning equipment and the aeration system.

We would estimate the annual O & M costs for the Compost System only to be as follows:

		<u>\$/Ton D.S.</u>	<u>\$/Year</u>
Carbon Amendment		\$0.00	\$0
Electric Power @ .07/KWH		\$45.52	\$6,048
Operations (Operators & Rate)	0.3 \$0.00	\$0.00	\$0
Equipment (Mtn & Repair)		\$18.45	\$2,451
		<hr/>	<hr/>
Subtotal O & M:		\$63.97	\$8,499
 Compost Sale Credit	\$0.00 / Cubic Yard	\$0.00	\$0
		<hr/>	<hr/>
TOTAL O & M:		\$63.97	\$8,499

Standard Scope of Supply

U.S. FILTER, DAVIS PROCESS, ECONOBAY SYSTEM EQUIPMENT

Project: U.S. ARMY, Korea Project No. 97009
Engineer:

Econo Compost Agitator

- 1 Each Model T510 Compost turner including agitating/turning unit, complete with all necessary hydraulic motors, controls, power reels, and related hardware.
Transfer platform not required.

Agitator Spare Parts

- 1 Lot Spare parts to be supplied for mechanical and hydraulic components. The Spare Parts list can vary depending on system requirements.

Process Control System

- 1 Each Programable Logic Controllers with Enclosures.
6 Each Proximity Switches (Machine Position Sensors).
4 Each Manually operated Thermocouples and cable.
1 Each Digital Process Controller

Process Aeration System

- 4 Each Blowers with cast aluminum housing and wheel and TEFC direct drive motor mounted on cast aluminum base.
1 Lot Plenum piping within bay.

Bay Wall Rail System

- 230 Feet ASCE Crane Rail or equal Rail System for bay walls and transfer platform (If transfer platform required).
1 Lot Bay Wall Rail Anchors and other necessary hardware.

Mixing Equipment

- | | |
|--------|--|
| 1 Each | Batch Mixer unit with automatic weight scales.
(Optional, but included in estimate) |
|--------|--|

Biomass Moisture Adjustment System

- | | |
|--------|--|
| 1 Each | Header system with directional spray nozzles to adjust moisture of composting material if necessary. |
|--------|--|

Start-up and Training

- | | |
|-------|---|
| 1 Lot | System start-up and initial operational assistance, including operator training for process operations and equipment maintenance. |
|-------|---|

Not included in U.S. FILTER, Davis Equipment Scope of Supply

Construction Management
Grading, Site Preparation, and Foundation
Site Utilities
Concrete Construction
Cure Pad Paving
Building or Building Erection
Aeration Gravel
Heating, Ventilation, Air Conditioning
Building Electric and Lighting
Motor Control Centers
Plumbing
Aeration Piping Outside of Bay Walls
Rolling Equipment (except Mixer Truck)
Amendment Storage, Metering & Transporting System
Amendment Processing Equipment
Odor Control Equipment
Installation and Erection of Equipment
Conveying Systems Outside of Compost Building
Dewatering Equipment
Permitting and Site Engineering
Bonding and Taxes

The estimated "Constructed" price includes all composting equipment, enclosed compost building, all slab and bay wall concrete work, building erection and installation of equipment, electrical, and system engineering. Land cost, site preparation, site utilities, and any equipment not contained in Davis' scope of supply or specifically noted are not included in this estimate.

The estimated price provided with this proposal is based on current pricing and assumes a twelve month construction period. This is an estimate only, and prices are subject to change without notice at any time.

EconoBay Equipment Description

Compost Turner:

The compost turner is of the agitation/conveyor design for operation within an open bay type composting system. The turner completely mixes the bay contents along with moving the material toward the bay discharge end and then conveying it from the bay.

The compost turner is electro/hydraulically powered and designed to turn or mix the contents of a series of compost bays. The unit consists of a rotating shaft with numerous material paddles attached. The paddles rotate into the pile; shearing, blending and aerating the composting material. The material moves approximately 7 feet each time the compost turning device operates.

All electrical and hydraulic components on the unit are suitable for severe duty, high moisture, corrosive and hostile environmental conditions.

The turner is constructed to extend from one bay side wall to the opposite side wall. The turner is supported on both rails by four wheels (two per side). The wheels allow for slight misalignment of the rails. The turner is designed to operate on 6-inch wide walls.

The turner frame is of heavy wall tubular steel construction designed to accept all imposed loads.

Curtains or skirts are provided to minimize spillage.

Control System:

The control system for the compost turner is housed NEMA 4X enclosures. Control switches, indicating lights and appropriate labels are provided on the front of each cabinet.

The control system is designed to meet non-mixing forward or reverse travel.

Upon initial lowering of agitator/conveyor at the discharge end, automatic start-up takes place.

Automatic forward travel is variable speed based on total load to conveyor and drum.

Automatically stop drive system under overload condition and restart after machine clearing.

Upon reaching the loading end of the bay, the turner stops and the conveyor makes a complete revolution to clean the bed before raising to transport position.

Automatically sense end of cycle and return turner to home position.

Emergency safety stop buttons are provided on each control panel.

Power is supplied to the turner through a festooning automatic rewind reel.

Aeration System:

The aeration system consists of a series of blowers in each standard length bay. Each blower feeds air into a separate aeration plenum in the floor of the bay. The blowers supply necessary oxygen to the biomass and can be used for temperature control. Each blower is controlled based on temperatures throughout the bay.

A thermocouple assembly is provided for each blower to be mounted in each aeration zone.

Each blower has a piping assembly to supply air distribution in each plenum to properly control the biomass conditions.

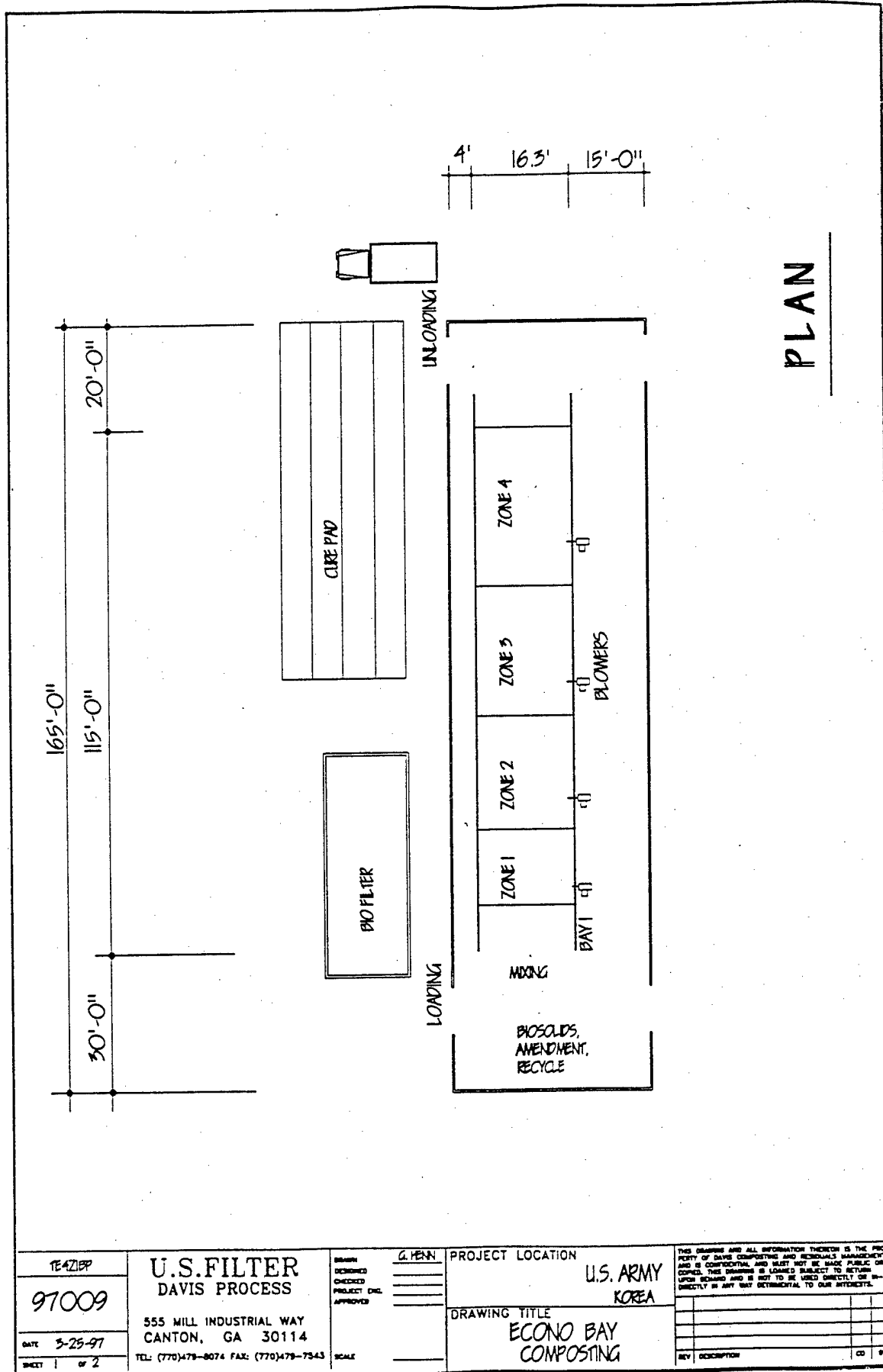
Moisture Control System:

Each bay is supplied with an overhead moisture adjustment system consisting of PVC headers with directional spray nozzles to adjust the moisture content of the bay contents if necessary. If the moisture content of the composting biomass falls below desired levels, water can be added at precise volumes to adjust the moisture of the compost and return the process to optimum composting conditions.

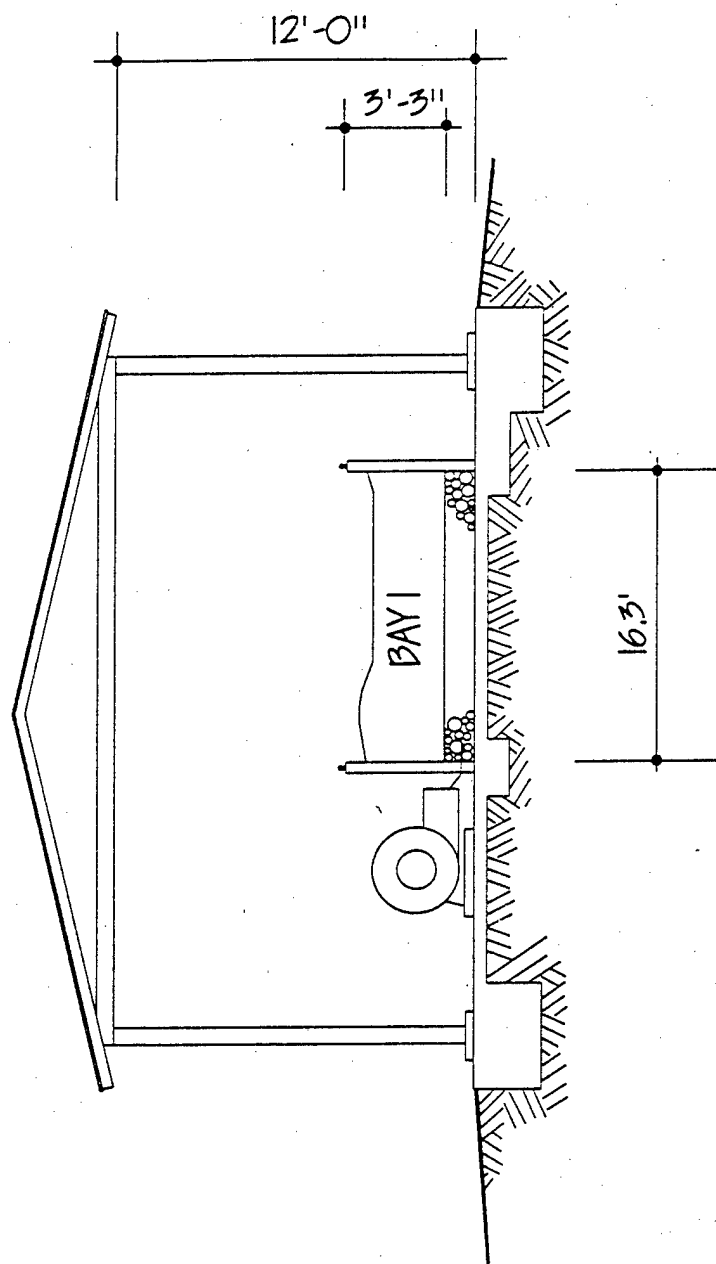
U.S. Filter, Davis Composting

Typical EconoBay System Drawings

The drawings that follow are for a typical *EconoBay* system of the size necessary to process the volume of wastes specified. The building dimensions stated in the sizing requirements for the system are approximate and can be modified depending upon equipment selection and space requirements:



TEAZLER 97009	U.S. FILTER DAVIS PROCESS	DESIGN CHECKED PROJECT ENG. APPROVED	G. HEN	PROJECT LOCATION U.S. ARMY KOREA	THIS DRAWING AND ALL INFORMATION THEREON IS THE PROPERTY OF DAVIS COMPOSTING AND RECYCLING MANAGEMENT AND IS CONFIDENTIAL AND MUST NOT BE MADE PUBLIC OR COPIED. THIS DRAWING IS LOANED SUBJECT TO RETURN UPON DEMAND AND IS NOT TO BE USED DIRECTLY OR INDIRECTLY IN ANY WAY DETRIMENTAL TO OUR INTERESTS.
DATE 3-25-97	555 MILL INDUSTRIAL WAY CANTON, GA 30114	SCALE		DRAWING TITLE ECONO BAY COMPOSTING	
SHEET 1 OF 2	TEL: (770)479-8074 FAX: (770)479-7543				



SECTION

TE42IB5	U.S. FILTER DAVIS PROCESS	DESIGN: <u>G. HENN</u>	PROJECT LOCATION: <u>U.S. ARMY KOREA</u>	THIS DRAWING AND ALL INFORMATION THEREON IS THE PROPERTY OF DAVIS COMPOSTING AND RESIDUALS MANAGEMENT AND IS CONFIDENTIAL AND MUST NOT BE MADE PUBLIC OR COPIED. THIS DRAWING IS LOANED SUBJECT TO RETURN UPON DEMAND AND IS NOT TO BE USED DIRECTLY OR INDIRECTLY IN ANY WAY DETRIMENTAL TO OUR INTERESTS.
97009		CHECKED: _____ PROJECT ENCL. _____ APPROVED: _____	DRAWING TITLE: <u>ECONO BAY COMPOSTING</u>	
DATE: <u>3-25-97</u>	555 MILL INDUSTRIAL WAY CANTON, GA 30114	SCALE: <u>N.T.S.</u>	REV DESCRIPTION	
SHEET <u>2</u> OF <u>2</u>	TEL: (770)478-8074 FAX: (770)478-7543		CO 97	

Appendix H: Resource Recovery Systems

K WINDROW COMPOSTERS

PRESENTING THE

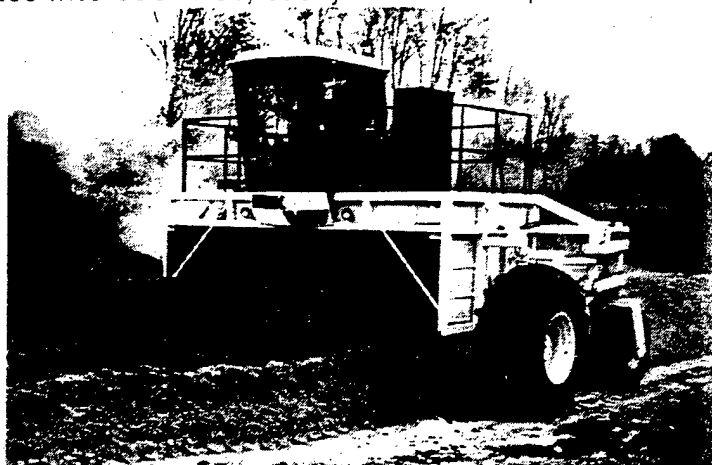
Converts nuisance organic wastes into odor free, easily handled compost.

For Use In:

- Sludge
- Leaves, yard wastes
- Livestock & Poultry Manures
- Municipal solid wastes
- Agricultural residues
- Racetrack wastes
- Packing and cannery wastes
- Paper mill wastes
- Complimentary with other systems
- Mixing for static pile

Options

- Special designs



K-W Model 614

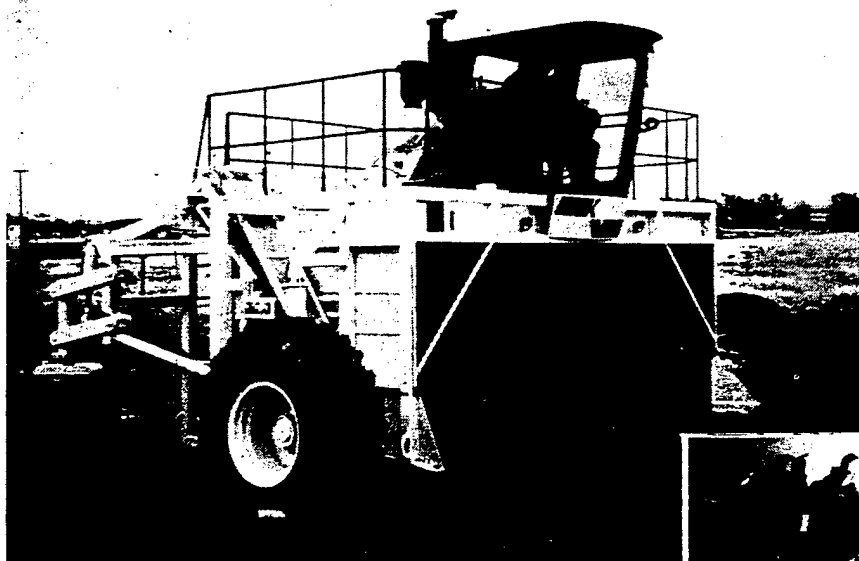
STANDARD SPECIFICATIONS: ALL MODELS

- Engine - Caterpillar 3306T Diesel, 325 h.p. or Caterpillar 3406T Diesel, 440 h.p.
- Tunnel - Height adjustment of 12" front and rear.
Polyethylene lined to reduce sticking.
- Drum - Diameter - 16 inches Thickness - 1/2 inch steel
Speed - 780 r.p.m. Shaft - 3 3/8" stress proof, runs full length of drum, center support.
- Flails - Fixed, attached with bolt, hard surfaced.
- Tire Size - Front - 18.4 x 26 or 23.1 x 26 or 28L x 26
Rear - 12.5L x 15 12.5L x 15 16.5L x 16.1
- Wheel Drive - Dual hydrostatic, wheel driven by planetary gear. Speeds of 0-4 mph forward and reverse. Automatic load control.
- Cab - Deluxe. McLoughlin Body Works cab. Dimensions 4'x4'x5' with heater, air conditioner, tinted glass, defrost, windshield wipers, radio, high back cushion seat, tilt steering console. Meets OSHA requirements. Extra 1/4" steel plate under cab.
- Warranty - OEM warranty for Caterpillar engine for 1 year. Parts and labor for 1 year. Extension of engine warranty up to 5 years available.
- Lights - Four forward and two rear.
- Options - Belt or hydraulic drum drive on all models. Tunnel height and width modifications. Fire extinguisher system. Tracks. Low Profile Models.

Contact:
LES KUHLMAN, Ph. D.
RESOURCE RECOVERY SYSTEMS
OF NEBRASKA, INC.

Route 4, 511 Pawnee Dr., Sterling, CO 80751
Phone: (970) 522-0663 FAX: (970) 522-3387

K COMPOST EQUIPMENT



K-W Model 616

K COMPOST
W EQUIPMENT



DRUM ASSEMBLY

DETAILED MODEL SPECIFICATIONS

	K-W 614	K-W 616-4	K-W 718
Tunnel Dimensions	6'x14'	6'x16'	7'x18'
Engine (Caterpillar)	3306	3406	3406
Engine Horsepower, Max.	325	440	440
Capacity, Tons/Hour (Sludge & Manure)	2000	3000	3000
Capacity, Yds ³ /Hour (Leaves, Yard Waste, MSW)	5000	7500	7500
Drum Drive (Standard)	Belt	Belt	Hydraulic
Weight, Lb.	24,500	26,000	28,000
Overall Width	24 feet	27 feet	29 feet
Overall Height	12'6"	12'6"	13'10"
Overall Length, Front To Rear	12'	15'6"	15'6"
Tire Size (Standard) Front	18.4x26	23.1x26	23.1x26
Tire Size (Standard) Rear	12.5Lx15	16.5Lx16.1	16.5Lx16.1
Fuel Consumption, Gal./Hr.	12	19	19
Fuel Tank Capacity, Gal.	140	225	225

MISCELLANEOUS STANDARD FEATURES

- Twin rear ladders for access each side of machine
- Heavy duty twin disc clutch
- Hand rails enclose deck. Walkways of anti-slip material
- Hydraulic tubing used for fluid lines whenever possible.
- Rear wheel assembly constructed with 3 inch stressproof shaft.

FURTHER DESCRIPTION AND EXPLANATION OF K-W SPECIFICATIONS

May 1992

1. **ENGINE** - Caterpillar 3306 (300 h.p.) or 3406 (440 h.p.) DITA diesel, H.D. full flow radiator, IBF 314 twin disc clutch, 12 volt starter, 12 volt charging alternator, H.D. dry type air cleaner, high water temperature shut-off, low oil pressure shut off, suction fan. The 3406 engine has a 24 volt system.
2. **CAB** - McLaughlin Body Works operator cab with dimensions of 4'x4'x5', air conditioner, heater, tinted glass, front wipers, tilt steering console, high back cushion seat. All wiring is enclosed. OSHA approved. AM/FM radio optional.
3. **DRUM** - Tube diameter of 16 inches, 1/2 inch wall thickness, 3.4375 inch stress-proof shaft running the full length of the drum with center support in the drum. Drum spins at approximately 800 r.p.m.
4. **FLAIL HOLDERS** - Constructed from 1/2 inch 4130 material, hard faced and welded to drum. Flails are fixed and attached with bolt. Fixed flails are easy to replace, may be hard surfaced for longer life and are not lost by the wearing out of the bolt or the hole in the flail.
5. **TUNNEL** - Lined with Ultra High Molecular Weight (UHMW) polyethylene. Polyethylene will withstand hard knocks from debris better than belting and will last longer than either belting or steel lined tunnels. Rusting of steel and weathering of belting occurs at attachment points causing steel or belting to come loose.
6. **PLANETARY GEAR** - in drive wheels. Consists of two wheel drive motors of 183.4 CIR each capable of 5500 psi maximum operating capacity. Pump is tandem axial piston propel pump with integrated electronic displacement control. Each section is 2.8 CIR capable of 500 psi maximum operating pressure. Superior to chain drive. Chains may break, stretch or come off and are difficult to keep shielded. Should a chain come off or break during loading and/or unloading the machine would become free wheeling as there are no brakes. This problem does not exist with the planetary gear in the drive wheels.
7. **AUTOMATIC LOAD CONTROL** - To maintain machine speed and engine load drop. Can be switched from automatic to manual mode. When in automatic mode, the K-W will slow down or stop when the engine r.p.m. drops to a set point.

Page - 2

FURTHER DESCRIPTION AND EXPLANATION OF K-W SPECIFICATIONS

8. **HYDRAULIC DRUM DRIVE** - Optional on the K-W 614 and K-W 616 and standard on the K-W 718. The K-W 718 is available with belt driven drum. Drum is driven by two 47.2 cubic inch per revolution motors. Each motor is capable of 35,000 inch pounds of torque at 5000 psi system pressure. Motors are driven up to 600 rpm by four 6.1 cubic inch per revolution, hydrostatic pumps. Drum drive pumps are plugged into a 1.19:1 increasing ratio helical gear pump drive. Drum drive motors are capable of 460 continuous horsepower. The pump drive is rated at 675 continuous horsepower.
9. **FRONT DRIVE WHEELS** - are set a sufficient distance from the frame so that they travel in the middle of the pathway between the windrows. This area is the driest and most solid compared to the area next to the windrow which may be soft and wet.
10. **REAR WHEELS (crazy wheels)** - Constructed with 3" diameter vertical shafts.
11. **TIRE OPTIONS** - Include 18.4 x 26, 23.1 x 26 and 28.1 x 26 on the front and 11.5L x 15, 12.5L x 15 and 16.5 x 16.1 on the rear.
12. **HYDRAULIC PUMPS AND MOTORS** - for hydrostatic drive are Sundstrand.
13. **ADDITIONAL PROTECTION FEATURES** - Fuel and hydraulic tanks are constructed of 3/8" steel on the bottom and 1/4" steel on the sides and top. An additional 1/4" steel plate is placed under the cab for added protection. Drive belts and drive lines are fully shielded. Deck is fully enclosed with a guard rail. There are no obstructions on the deck.

Resource Recovery Systems of Nebraska, Inc.

Route 4, 511 Pawnee Drive — Sterling, Colorado 80751-8696

970) 522-0663 — FAX (970) 522-3387

PRICE LIST KW COMPOSTING EQUIPMENT

January 1, 1997

ALL PRICES ARE F.O.B. COLORADO

1. KW 510 - \$121,000.00
 - a) Tunnel - 5' x 10'
 - b) Engine - 230 h.p.
 - c) Drum - Hydraulically driven
 - d) Rear Wheel Drive
 - e) Tires - 9.5L x 15 Front, 13.6 x 28 Rear
2. KW 614B - \$130,000.00
 - a) Tunnel - 6' x 14', Rectangular
 - b) 3306 DITA Caterpillar Engine, 300 h.p.
 - c) Drum is belt driven, clutch engaged
 - d) Front Wheel Drive
 - e) Tires - 18.4 x 26 Front, 12L x 15 Rear

Options:

 - a) Hydraulic drum drive \$23,760.00
 - b) 23.1 x 16 front tires 2,025.00
 - c) 28L x 26 front tires 2,275.00
 - d) 16.5 x 16.1 rear tires 1,485.00
 - e) Increase engine h.p. to 325 2,000.00
3. KW 616B - \$167,500.00
 - a) Tunnel - 6' x 16'
 - b) 3406 DITA Caterpillar engine, 440 h.p.
 - c) Drum - Belt driven, clutch engaged
 - d) Tires - 23.1 x 26 Front, 16.5 x 16.1 Rear

Options:

 - a) Hydraulic driven drum \$34,460.00
 - b) 28L x 26 front tires 2,275.00
4. KW 718H - \$212,500.00
 - a) Tunnel - 7' x 18' Rectangular
 - b) 3406 DITA Caterpillar engine, 440 h.p.
 - c) Hydraulic Drum Drive is standard
 - d) Tires - 23.1 x 26 Front, 16.5 x 16.1 Rear

Options:

 - a) Deduct for Belt Drive Drum .. \$34,460.00
 - b) 28L x 26 Front Tires ... 2,275.00

NOTE: All models are front wheel drive unless otherwise specified
All models are with McLaughlin Body Works (Implement) Cab

OPTIONS -- ALL KW COMPOSTERS

- 1) Increase Tunnel Width \$2,270.00 per Foot
 - 2) Increase Tunnel Height 2,860.00 per Foot
 - 3) AM/FM Radio 345.00
 - 4) Hydraulic Rear Flap 2,430.00
 - 5) Fire Suppression System 3,210.00
 - 6) Full Tracks(Estimate) 32,000.00 *
- * Option: Good used tracks if available

All prices subject to change without notice.

Appendix I: Transcripts of Phone Interviews With Composting Facilities

Composting Questionnaire

Facility: Burnsville, NC

Contact person: Tom Story, Director of Public Works

phone #: (704) 682-2420

date: 4/23/97

Which type of composting facility do you have?

Aerated static pile. We use a back hoe with a front end bucket to build the piles. We lay down approximately 12 in. of bark over a concrete slab with two 4-in. perforated plastic pipes running through it, build up the pile on top of it, and put 12 in. of bark over the top of the pile for insulation. A squirrel cage blower pulls air in through the pile. We are required to run analyses on the pile for fecal density and metals (TCLP and toxicity test). If the analysis is acceptable, then we can distribute the composted material. A trommel screen is used to separate the fines out of the final compost, which is released to the community. The bark is recycled.

We considered lime stabilization (N-Viro) instead, but the lime costs money, a silo and more equipment are required, it's less simple to operate and would have to pay a surcharge for the technology to the company for any biosolids that were land applied.

Is it indoors or outdoors? Is it under a shelter?

No shelter: We have a few problems when it rains, but the rain is not enough to cause the temperature to drop below the levels required for pathogen

destruction. Mainly, rain causes the solids content to decrease and, thus, the composting time to increase. Available land area for expansion is another problem we are experiencing.

How many dry tons per day do you handle?

We have a 800,000 gpd plant which treats mainly domestic waste with a small amount of industrial. We use contact stabilization and extended aeration. We handle 100 dt/year of sludge.

What is the percent solids of the incoming sludge? Do you dewater it first?

We condition and dewater first using a screw press. This is a thickening process with polymer addition. We achieve on average about 13 percent solids (ranges from 10 to 15 percent).

Do you achieve Class A biosolids in the final product?

Yes.

What is the percent solids of the final product?

We don't run any solids test after the bulking agent is added. The final product has a much high solids content, however. It has the consistency of moist potting soil.

What do you do with the final product?

We produce a relatively small amount of biosolids. Thus, it is not cost effective to sell it. We give it away for use as mulch, soil conditioner, reclamation of poor soil. A local Christmas tree farm used a lot of our biosolids.

What was the construction cost? What is the annual O&M? Does this include amendment?

We spent \$75,000 to \$80,000 to build the entire facility. This includes the concrete slabs, gutters, pump pit, sump pumps, pipes to pump runoff to head works of plant, two 4-in. perforated plastic pipes, squirrel cage blower, conveyor

belt, storage bins, electrical work, and an engineering fee. We already owned a front end loader and other needed machinery at the plant. So, these are not included in the construction cost. The operations and maintenance cost are not significant over and above the routine maintenance at the WWTP. We decided it would be more cost effective to have an operator split working time between the composting and other tasks at the WWTP than to hire a person to work 8 hours a day when only 1 to 2 hours is needed. The main task which needs to be done daily is read the pile temperature.

What do you use for amendment?

Wood chips and/or shredded tree bark. During the fall and winter months, we get these for free from a local plant. During the spring when these are in high demand for lawn use, we have to pay \$10 per dump truck. It basically covers the gas and labor for someone to bring it to our plant. Tree bark is an excellent bulking agent due to the sap and other components which have the ability to generate heat. Our permit requires us to keep the temperature of the pile above 131 °F for 3 days. With a mixing ratio of 2:1 (bark:sludge), we are able to keep the temperature between 150 and 160 °F for 15 days (or longer if necessary). Saw dust does not work as a bulking agent. It does not provide enough air cavities for proper aeration and heat flow.

Do you have any problems with the performance of you facility? (inadequate aeration, clumping, etc.?) No.

Composting Questionnaire

Facility: Fort Collins

Contact Person: Steve Putnam

phone #: (970) 221-6932

date: 4/15/97

Which type of composting facility do you have?

The facility was built for aerated windrow composting. However, we have also used aerated static pile. This works out better because there is less labor involved. In the static pile, we cover the pile with a layer of finished compost.

Is it indoors or outdoors? Is it under a shelter?

We have high winds here and the usual rain and snow. So, we have to have a shelter. It has three walls and is open to the south.

How many dry tons per day do you handle?

The facility was designed for 6 dt/day. However, we actually only compost about 0.25 dt/day. Composting is our backup to using our sludge as fertilizer.

What is the percent solids of the incoming sludge? Do you dewater it first?

We anaerobically digest our sludge and then dewater it. To dewater it, we take it up in the mountains where it is very windy, lay it out on a concrete slab, and leave it. We can achieve between 14 and 70 percent biosolids in 2-3 weeks, depending on the weather.

Do you achieve Class A biosolids in the final product?

We are not worried about achieving Exceptional Quality biosolids.

What is the percent solids of the final product?

What do you do with the final product?

Most biosolids are land applied as fertilizer immediately after digestion and dewatering. The extra biosolids are sent through the composting facility to stabilize and reduce the odor.

What was the construction cost? What is the annual O&M? Does this include amendment?

We spent \$3.5 million for the entire facility and two pieces of machinery. This price would be cheaper for aerated static pile due to less advanced equipment. We spend \$350-400/dry ton in O&M costs.

What do you use for amendment?

wood chips

Do you have any problems with the performance of you facility? (inadequate aeration, clumping, etc.?)

Composting Questionnaire

Facility: Go Wanda, NY

Contact Person: Mike Hutchinson

phone #: (716) 532-5931

date: 4/24/97

Which type of composting facility do you have?

Aerated static pile.

Is it indoors or outdoors? Is it under a shelter?

We have a pole barn. The aeration area has walls. All other areas have a roof, but no walls.

How many dry tons per day do you handle?

1,000 yd/yr

What is the percent solids of the incoming sludge? Do you dewater it first?

Yes, we dewater the sludge to 20 percent solids. Our sludge is anaerobically digested first.

Do you achieve Class A biosolids in the final product? Yes.

What is the percent solids of the final product? 50 to 60 percent

What do you do with the final product?

We give it away to home owners.

What was the construction cost? What is the annual O&M? Does this include amendment?

We converted our existing drying beds into the composting area. This cost us roughly \$30,000. We have been composting since 1990. We designed everything ourselves, and a consulting firm handled the permits.

We spend \$20/yd in O&M costs.

What do you use for amendment?

Wood chips. The most important thing is to get the correct mixture. You may have to experiment for a while until the right mix is found to reach the proper temperatures. The amount of carbon is important. We use a 2:1 ratio of wood chip to sludge.

Do you have any problems with the performance of you facility? (inadequate aeration, clumping, etc.?)

We have experienced no problems with compost quality (i.e., aeration, clumping). We have had problems with our shredding and screening equipment, however.

Could you please send me a copy of your report?

Mike Hutchinson

Village of Go Wanda

Sewage Department

Aldrich Street Extension

Go Wanda, NY 14070

Composting Questionnaire

Facility: Springville, Utah

Contact Person: Rick Roberts

phone #:(801) 489-2745

date: 5/13/97

Which type of composting facility do you have?

Windrow, piled

Is it indoors or outdoors? Is it under a shelter?

We have no shelter. The winter causes problems. In the spring, the compost is too wet and our fecal Coliform count does not pass.

How many dry tons per day do you handle?

2 dry tons/day

What is the percent solids of the incoming sludge? Do you dewater it first?

We dewatered it to 18 to 20 percent solids.

Do you achieve Class A biosolids in the final product?

Yes.

What is the percent solids of the final product?

50 to 60 percent moisture (40-50 percent solids)

What do you do with the final product?

We sell it to the public for use on flowers and other things like that. We do not advertise, and we do not make a profit.

What was the construction cost? What is the annual O&M? Does this include amendment?

For the composting facility with a belt press, we spent \$250,000. We use an old loader we already owned to turn our piles. We can build the piles higher than can be used with a turner. We also spent about 30 percent of \$250,000 on a grinder, which we share.

What do you use for amendment?

Green waste from the city which residents bring to us for free. Otherwise, they would have to pay to have their yard waste landfilled.

Do you have any problems with the performance of you facility? (inadequate aeration, clumping, etc.?)

We may need to look into keeping more of our bulking agent. We need to buy screens.

Winter is our biggest problem. It don't take long to lose temperature. One winter I reheated the piles by mixing in an ammonia fertilizer. We were able to bring the temperatures back up to pass. However, this winter's compost will most likely not meet regulations.

Personally, I wouldn't do it if it is in a moist climate. I would not compost. We are lucky. Most other operations around here cannot meet Class A and end up with Class B biosolids.

Appendix J: Krüger

PROPOSAL
for the
ATAD PROCESS
Camp Casey, Korea

for
U.S. Army Corps of Engineers
P.O. Box 9005
Champaign, IL 61826-9005

Submitted

April 17, 1997

By

John Brinkley
Krüger, Inc.
401 Harrison Oaks Blvd., Suite 100
Cary, North Carolina 27513
Krüger Project No.: 139701

Table of Contents

	Page
I. Prologue	1
II. Introduction to Krüger	1
III. ATAD Process Description	2
A. Introduction	
B. Process Specifics	
C. Land Disposal	
IV. Design Basis	4
V. Scope of Supply	5
VI. Aeration Equipment Description, Operation, Design, and Function	6
VII. ATAD System Price, Present Worth and Cost/Dry Ton	8

I. Prologue

Krüger, Inc. is pleased to offer Camp Casey, Korea a proven solution to meet the U.S. federal requirements regulating the use or disposal of sewage sludge. These standards promulgated in the EPA regulation 40 CFR Part 503, in conjunction with 40 CFR Parts 122, 123, and 501, defining permitting requirements, comprise the regulatory framework of the national sewage sludge program.

Autothermal thermophilic aerobic digestion or ATAD has been studied since the 1960s and significantly developed since the mid-1970s. Currently, there are over 45 full-scale operating facilities in Europe and North America. The Fuchs system now offered through Krüger has a proven track record and has been responsible for the sale of over 90 percent of all systems operating.

The following proposal is offered to Camp Casey, Korea utilizing the entire practical, as well as technical, experience of Fuchs Gas.

II. Introduction to Krüger

Krüger is an environmental technology company. The Krüger Group based in Denmark operates worldwide within the fields of energy conservation, water supply, wastewater treatment, solid waste management, and rural development.

The Krüger Group employs about 1,100 people; approximately half of these people are engineers and scientists with vast experience in their related fields.

Krüger has subsidiaries and offices throughout the world, e.g. Belgium, France, Greece, Ireland, Germany, Cameroon, Burkina Faso, Guinea, Niger, Tanzania, Hong Kong, Indonesia, China, the Philippines, Sri Lanka, and the United States.

Krüger, Inc. (USA) located in Cary, North Carolina operates as an equipment supplier based on Krüger's worldwide patented processes for biological treatment of wastewater. Krüger's process know-how was acquired through years of extensive research and development, which is a continuous effort. Krüger's R&D division currently employs more than 50 engineers and scientists and includes two fully-equipped research and biotechnology laboratories.

Krüger acquired the wastewater business of Air Products & Chemicals, Inc., including the patents for the A/O, A²/O and OASES processes, in June 1991. This coincided with Krüger's acquisition of the worldwide exclusive license right to the OWASA process (optimization of biological phosphorous removal through the fermentation technology). Krüger is now capable of offering the equipment and the process know-how for both secondary and advanced wastewater treatment.

III. ATAD Process Description

A. Introduction

The ATAD process was developed in the Federal Republic of Germany (FRG) in 1970 by Popel and his colleagues working on animal manure and sewage sludge. Much of the available data and process know-how are based upon Fuchs research and design. Fuchs has the most FRG installations and has by far the most process knowledge.

Autothermal Thermophilic Aerobic Digestion (ATAD) is an aerobic digestion process that operates within a thermophilic temperature range (40°C to 80°C) without the introduction of supplemental heat.

The typical ATAD system consists of two reactors that are covered and insulated. Sludge, which has been thickened to a minimum of 4-percent solids, is fed to the reactors on a batch basis. Each batch is 23 hours allowing 1 hour total for the fill and discharge cycles. Sludge in the reactors is mixed and aerated throughout the 23-hour cycle. Temperatures in the first reactor normally exceed 45°C in 6 days detention time and can reach up to 60°C in the second reactor, depending on mixing and tank insulation. As the sludge aerobically digests, heat is released, creating an autothermal environment. The temperature of the reactors being greater than 40°C inhibits nitrification and limits the oxygen demand to approximately 1.4-kg O₂ for every kg of V.S. destroyed. Volatile solids reduction normally ranges from 30 to 50 percent and occurs in just 6 to 8 days HRT. The rate of digestion in the system doubles at 50°C as compared to 20°C. The number of viable organisms in the system start drying off and V.S. reduction stabilizes as the temperature approaches 60° to 65°C; hence, the process is self-regulating.

B. Process Specifics

Feed solids must be prethickened to a minimum of 4-percent solids; 4- to 6-percent solids is desirable. Typically, primary and WAS is co-thickened in the primary clarifier. Gravity belt thickening or DAF thickening may also be used. Sludge less than 3-percent solids will have difficulty achieving thermophilic temperatures because of too much liquid mass. Sludge greater than 6-percent solids is difficult to mix and aerate. The feed solids must also contain a minimum of 55-percent volatile solids.

Influent screening should be used at the plant to eliminate plastics and stringy material from the sludge (10-12 mm bar spacing maximum). A good grit removal system is recommended to minimize abrasion on mixers and aerators. If 100% primary sludge is to be processed through an ATAD system it is recommended that a macerator be put in-line before the ATAD feed.

Typically an ATAD system has a minimum of 2 reactors operating in series. Both concrete and steel reactors have been used, but steel is the most commonly used due to heat stress concerns in concrete. The steel reactors are cylindrical, flat-bottomed and covered. Each reactor is insulated with 4 inches of mineral wool along the walls with 4 inches of high compression foam glass insulation for the top and bottom. The reactors are then clad with ribbed aluminum sheeting for protection from the elements.

Waste sludge is fed to the reactors on a batch basis. Batch feeding in 1-hour/day periods is preferred to minimize short circuiting potential and to ensure that the incoming waste sludge is exposed to thermophilic reactor temperatures for a minimum of 23 hours/day without interruption. This ensures the highest degree of pathogen reduction. A typical reactor detention time is 6 to 8 days (3 to 4 days per reactor). Sixty percent of the volatile solids destruction occurs in the second reactor. Reactor temperatures are monitored with temperature probes.

Waste sludge mixing and aeration is provided with aspirating aerators mounted tangentially through the reactor wall. A circulation aeration device mounted in the center of the reactor can be used in conjunction with the spiral aerators. The waste sludge aeration leads to the generation of surface scum, which is controlled, with foam cutters supported from the reactor roof. The foam cutters do not eliminate the foam, but instead keep it at a manageable level to allow its beneficial use.

Off gas from the process can typically have a slight musty odor and should be either water scrubbed, passed through a biofilter, or diluted with ambient air.

Sludge from the second stage reactor must be cooled down prior to dewatering. Typically, this is done in gravity thickeners, holding tanks, or via heat exchangers. Twenty-five day minimum post-digestion holding is desirable to bring the temperature to 20°C. Mixing should be done in the holding tank for 1 hour each day.

C. Land Disposal

Through the use of a Krüger/Fuchs ATAD system, "Exceptional Quality" sewage sludge can be land-applied on any type of site. There are no human or animal contact restrictions, time limits for land use after application or crop specific limitations associated with land disposal of Class A biosolids from ATAD systems.

The EPA requires periodic sampling to ensure that land applied biosolids meet all the criteria set forth in 40 CFR Part 503 regulation. Generally, this proof is recorded on a daily basis with ATAD waste. Normal system temperature recording, V.S. testing, and metals testing will provide the necessary data required as proof of regulation conformance. This virtually eliminates any unusual sampling methods as may be associated with conventionally digested or lime stabilized biosolids.

IV. Design Basis

The Krüger/Fuchs design is based on over 45 full-scale installations and numerous pilot studies. The design information presented in this proposal represents a preliminary design developed by Krüger and Fuchs specifically for the Camp Casey, Korea Facility.

Design Data

Plant influent flow	2.0 MGD
Sludge Type	WAS
Waste sludge flow rate	8,870 gpd
Dry solids content	5%
Volatile solids content	3.25%

Reactor Design

Number of trains	1
Number of reactors/train	2
Size of reactors each train	<u>Reactor I and II</u>
Diameter	25 ft
Total height	13.5 ft
Filling level	10.5 ft
Working volume	38,511 gallons
Total system retention time	8.7 days

Mechanical Equipment

	<u>Reactor I and II</u>	<u>Total KW/Train</u>
Spiral aerator type	WBL-VII	
Number of spiral aerators/reactor	2	
kW/Spiral	7.5	30
Circulation aerator type	UBL-IV	
Number of circulation aerators/reactor	1	
kW/Circulation	4.0	8
Foam controller type	SSc/1	
Number of foam controllers/reactor	6	
kW/Foam controller	1.0	12

*Power Consumption (Total of All Reactors) 1,150 kwh/day

*ATAD units operate 23 hrs/day. The daily power consumption does not include ATAD feed, transfer, discharge or sludge pumps for transferring sludge to land application vehicles.

V. Scope of Supply

A. General

Krüger, Inc.'s scope of supply shall include process design of the ATAD system, aeration/mixing equipment, all reactor vessels, valves, controls, and instrumentation to facilitate a complete system. Krüger is flexible in the approach to this project and would entertain any suggestions regarding additions or deletions to our scope of supply.

B. Krüger, Inc. Scope of Supply

1. **Process and Design Engineering** - Krüger shall provide engineering and design support for the ATAD system as follows:
 - Process design of Fuchs Process
 - General reactor schematic review
 - Technical instructions for ATAD system start-up, operation and maintenance
2. **Field Service** - Krüger shall perform a variety of field services necessary to start-up, test and operate the ATAD system. The field services included in this proposal shall be as follows:
 - 10 days in 2 trips for start-up assistance by Krüger personnel
3. **Equipment Supply** - Krüger shall furnish the following equipment:
 - 4 spiral aerators
 - 2 circulation aerators
 - 12 foam controllers
 - 1 PLC-based control system, including instrumentation
 - 2 reactor vessel system, installed
 - Temperature Control System
 - ATAD system valves, manual and automatic, installed
 - Labor, materials, and installation required for reactor vessels; fabrication, erection, and hydrostatic testing supervision
 - Structural walkway between reactors, installed
 - Reactor vessel blasting, coal tar epoxy coating, insulation, and aluminum jacket

C. Optional Equipment

Krüger rotary drum type sludge thickener
Krüger odor control system
Krüger/Landia mixers for sludge holding tanks
Krüger belt filter press

Krüger can provide these items if they are not currently available at the plant in question, and are required for proper ATAD system functioning or sludge disposal.

D. Contractor Scope of Supply

- Plant bar screen with a maximum 10-12 mm bar spacing
- Grit removal system
- Pre-ATAD sludge holding tank (2 days minimum capacity)
- Treated sludge storage tank (30 days capacity)
- Utilities - MCC
- Labor and material for installation of aerators, foam controllers, control panel, field wiring, pumps and all associated ancillary equipment
- Reactor vessel foundations
- Water supply and removal for hydrostatic reactor vessel testing
- Odor control system
- Interconnecting piping
- ATAD Discharge & Feed Pumps

VI. Aeration Equipment Description, Operation, Design, and Function

A. Description

The spiral aerator, such as used in ATAD installations, consists essentially of an air-cooled motor, which is integrated with a hollow shaft complete with spiral propeller. The spiral propeller is immersed at an incline into the sludge to be aerated.

B. Operation

When operating, the spiral propeller generates a flow angular to the bottom of the reactor. Simultaneously, in accordance with the "water jet pump principle," the spiral aerator sucks in air through the hollow shaft; this suction produces small bubbles, which are then drawn downward by the jet of liquid.

The very small bubbles, in conjunction with the intense turbulence, provide rapid oxygen transfer and a high degree of oxygen dissolution.

C. Design

The spiral aerators are sturdy and simple in design. The hollow shaft with its shank, the spiral propeller, the intermediate flange, as well as all fasteners, is manufactured from AISI 304 stainless steel.

The drive units are special motors with hollow shafts. The units are high efficiency and equipped with permanently lubricated grooved ball bearings. The motor housings are manufactured from aluminum or a high quality cast-iron.

The aerator shafting is manufactured to allow for easy insertion or extraction. The aerator shaft is inserted into the hollow motor shaft. This allows for accurate and precise shaft guidance.

The aerator shaft is manufactured from extruded seamless AISI 304 stainless steel tube, and is dynamically balanced together with the coupling and the spiral propeller.

The immersion section does not contain any bearings or seals, which eliminates any maintenance work and virtually eliminates wear.

D. Function

The spiral aerators provide the ATAD system with the necessary supply of oxygen and the thorough mixing of the sludge. The spiral aerators also accelerate a rotation of the entire content of the reactor around the vertical axis.

They are arranged tangentially on a standpipe which, in turn, is welded at an angle to the reactor casing. The aerator driving facility and the motor end of the shaft, with the air entry ports are exposed to the atmosphere. The hollow shaft with the spiral propeller leads through the standpipe and the reactor wall into the sludge.

E. General

The ATAD process has many benefits that include high disinfection capability, minimum area requirements, a high sludge treatment rate, and a high V.S. reduction rate, which all spell reduced disposal costs. This technology is easy to operate, does not require full-time staff, and is a cost-effective solution to aerobic digestion consistent with the new U.S. regulations on sludge disposal.

F. Temperature Control System

Generally speaking, the majority of ATAD systems will not require temperature control. When designing an ATAD system a thorough heat balance is generated to determine whether or not the system will be autothermal. Considering all the variables that effect the system, we can determine whether heat supplement, transfer or removal will be needed. We then custom design the system required for the application in question.

VII. ATAD SYSTEM PRICE (4/17/97):

A. Capital Cost of ATAD System Installed:

Krüger-furnished equipment and services per sections IV. B.	\$	1,013,000.00(+/-10%)
--	----	----------------------

B. Operation and Maintenance Cost:

Annual O & M Cost:

(60 kw)(\$0.06/kwh)(23 hr/d)(365 d/yr)	\$	30,200.00
Annual Labor Cost	\$	3,600.00

Total O&M	\$	33,800.00
Total O & M Cost/Dry Ton	\$	50.00
PW of O&M, 20 year @ 7.6%	\$	348,000.00

C. Total Cost Per Dry Ton for Total
Capital and Present Worth:

	\$	100.00
--	----	--------

USACERL DISTRIBUTION

Chief of Engineers

ATTN: CEHEC-IM-LH (2)

ATTN: CEHEC-IM-LP (2)

ATTN: CECC-R

ATTN: CERD-L

ATTN: CERD-M

Defense Tech Info Center 22304

ATTN: DTIC-O (2)

8th US Army, Korea

ATTN: HQ USFK/EUSA (20)

29

03/98